

Hydrogen Flammability Assessment in SMR Containment Using the CAFT Model

Sihyeong Yu^a, Dosu Park^a, Joongoo Jeon^{b*}

^a Department of Quantum System Engineering, Jeonbuk National
University,

^b Division of Advanced Nuclear Engineering, POSTECH





Table of Contents

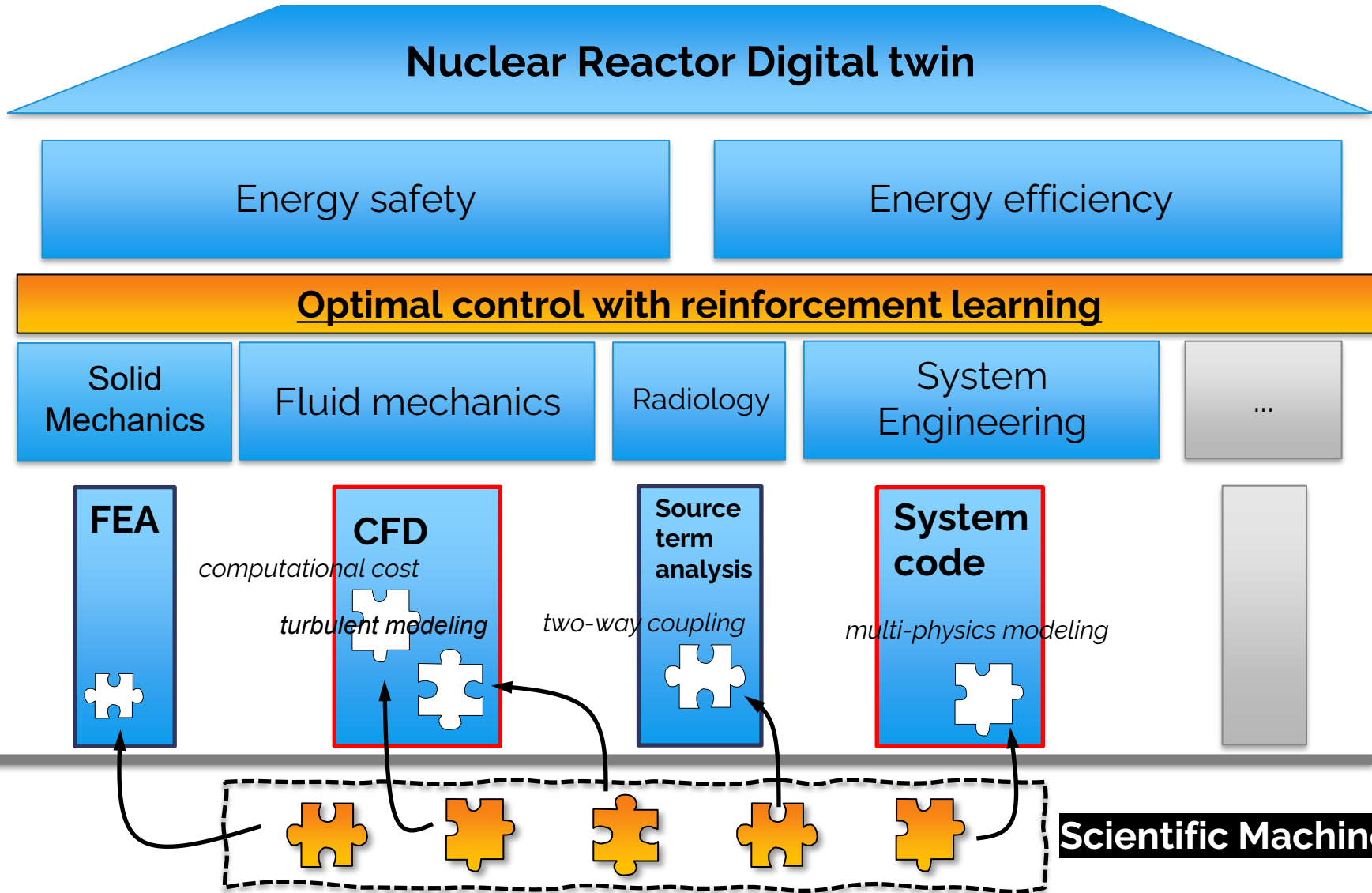
※ PART 1 – Introduction

※ PART 2 – Methodology

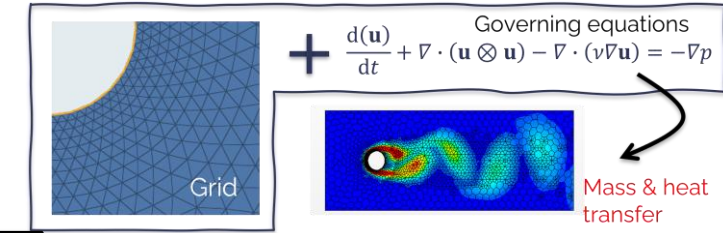
※ PART 3 – Result

※ PART 4 – Conclusion

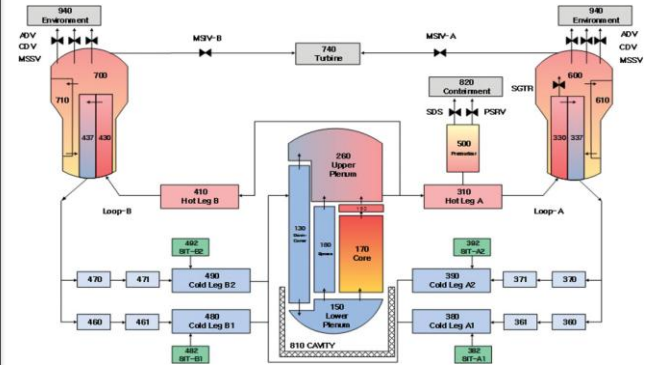
NINE Lab's Vision



- Computational fluid dynamics (CFD)



- System code (nuclear reactor)



Overview

1. What is CAFT model?

- A thermodynamic model that determines flammability by calculating the maximum adiabatic flame temperature of a given gas mixture.

2. Why CAFT model for SMRs?

- Experimental data are scarce under hydrogen-rich and high-T/P conditions; the CAFT model overcomes these limits and is applicable to UFL regimes characteristic of SMR vacuum CNVs.

3. Flammability Assessment in NuScale SMR Severe Accident

- CAFT analysis identifies flammable conditions during 44–48 h, integrating the combined contribution of all major species through a single thermodynamic metric — **refining the conservative margins of single-species criteria with a more accurate, energy-based evaluation.**

Introduction

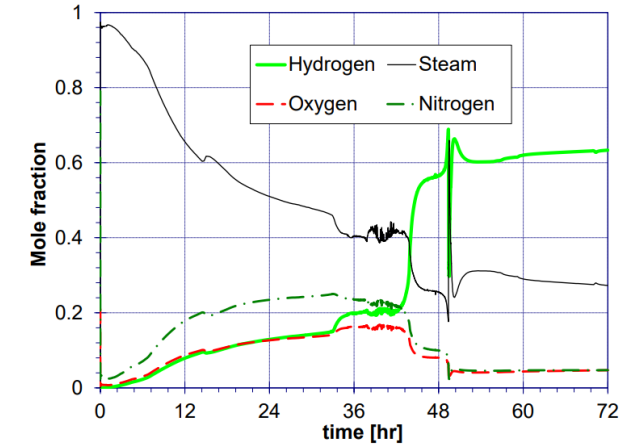
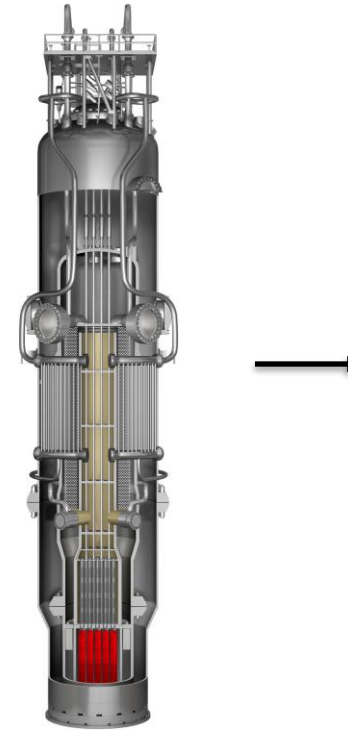
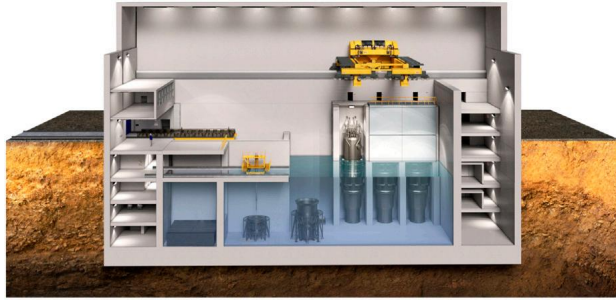


Figure 3.5 Control-volume-averaged containment atmosphere composition

Why Rich-hydrogen Condition?

- Initial state: NuScale SMR adopts a vacuum CNV → Low initial O₂ inventory → Combustion-inert atmosphere
- During Severe Accident: Massive H₂ generation by Core oxidation + Steam condensation on cold CNV walls reduces steam fraction → H₂ concentrates rapidly
- Consequence: O₂ production from radiolysis can drive the mixture toward the Upper Flammability Limit(UFL)

Introduction

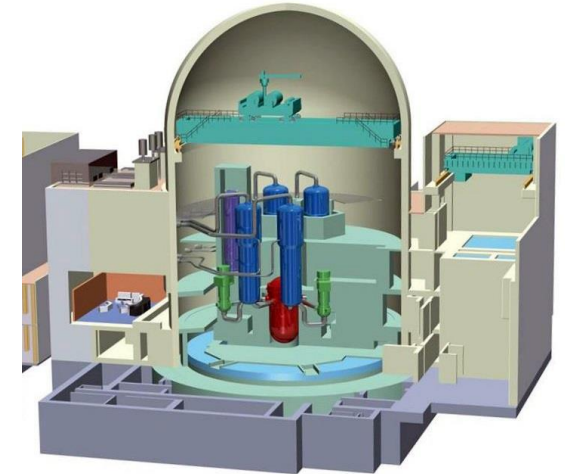


NuScale SMR

- Small vacuum CNV
 - Persistently low O₂ inventory
 - H₂ concentrates in CNV
- **Rich-H₂ condition**

Large PWR

- Large containment volume
 - Substantial O₂ inventory throughout SA
 - H₂ diluted in large volume
- **Lean-H₂ condition**



Research Gap

- Conventional flammability assessment tools (e.g., LFL-based criteria, single-species O₂ thresholds) have been **developed and extensively validated for lean-H₂ conditions** typical of large PWR severe accidents.
- However, **their applicability to rich-H₂ conditions—characteristic of SMR vacuum CNVs—has not been systematically verified.**

Introduction



Research Objective & Novelty

➤ Objective

- Verify the applicability of the CAFT model under hydrogen-rich conditions characteristic of SMR vacuum CNVs
- Apply the validated CAFT model to a representative NuScale severe accident transient (LCC-05T-03, ERI/NRC 18-202)

➤ Novelty / Contribution

- First application of CAFT-based flammability assessment to SMR vacuum CNV transient data
- Identifies a **previously-unreported flammable window (44–48 h)**



Table of Contents

※ PART 1 – Introduction

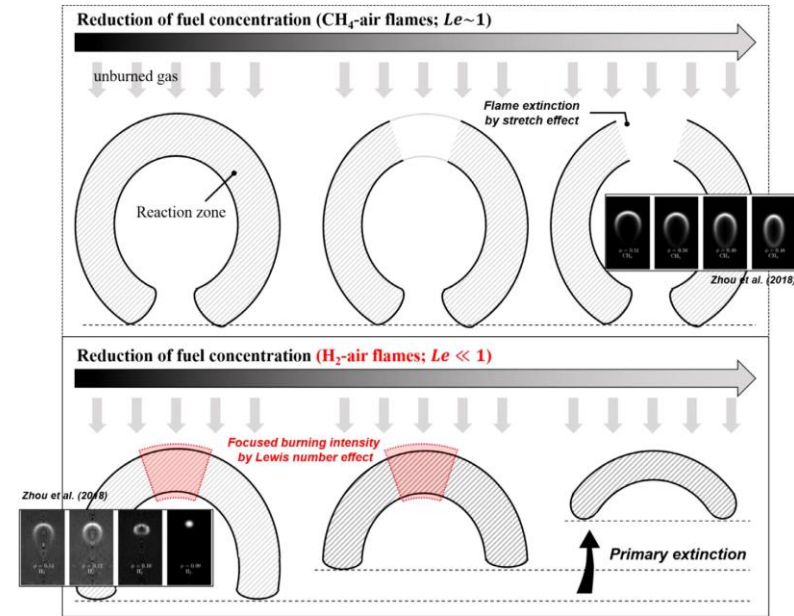
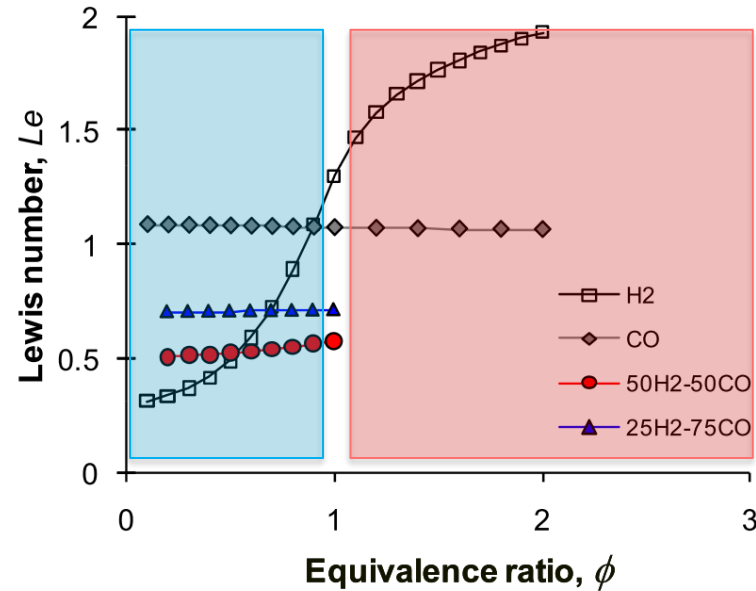
※ PART 2 – Methodology

※ PART 3 – Result

※ PART 4 – Conclusion

Methodology

$$Le = \frac{\text{Thermal diffusivity}}{\text{Mass diffusivity}} = \frac{\alpha}{D}$$



Lean vs Rich : Different Mechanism

Lean hydrogen ($\phi < 1$)

Deficient species: H₂

Mass diffusivity follows H₂ properties

Thermo-diffusively unstable flame

Rich hydrogen ($\phi > 1$)

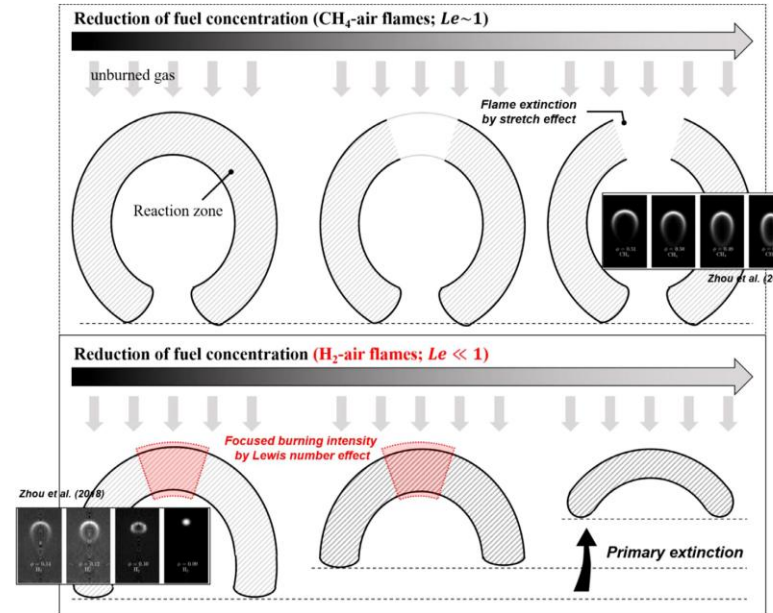
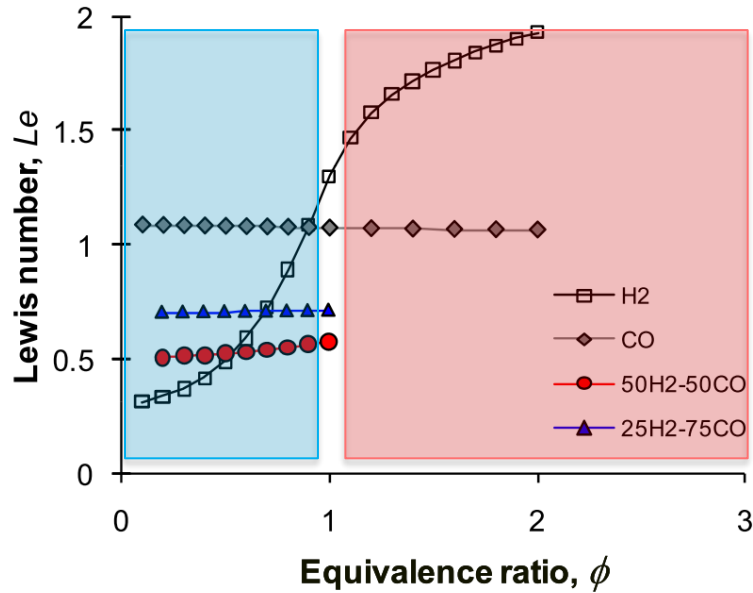
Deficient species: O₂

Mass diffusivity follows O₂ properties

Stable, hydrocarbon-like behavior

[1] Burbano et al., *Laminar burning velocities and flame stability analysis of H₂/CO/air mixtures with dilution of N₂ and CO₂*, International Journal of Hydrogen Energy, 2011
 [2] Jeon et al., *Identification of the extinction mechanism of lean limit hydrogen flames based on Lewis number effect*, International Journal of Heat and Mass Transfer, 2021.

Methodology



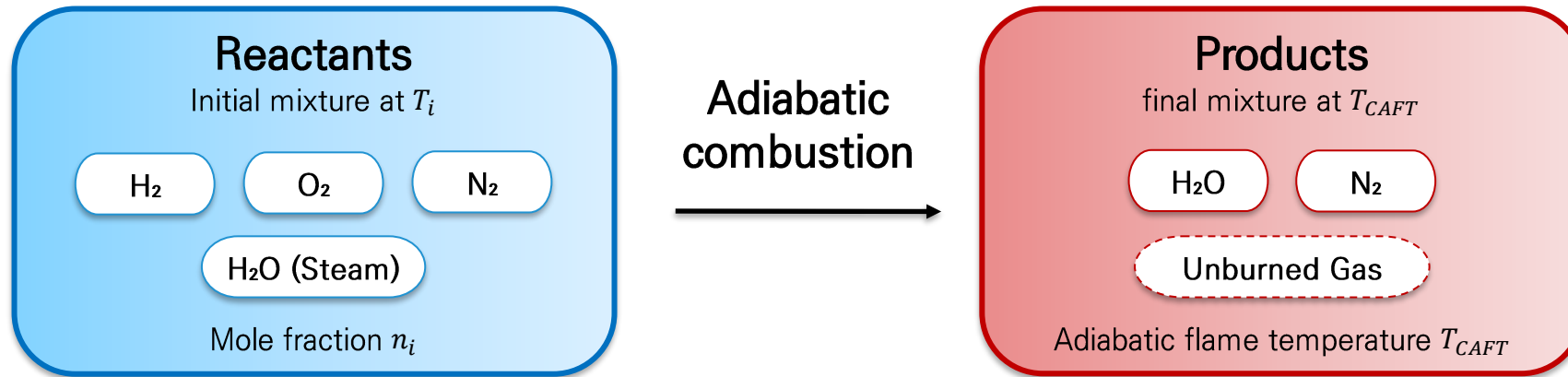
Analogy with Hydrocarbon-Air Flames

- Rich-Hydrogen flames ($Le > 1$) share the same diffusion-thermal regimes as hydrocarbon-air flames
- The CAFT model has been extensively validated for hydrocarbon-air-diluent systems including the upper flammability limit prediction.

[1] Burbano et al., *Laminar burning velocities and flame stability analysis of H₂/CO/air mixtures with dilution of N₂ and CO₂*, International Journal of Hydrogen Energy, 2011

[2] Jeon et al., *Identification of the extinction mechanism of lean limit hydrogen flames based on Lewis number effect*, International Journal of Heat and Mass Transfer, 2021.

Methodology – CAFT Model



$$\sum_{\text{reactants}} n_i [\Delta H_{f,i}^0 + \bar{c}_{p,i} (T_i - T_{ref})] - \sum_{\text{products}} n_i [\Delta H_{f,i}^0 + \bar{c}_{p,i} (T_{CAFT} - T_{ref})] = 0$$

Calculated Adiabatic Flame Temperature (CAFT) Model

- A thermodynamic flammability model that determines combustion feasibility from the **maximum flame temperature** of a gas mixture under **adiabatic, isobaric** conditions.
- Based on the principle of energy conservation: the enthalpy released by complete combustion of reactants equals the sensible enthalpy required to heat the products to the adiabatic flame temperature.
- **Assumption: Well-mixed atmosphere**

[1] Vidal et al., *Evaluation of lower flammability limits of fuel-air-diluent mixtures using calculated adiabatic flame temperatures*, Journal of hazardous materials, 2006.

Methodology – CAFT Model

Core Assumption

- The adiabatic flame temperature at the flammability limit remains nearly constant, independent of the mixture composition.
- Rooted in Arrhenius theory: flame propagation requires a threshold peak temperature corresponding to the minimum reaction rate, which is determined primarily by fuel type rather than diluent composition.

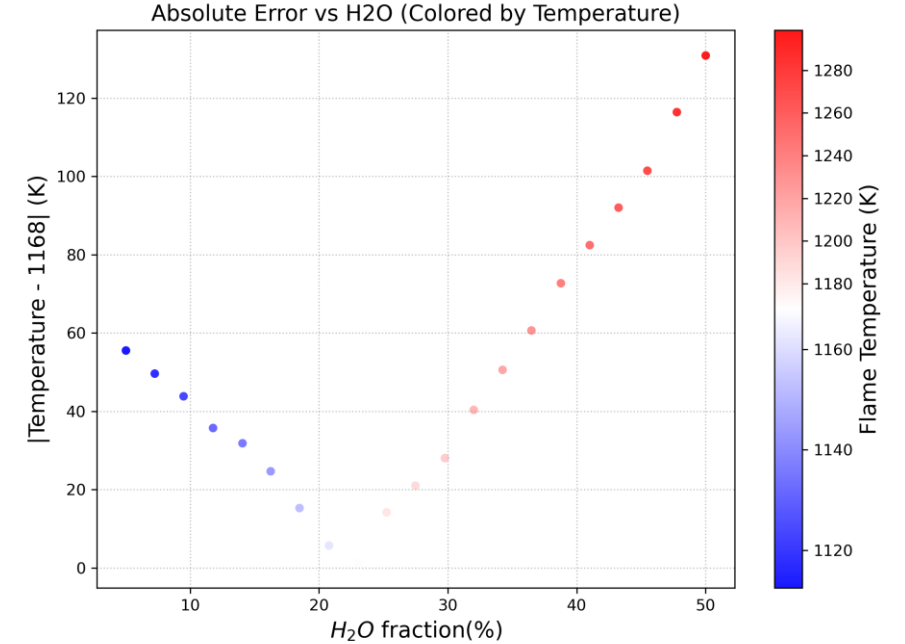
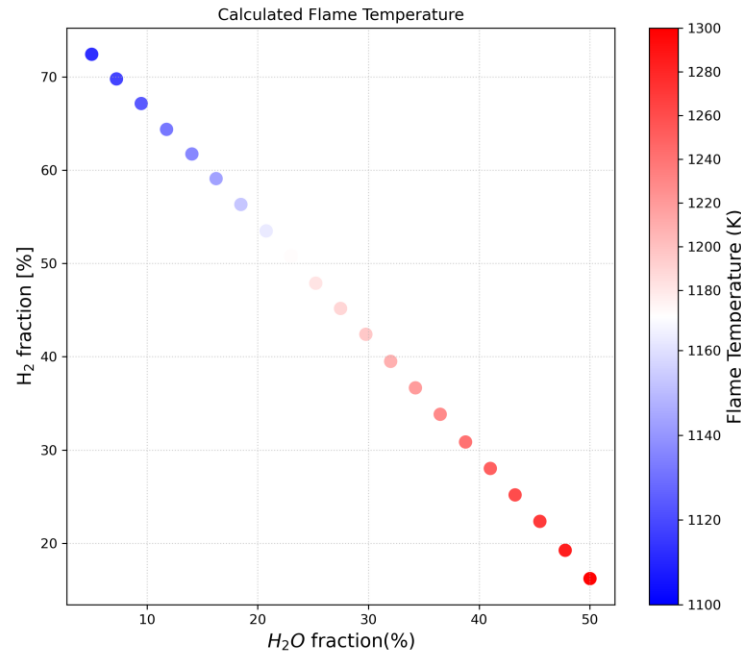
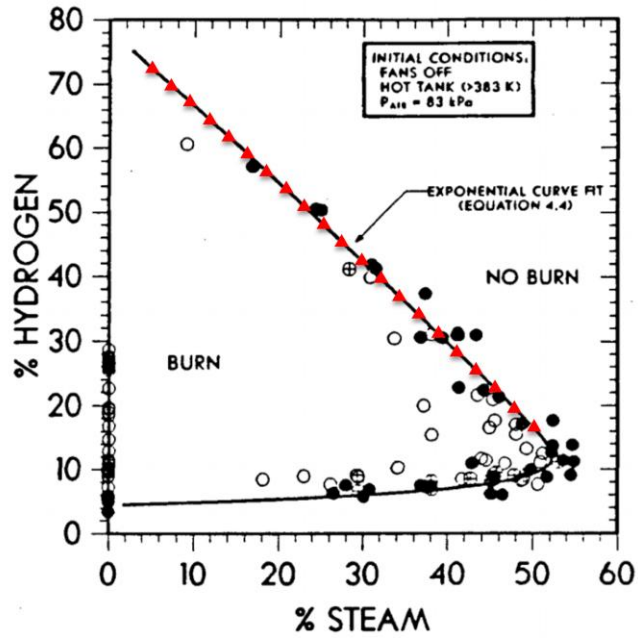
Lower Flammability Limit (LFL)	Upper Flammability Limit (UFL)
$T_{Threshold} \approx 610 \text{ K}$	$T_{Threshold} \approx 1160 \text{ K}$
Measured at H ₂ -air LFL (~4 vol% H ₂)	Measured at H ₂ -air UFL (~75 vol% H ₂)
CAFT model shows up to ~40% error (resolved with CNAFT)	Validated within ~12% accuracy for H ₂ -air-steam (next slide)

Flammability Criterion

- $T_{CAFT} \geq 1160 \text{ K} \rightarrow$ Flammable
- $T_{CAFT} < 1160 \text{ K} \rightarrow$ Non-flammable

[1] M Terpstra, *Flammability limits of hydrogen-diluent mixtures in air*, University of Calgary, 2012.
 [2] Jeon et al., *A flammability limit model for hydrogen-air-diluent mixtures based on heat transfer characteristics in flame propagation*, Nuclear Engineering and Technology, 2019.

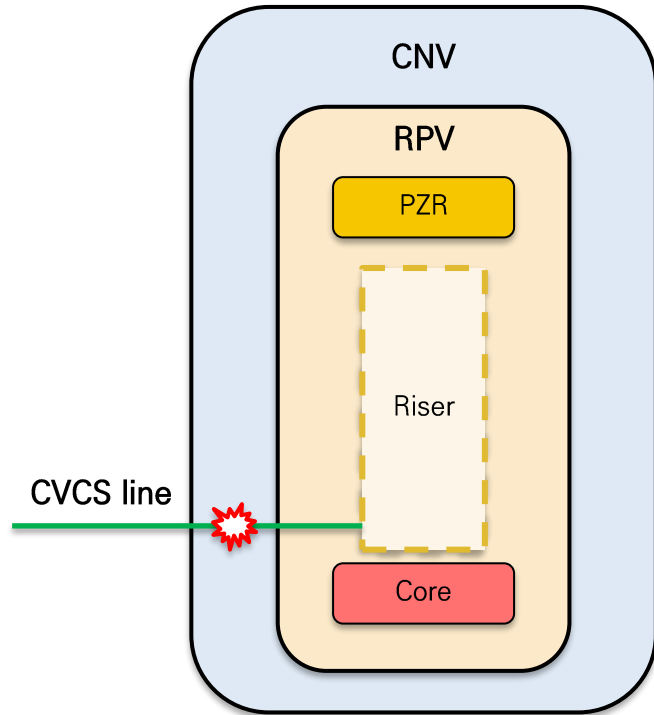
Methodology – CAFT Model



Applicability of CAFT model in Hydrogen-rich conditions

- Validation: FITS experiment
- Flame temperature deviation < 12% ($|T_{CAFT} - 1160K| \leq \sim 140K$)
- UFL prediction deviation < 15%

Methodology – SMR SA Scenario



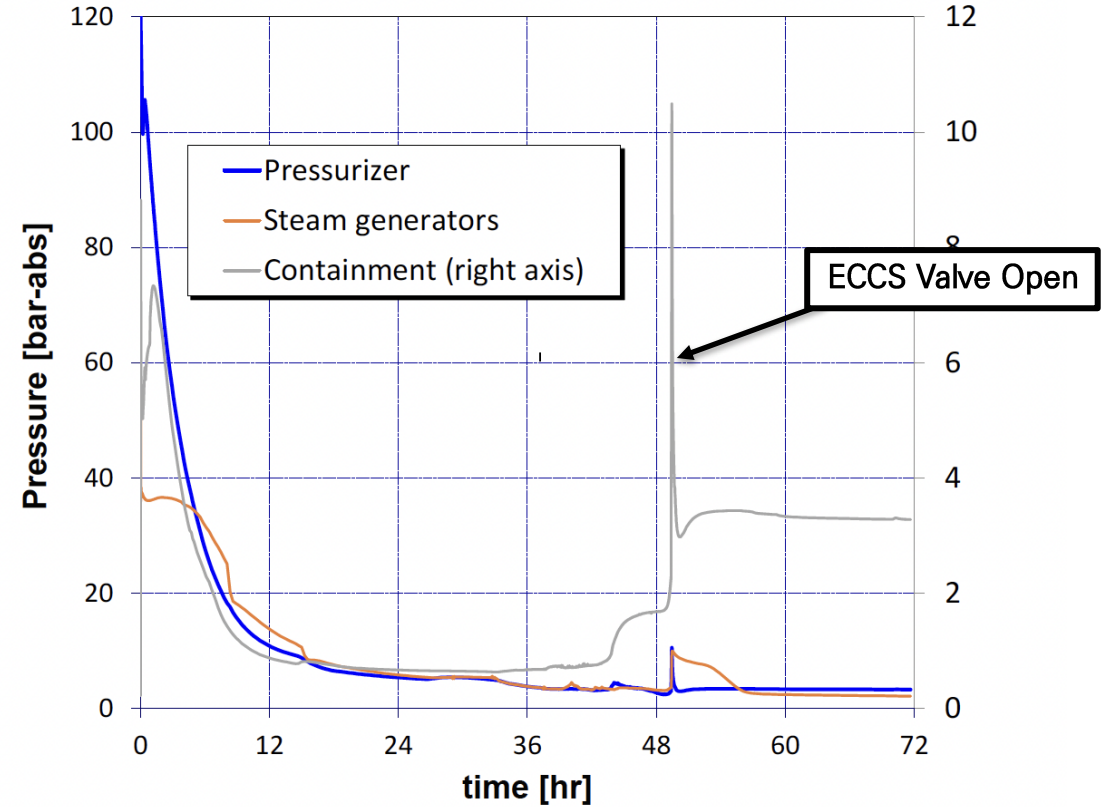
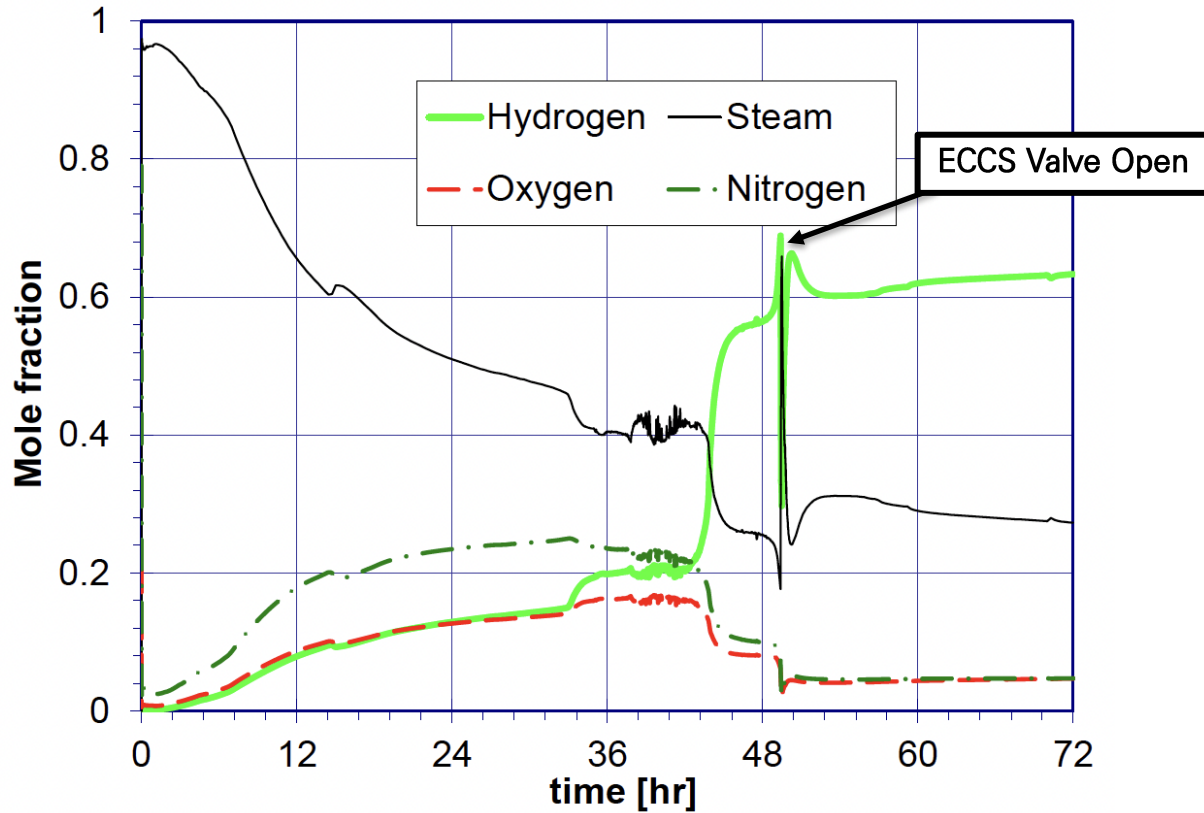
Time	Event
$t = 0$	CVCS pipe rupture
$t \approx 30$ h	Core uncover
$t = 49.38$ h	ECCS valves forcibly opened (Core reflood)
$t = 49.38$ – 72 h	Radiolytic O_2 accumulation
$t = 72$ h	$O_2 \approx 5$ mol%

NuScale SMR Severe Accident Scenario (LCC-05T-03)

- **Initiating event:** CVCS line rupture inside the CNV → reactor coolant directly released into the containment volume
- **Key features:** Closed, single-volume CNV (no gas exchange with environment) → Long-term radiolytic O_2 source persists even after oxidation ceases → Initially H_2 -rich condition

[1] Assessment of Hydrogen Combustion During Severe Accidents in a NuScale Plant Module, ERI/NRC 18-202, 2019

Methodology – SMR SA Scenario



Since no graph data was provided for the gas temperature, the gas temperature value of 369.65K available in the report was used.

[1] Assessment of Hydrogen Combustion During Severe Accidents in a NuScale Plant Module, ERI/NRC 18-202, 2019

Table of Contents

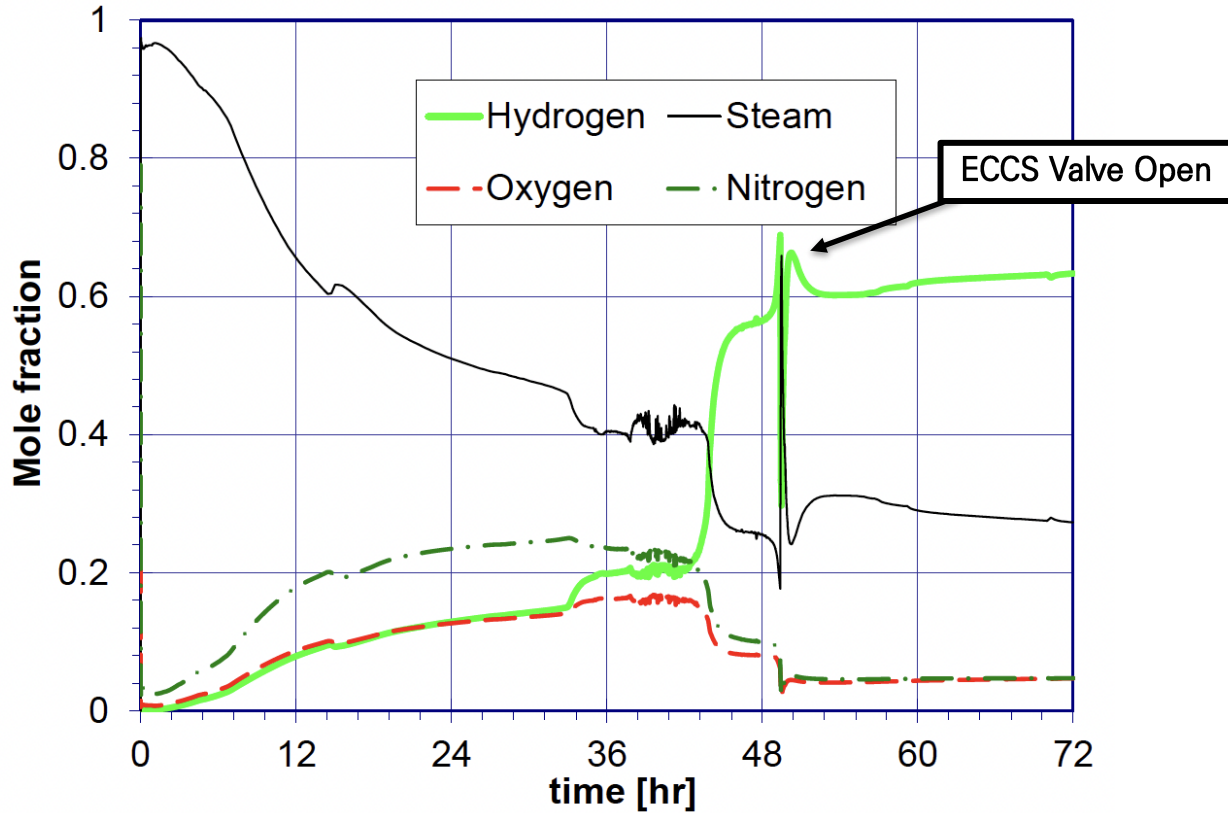
※ PART 1 – Introduction

※ PART 2 – Methodology

※ PART 3 – Result

※ PART 4 – Conclusion

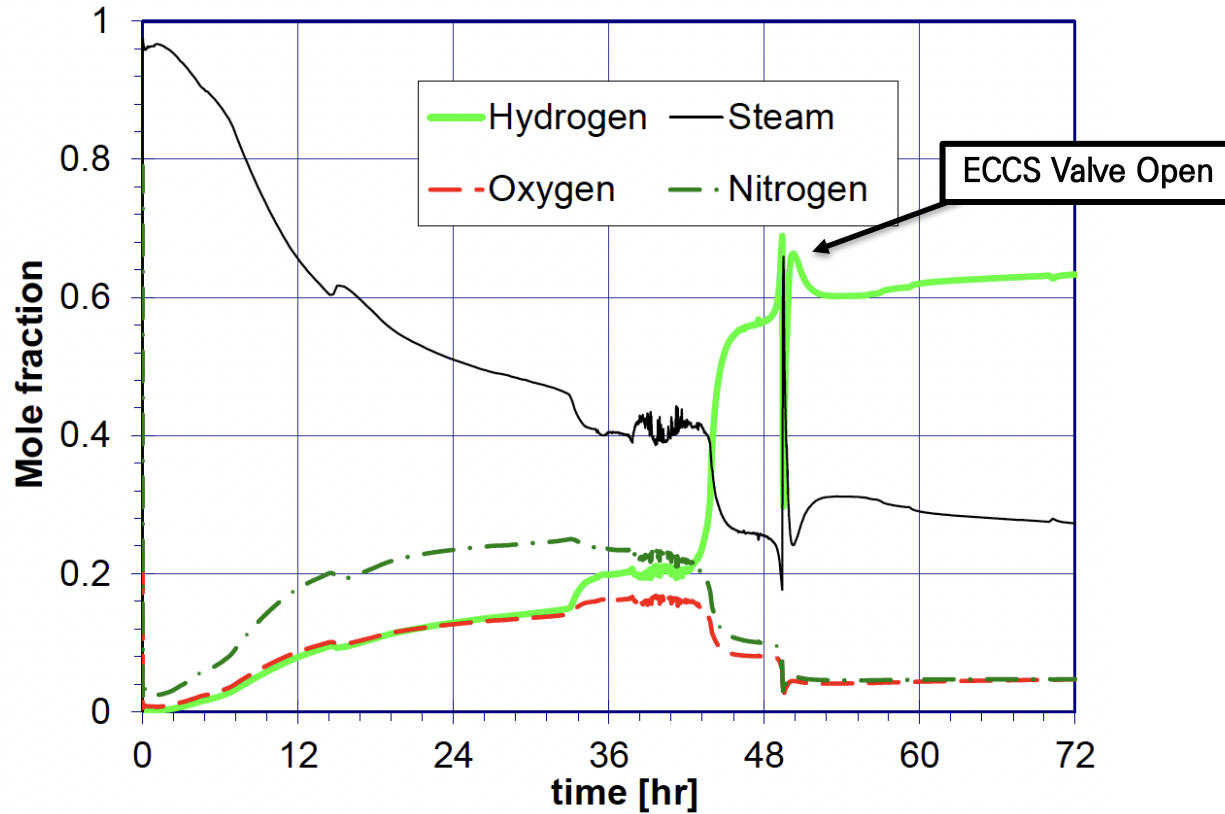
Result



Hour	H ₂ O (%)	H ₂ (%)	O ₂ (%)	N ₂ (%)	P (Pa)
44	31.42	44.98	10.43	13.63	113044
46	26.13	55.20	8.25	10.52	161535
48	25.38	56.54	8.11	10.01	168244
50	24.41	66.30	4.44	5.04	300857
54	31.19	60.17	4.11	4.58	343244
60	29.01	62.02	4.34	4.76	333842
66	27.98	62.77	4.58	4.76	330569
72	27.37	63.28	4.67	4.86	328967

[1] Assessment of Hydrogen Combustion During Severe Accidents in a NuScale Plant Module, ERI/NRC 18-202, 2019

Result



Hour	Flame Temperature(K)	Flammability
44	1834.52	O
46	1552.52	O
48	1536.48	O
50	1006.03	X
54	943.93	X
60	981.62	X
66	1017.81	X
72	1032.57	X

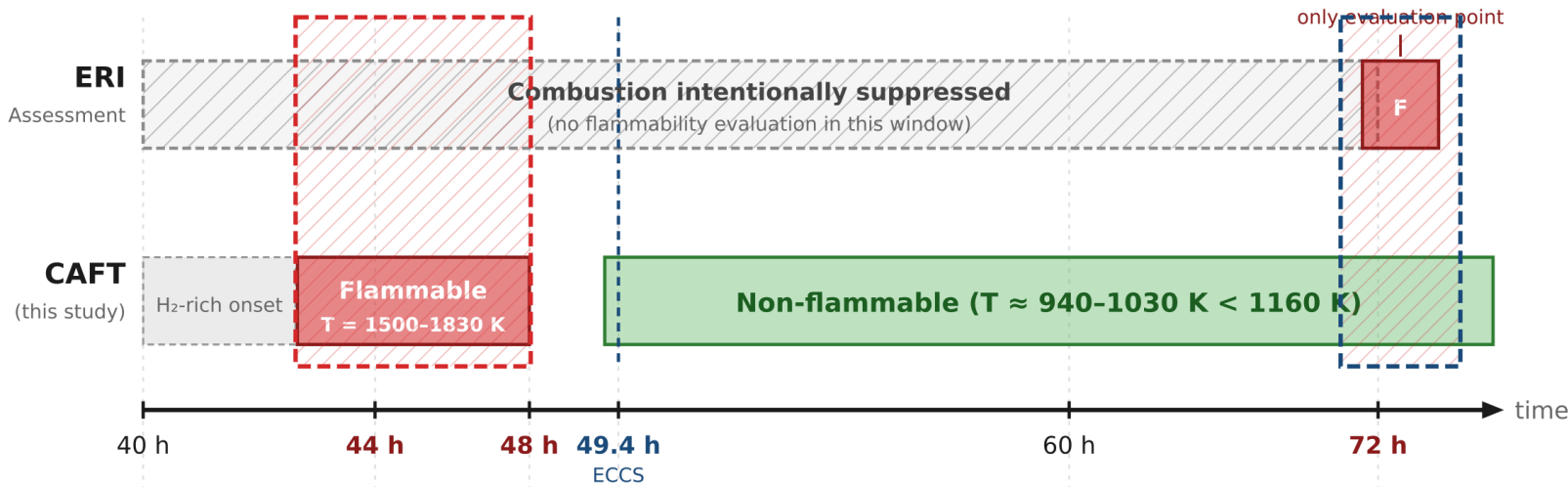
[1] Assessment of Hydrogen Combustion During Severe Accidents in a NuScale Plant Module, ERI/NRC 18-202, 2019

Result



ERI vs. CAFT — Filling the Gap in Flammability Assessment

Same LCC-05T-03 transient data, different evaluation scopes



★ **Newly identified window**
 ERI: not evaluated (suppressed)
 CAFT: **flammable** (O₂ ≈ 8%, low steam)

◆ **Reassessment of 72 h**
 ERI: flammable (O₂ = 5%, direct calc)
 CAFT: **non-flammable** (steam dilution)

Key Insights

- ERI's own MELCOR transient shows O₂ ≈ 8 mol% at 44–48h, but combustion in this window was intentionally suppressed and never evaluated
- CAFT applied to the same MELCOR data identifies 44–48h as **the actual high-risk window** — while the 72 h "worst case" lacks combustion energy due to post-ECCS steam dilution

Note

The 44–48 h window already exceeds ERI's own 5 mol% O₂ threshold. Its omission from the ERI assessment likely reflects the scenario framing.

Table of Contents

※ PART 1 – Introduction

※ PART 2 – Methodology

※ PART 3 – Result

※ PART 4 – Conclusion

Conclusion

- **Hydrogen-rich flammable window identified** At $t = 44\text{--}48$ h: The CAFT-predicted flame temperature exceeds **1500 K** — well above the 1160 K threshold. This window lies outside ERI's evaluation scope.
- **Reassessment of the 72 h “worst-case”**: Post-ECCS steam dilution lowers flame temperature to ~ 1030 K at 72 h, falling below the combustion threshold despite O_2 reaching 5 mol%.
- **Methodological implication**: Single-concentration criteria ($\text{O}_2 \geq 5\%$) may **underestimate transient risk** and **overestimate steady-state risk**. The CAFT model provides a thermodynamically rigorous, energy-based framework for SMR hydrogen risk assessment.
- **Future work**
 - CFD analysis of ECCS-induced gas mixing
 - Heat loss consideration at the UFL
 - Extension to i-SMR

Acknowledgment



This work was supported by the Regulatory Research Management Agency for SMRs (RMAS) and the Nuclear Safety Research Program through the Korea Foundation of Nuclear Safety (KoFONS) using the financial resource granted by the Nuclear Safety and Security Commission (NSSC) of the Republic of Korea (Nos. RS-2024-00509653, RS-2024-00403364).



**Thank You.
Any Questions?**

Sihyeong Yu*

Undergraduate Internship

NINE Lab,

Department of Quantum System Engineering,

Jeonbuk National University

tlgud02@jbnu.ac.kr