

## Effect of Temperature on Electrochemical Catalytic Decomposition of H<sub>2</sub>O<sub>2</sub> on UO<sub>2</sub>

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### 1. Introduction

Spent nuclear fuel is safely and permanently disposed of in deep geological environments. However, various safety scenarios are reviewed to ensure its safe management. Dissolution of spent nuclear fuel in groundwater exposure is a critical consideration from the perspective of radioactive material dispersal. Uranium oxide (UO<sub>2</sub>) is oxidized by H<sub>2</sub>O<sub>2</sub>, a radiolysis product of water. When uranium (IV) oxide oxidized to U(V) or U(VI) oxides, uranium readily dissolves in groundwater through the formation of carbonate/bicarbonate complexes. [1].

However, unlike UO<sub>2</sub>, spent nuclear fuel possesses oxygen vacancies due to lanthanide doping, and a small grain size. The oxidation of spent nuclear fuel by H<sub>2</sub>O<sub>2</sub> is significantly suppressed. Furthermore, H<sub>2</sub>O<sub>2</sub> decomposition is promoted by ε-particles (noble metal inclusions), so oxidation rarely occurs. The underlying mechanism for this oxidation inhibition is the decomposition of H<sub>2</sub>O<sub>2</sub> on the UO<sub>2</sub> surface. In other words, the redox reaction between UO<sub>2</sub> and UO<sub>2+x</sub> is understood to act as a catalyst for H<sub>2</sub>O<sub>2</sub> decomposition [2].

The decomposition of H<sub>2</sub>O<sub>2</sub> is influenced by various factors such as temperature, H<sub>2</sub>O<sub>2</sub> concentration, and catalytic surface properties [3]. In this study, the effect of temperature on the electrochemical catalytic behavior of UO<sub>2</sub> was investigated. After confirming that UO<sub>2</sub> can act as a catalyst for H<sub>2</sub>O<sub>2</sub> decomposition at room temperature based on redox potential analysis, its catalytic feasibility up to 100°C was evaluated by comparing temperature-dependent reduction potentials.

### 2. Methods and Results

#### 2.1 Analysis Condition

The oxidation reaction of UO<sub>2</sub>, which acts as a catalyst in groundwater, should be considered as oxidation to UO<sub>2+x</sub> (0 < x < 0.33), but since it is

difficult to obtain thermodynamic data for the corresponding compound, UO<sub>2+x</sub> was conservatively approximated by assuming x = 1 for the purpose of potential estimation. In addition, the pH was assumed to be pH 9 considering the groundwater conditions. The pH at high temperatures should be calculated by considering the high-temperature dissociation and decomposition of carbonates. However, for simplicity, the high-temperature pH was estimated by applying a constant offset to the neutral pH of water at each temperature.

#### 2.2 Analysis Methods

For the reduction potentials of H<sub>2</sub>O<sub>2</sub> to H<sub>2</sub>O and O<sub>2</sub> to H<sub>2</sub>O<sub>2</sub> at 25°C, commonly known values were used. The potentials for the onset of reduction and oxidation of H<sub>2</sub>O<sub>2</sub> at high temperatures were calculated by applying the chemical potential values at room temperature and the temperature-dependent heat capacity (C<sub>p</sub>) values to the Linear Ionic Heat Capacity Approximation (LIHCA) method [3]. The chemical potential and heat capacity data of the compounds involved in the analysis were used from reported data [4]. Since the oxidation and reduction reactions of H<sub>2</sub>O<sub>2</sub> and the redox reactions of UO<sub>2</sub>/UO<sub>2+x</sub> (x = 1 assumption), which are the considered reactions, have the same potential shift according to pH change at each temperature, the potential comparison was made based on pH 0 at each temperature.

#### 2.3 Potential shift comparison for temperature change

For UO<sub>2</sub> to act as an electrochemical catalyst for the H<sub>2</sub>O<sub>2</sub> decomposition reaction, both the oxidation of UO<sub>2</sub> and the reduction of UO<sub>2+x</sub> by H<sub>2</sub>O<sub>2</sub> must occur. As mentioned earlier, due to the lack of thermodynamic data, the analysis temporarily used data for UO<sub>2+1</sub> by assuming x = 1. While the data was used conservatively, it should be noted that in real systems, once UO<sub>2</sub> is oxidized to UO<sub>2+1</sub>, it is not

reduced back to  $\text{UO}_2$  by a reducing agent.

For the continuous oxidation of  $\text{UO}_2$  and the reduction of  $\text{UO}_{2+x}$  by  $\text{H}_2\text{O}_2$  to  $\text{UO}_{2+x}$  must occur spontaneously, and the reduction of  $\text{UO}_{2+x}$  to  $\text{UO}_2$  must also occur spontaneously. Therefore, the redox potential of  $\text{UO}_2/\text{UO}_{2+x}$  must be lower than the reduction potential of  $\text{H}_2\text{O}_2$  and higher than the oxidation potential of  $\text{H}_2\text{O}_2$ .

Figure 1 shows the reduction potential of  $\text{H}_2\text{O}_2$ , the oxidation potential of  $\text{H}_2\text{O}_2$ , the starting potential of  $\text{H}_2\text{O}_2$  oxidation, and the redox potential of  $\text{UO}_2/\text{UO}_{2+1}$  over the temperature range of  $25^\circ\text{C}$  to  $100^\circ\text{C}$ . Each potential value was calculated for the  $\text{pH} = 0$  condition. Since the  $\text{pH}$  at  $25^\circ\text{C}$  was set to 9,  $\text{pH}$  corrections at each temperature were necessary. However, since the potential shift due to  $\text{pH}$  change is constant at  $(2.303 \cdot \text{RT}/\text{F}) \cdot \Delta\text{pH}$  for all three reactions at a constant temperature, the potentials at  $\text{pH} 0$  for the corresponding temperatures were compared with each other.

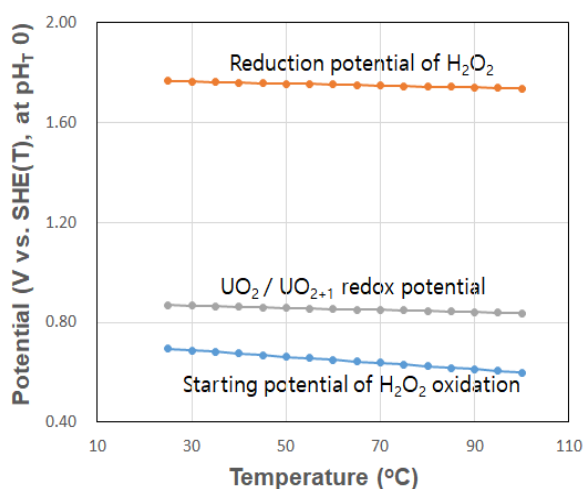


Fig. 1. Changes in reduction potential (vs. SHE(T)) with temperature. Reduction potential of  $\text{H}_2\text{O}_2$  (orange), reduction potential of  $\text{UO}_{2+1}$  (to  $\text{UO}_2$ ) (grey), reduction potential of  $\text{O}_2$  (to  $\text{H}_2\text{O}_2$ ) (blue).

As temperature increases, the redox potential of  $\text{UO}_2/\text{UO}_{2+x}$  ( $x = 1$ ) decreases slightly, but remains consistently between the potentials at which  $\text{H}_2\text{O}_2$  reduction and oxidation reactions begin in the temperature range of  $25^\circ\text{C}$  to  $100^\circ\text{C}$ . This suggests that the  $\text{UO}_2$  surface can act as an electrochemical catalyst for  $\text{H}_2\text{O}_2$  decomposition within this temperature range.

Meanwhile, the temperature-dependent potential slope for the  $\text{H}_2\text{O}_2$  oxidation reaction was evaluated to decrease slightly more steeply with increasing temperature than the other two reactions. This

reaction ( $\text{H}_2\text{O}_2 \rightarrow \text{O}_2 + 2\text{H}^+ + 2\text{e}^-$ ) is different from other reactions in that it generates gas ( $\text{O}_2$ ). This behavior can be attributed to the additional entropy contribution associated with  $\text{O}_2$  gas formation, which affects the temperature dependence of the Gibbs free energy of the reaction.

### 3. Conclusions

Thermodynamic comparison of temperature-dependent reduction and oxidation potentials indicates that the  $\text{UO}_2$  surface can function as an electrochemical catalyst for  $\text{H}_2\text{O}_2$  decomposition in the temperature range of  $25^\circ\text{C}$ – $100^\circ\text{C}$ . The slightly steeper temperature dependence observed for the  $\text{H}_2\text{O}_2$  oxidation reaction is attributed to the positive entropy contribution associated with  $\text{O}_2$  gas formation.

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