UVC Photo-Fenton Decomposition behavior of oxalic waste depending on H₂O₂ and iron catalyst for NPP chemical decontamination

Saifur Rahman^{1*}, Dohyeon Kim¹, Sang-June Choi^{1,2*}, Wonzin Oh^{2*}, Jeong-joo Kim³, Cho-Rong Kim³, Ki-Chul Kim⁴, 1School of Architectural, Civil, Environmental, and Energy Engineering, Kyungpook National University, 80 Daehak-ro, Buk-gu, Daegu 41566, Republic of Korea

2Research Institute of Advanced Energy Technology, Kyungpook National University, 80 Daehak-ro, Buk-gu, Daegu 41566,

Republic of Korea

3KHNP Central Research Institute, 70, Yuseong-daero 1312beon-gil, Yuseong-gu, Daejeon, Republic of Korea

4KEPCO KPS, 96-1 Gilchon-Gil, Jangan-Eup, Gijang-Gun, Busan, Republic of Korea

*Corresponding author: wonzin@knu.ac.kr; sjchoi@knu.ac.kr

1. Introduction

This is a study on the decomposition of oxalic acid waste

generated from the NPP chemical decontamination. The previous study on UVC photo-Fenton decomposition of oxalic acid (Jinhee Kim, wonzin Oh et al, NET 51, 2019) showed that the type of UV lamp and the irradiance density in terms of applied UVC energy irradiation/per volume,[kw*irradiation time/L] are important factors in simulation of the decomposition performance. The decomposition behavior of oxalic acid were studied as a function of H_2C_2 and iron catalyst concentration using a medium pressure UV lamp. Furthermore, the concentration ratio of H_2O_2 and iron catalyst was also investigated experimentally.

2. Methods and Results

2.1 Method



Figure 1 Photo-reactor schematic for photo-Fenton treatment

The Fig 1 showed the experimental system for UVC Photo-Fenton decomposition of the oxalic waste. The decomposition behavior of oxalic waste depending on the amount of UVC energy applied were studied by varying the amount of hydrogen peroxide and iron(2+) catalyst together with its ratio. Table 1 showed the typical experimental condition in the study. As an iron catalyst FeCl2 was used in study. Residual concentration of H2C2O4 with reaction time was measured by TOC analyzer (TOC-V CPH, SHIMADZU, JAPAN).

2.2 Materials

Ferrous chloride (FeCl₂-4H₂O, Min. 99%), oxalic acid (H₂C₂O₄-2H₂O, Min. 99.5~100.2%), and hydrogen peroxide (H₂O₂, Min. 28%) were purchased from DAEJUNG company Korea. The size of UV reactor was 3L, waste volume 6L, Circulation rate 400ml/min, Reactor residence time 240 (min).

2.3 Results

In the previous study, the UVC decomposition behavior of oxalic acid was shown to be a first-order reaction of the oxalic acid concentration depending on the applied UVC energy density as follows:

 $\begin{array}{l} - dC_Ox / d\eta = k^* C_Ox, \text{ ic: } C_Ox(0) = Co_Ox \\ C_Ox(\eta) = Co_Ox^* exp(-0.693/kh^*\eta), \\ \text{where } kh = 0.693/k \text{ is half decomposition energy} \\ \text{density.....} \end{array}$

The table 1 and Fig 2 is an typical example of experimental condition and its simulation result using Eq(1) which shows that the decomposition reaction constant in terms of kh is 3.2[kJ/L] and R² is 0.99.

C_H2O2 =80 mM/L , Co_ox = 40[mM/L] , C_Fe(2+)=2 mM/L, with a random sampling time interval .								
Time [min]	Roh_UV= Kw*T/V,[kJ/L]	рН	C_H ₂ C ₂ O ₄ [mmol/L]	Residual (%) by TOC	C_Fe ²⁺ [mmol/L]	C_H+ [mmol/L]	TOC PPm	Residual[%] by Oh's model with Th=3.2
time[min]	Roh_UV			Resd_TOC[%]				Resd_Model[%]
0.00	0	2.08	32.9	100.0	2	8.31	788.5	100.00
10.00	3.96	2.12	14.6	44.5	2	7.58	350.6	42.42
20.00	7.92	2.25	12.9	39.4	2	5.62	310.5	17.99
40.00	15.84	2.49	12.3	37.5	2	3.23	295.6	3.24
60.00	23.76	2.52	11.1	33.6	2	3.01	265.3	0.58
90.00	35.64	2.56	9.6	29.2	2	2.75	230.5	0.04
120.00	47.52	2.60	8.2	24.8	2	2.51	195.6	0.00
150.00	59.4	2.72	6.9	21.0	2	1.9	165.5	0.00
180.00	71.28	2.85	6.1	18.4	2	1.41	145.2	0.00
240.00	95.04	3.04	4.8	14.5	2	0.91	114.3	0.00

Table 1. Example of Oxalic Waste UVC Photo FentonDecomposition Experimental Condition



Fig. 2 UVC Photo Fenton Decomposition Performance Simulation Result of Table 1 Decomposition Condition



Fig. 3 Experimental result and its linear simulation of the applied energy density for half oxalate decom-position, kh[kJ/L], depending on C_H₂O₂/C_Ox at Co_Ox of 10,20,30,40 [mM/L] and C_Fe of 2[mM/L]

The above figure shows that the decomposition behavior of oxalic acid Waste in terms of half energy density is linearly correlated with the ratio of hydrogen peroxide to oxalic acid concentration and the correlation equation is as follows:

Th, $[kJ/L] = -53.82 * C_hp/C_ox +113.5$ with R² of 0.97.....(2)



Fig. 4 Effect of half decomposition energy density depending on Fe(2+) catalyst concentration at C_ox of 10 and 20 [mM/L]

The Fig. 4 shows that the decomposition half energy density is not affected of increase of Fe(2+) concentration more than 2[mM/L], while at C_Fe(2+)<2 [mM/L], the decomposition half energy

density increase by decrease of C_Fe(2+) up to almost two times.

4. Conclusion

The following conclusions were obtained for oxalate decomposition behavior by UVC Photo-Fenton depending on H_2O_2 , $H_2C_2O_4$, and Fe^{2+} Concentration.

- 1. The decomposition rate in terms of half decomposition time constant of th was drastically increased depending on increase of the ratio of C-Hp/C-ox up to 2 where th approaches to zero.
- The concentration of Fe²⁺ as a catalyst take a role to increase the decomposition rate of oxalic acid waste, but increase of Fe²⁺ concentration more than 2[mM/L] do not increase the decomposition rate.

ACKNOWLEDGEMENT

This work was supported by the Korea Institute of Energy Technology Evaluation and Planning (KETEP) (No. 20191510301310)

REFERENCES

[1] Eung-Ho Kim et al., "Decomposition of oxalic acid by UV irradiation in nitric acid"-RXUQDORI Journal of the Korean Industrial and Engineering Chemistry, 8(1), 108-113 (1997).

[2] Dong-Yun Ha et al., "Study of decomposition characteristic of oxalic acid and citric acid by UV/H2O2", Journal of Korean Society of Environmental Engineers, 22(7), 1307-1318 (2000).

[3]Kim, J.-H., Lee, H.-K., Park, Y.-J., Lee, S.-B., Choi, S.-J., Oh, W., Kim, H.-S., Kim, C.-R., Kim, K.-C., Seo, B.-C., 2019. Studies on decomposition behavior of oxalic acid waste by UVC photo-Fenton advanced oxidation process. Nuclear Engineering and Technology 51, 1957-1963.