

## Measurement of the Heat Load Imposed on the Reactor Vessel Depending on the Crust Layer in a Severe Accident

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### 1. Introduction

In an In-Vessel Retention and External Reactor Vessel Cooling (IVR-ERVC) situation, the molten corium in the oxide pool may be solidified and form a crust layer along the oxide layer boundary. This changes thermal boundary and geometrical condition of the oxide pool which may affect natural convection heat transfer of the oxide pool [1]. However, only a few studies [2,3] were performed regarding the crust layer. We measured the mean  $Nu$  imposed to reactor vessel and local heat flux and comparative analyses were performed between the crust free and crust conditions with a few different thicknesses depending on the decay heat.

### 2. Experimental set up

#### 2.1 Experimental methodology

Heat and mass transfer systems are analogous. This means that the governing equations of two systems are mathematically the same. Thus, the heat transfer problems can be solved by the mass transfer experiments [4].

The limiting current technique, a method of measurement, is used by the mass transfer system and developed by several researchers [5–8], and this methodology is now well-established [9–11].

By using the mass transfer system, we could achieve high  $Ra'_H$  with compact test rigs, ideally isothermal cooling condition and uniform heat generation.

Because internal flow towards bottom of the test rig is formed in heat transfer, anode could simulate as cold wall in mass transfer. But, the current is not measured in anode [12]. Therefore, we performed the tests using the inverted test rigs against the gravity direction and simulated the same internal flow.

#### 2.2 Phenomena modeling

To simulate the natural convection in the oxide pool, we assumed that the outer vessel wall is sustained as isothermal condition due to the ERVC and the temperature difference between inner and outer vessel wall was neglected to simplify modeling. Through these assumptions, the oxide pool boundary was simulated by an isothermal wall.

Thickness of the crust layer,  $\Delta x$ , is determined by the heat balance,  $q'' = -k(\Delta T/\Delta x)$ . The heat balance equations [13] and geometrical and thermodynamic

properties [13–15] were employed to estimate the crust layer thickness.

The temperature difference in the system is reduced by the crust layer. When the crust layer is formed, the temperature of the oxide pool boundary is changed into the melting temperature of the crust layer. In the mass transfer system, the temperature difference was replaced with the concentration difference.  $Da$  in the system was also changed by analogy. In the heat transfer system, the  $Da$  ratio ( $\Delta T_2/\Delta T_1$ ) was 0.130. In order to maintain the ratio, the working fluid concentrations were determined as 0.026 M for with crust and 0.2 M for without crust.

Table I listed the test matrix. It was confirmed that a semi-circular test rig with 0.1 m height can achieve  $Ra'_H$  of  $\sim 10^{15}$  in previous studies of our research group [9–11,16–21]. Based on this, the thicknesses of the crust layer were downscaled in mass transfer system.

Table I: Test matrix

Crust formation	Thickness (m)	$Ra'_H$	$Pr$
With crust	N/A	$9.51 \times 10^{14}$	2283
Without crust	0.003	$6.23 \times 10^{13}$	1979
	0.01	$4.79 \times 10^{13}$	
	0.03	$1.63 \times 10^{13}$	
	0.05	$3.97 \times 10^{12}$	

Figure 1 presents the test rigs, mass transfer experimental rig for a 2-D oxide pool with crust layer (MasSTER-OP2(CL)), which radius is 0.1 m. The width is 0.04 m, which is enough to neglect the effect of the side wall [22]. The copper cathodes were located along the inner surface. To check the influence of insulation layers among piecewise electrodes, halves of the inner surfaces consisted of a single electrode and the other halves consisted of piecewise electrodes for the local currents measurement. The curved surface consisted of nine piecewise electrodes, and eight along the top plate. To simulate the internal heat source, copper anodes were attached at both sides. Copper sulfate-sulfuric acid ( $\text{CuSO}_4\text{-H}_2\text{SO}_4$ ) solution was used as a working fluid.

Figure 2 presents the experimental circuit. A power supply (K1810 of Vüpower) and data acquisition system (NI-9225, NI-9227 of National Instruments) was used.

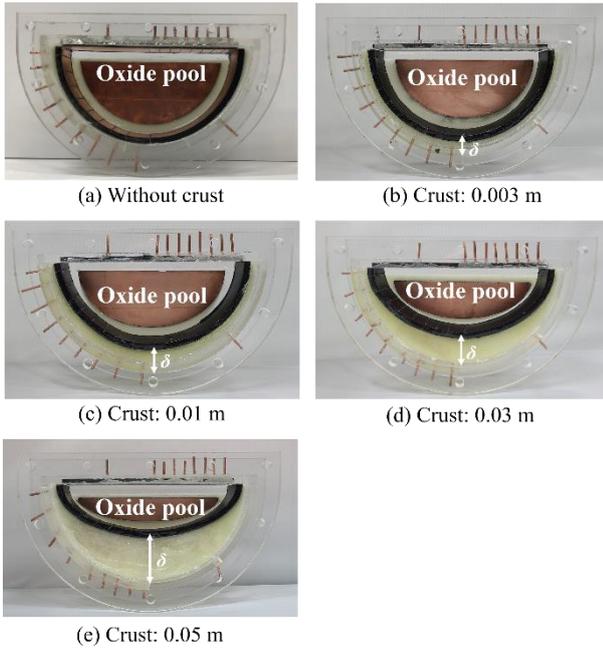


Fig. 1. Test rigs.

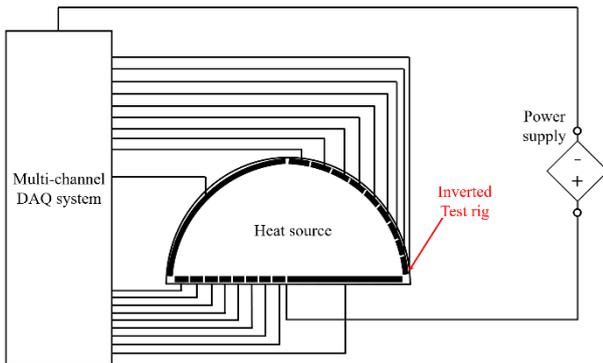


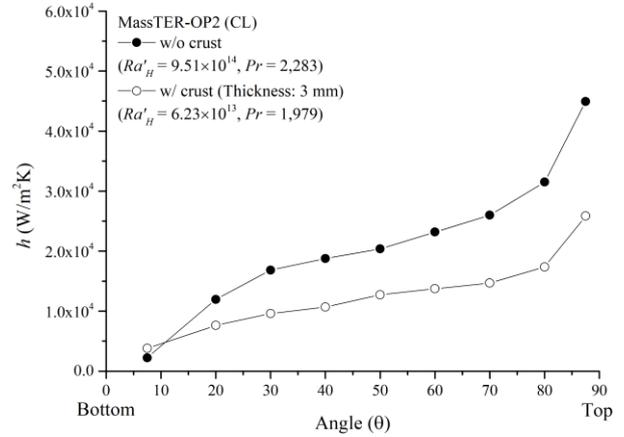
Fig. 2. Experimental circuit.

### 3. Results and Discussion

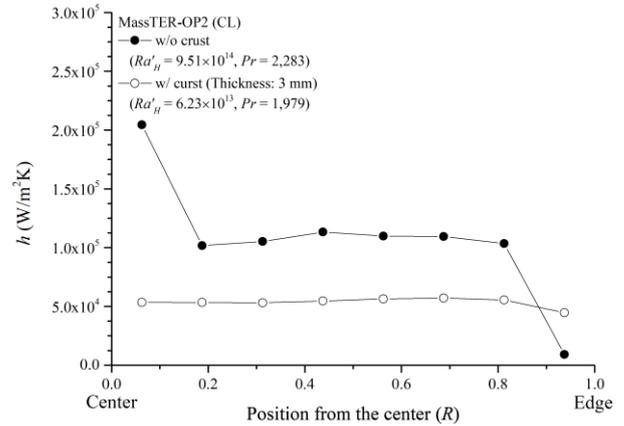
Figure 3(a) presents the local heat transfer coefficient ( $h_{loc}$ ) measured along the curved surface for both conditions. The  $h_{loc}$  values in without crust layer condition were greater than those in with crust layer condition because the crust layer works as the thermal insulator.

Figure 3(b) shows the  $h_{loc}$  values of the top plate. The  $h_{loc}$  values in without crust layer condition were greater than those in with crust layer condition as more heat is imposed to top plate because of insulation effect of the crust layer. In without crust condition, the  $h_{loc}$  values had a peak at the center. The rising plume from the bottom of the curved surface improved the  $h_{loc}$  at the center of the top plate. Meanwhile, monotonic shape of  $h_{loc}$  was observed in the with crust condition. This seems to be induced by the thermal boundary condition. In with crust layer condition, the temperature difference is decreased and  $Ra'_H$  decreased from  $9.51 \times 10^{14}$  to  $6.23 \times 10^{13}$ . Hence, the buoyancy of the rising plume was reduced and a side

flow was generated before it arrives at the top plate in with crust condition. In all cases, the  $h_{loc}$  at the edge of the top plate showed very low heat transfer because the stagnant flow was generated.



(a) Local heat transfer coefficient at the curved surface

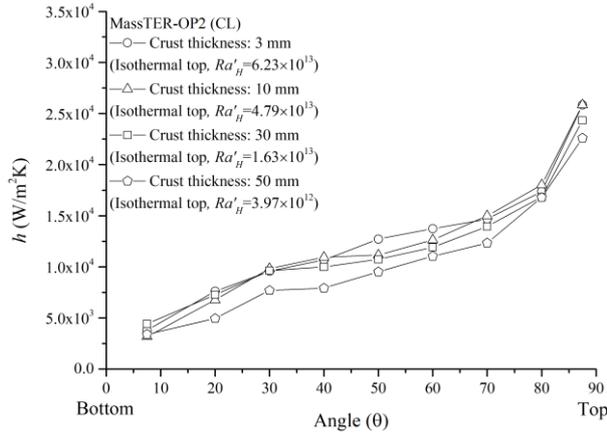


(b) Local heat transfer coefficient at the top plate

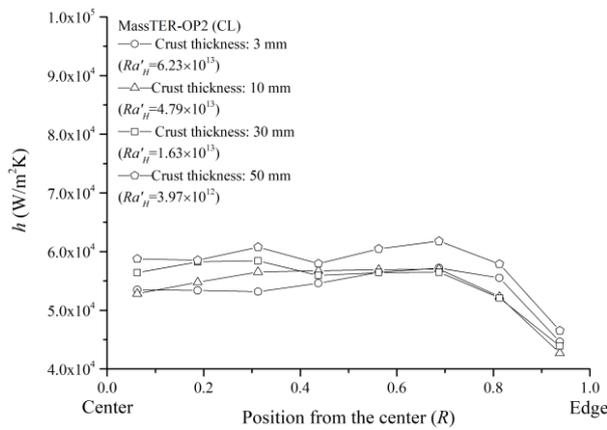
Fig. 3. Comparison of local heat transfer coefficient according to the crust existence.

Figure 4 presents the  $h_{loc}$  measured at the curved surface and top plate according to crust thickness. The  $h_{loc}$  values measured at the curved surface is reduced as the crust layer became thicker, as shown in Fig. 4(a). Because increase in crust thickness leads to decrease in  $Ra'_H$ , which leads to decrease in  $h_{loc}$ . Fig. 4(b) presents that the  $h_{loc}$  values measured at the top plate increased when the crust thickness increased as the downward cooling was decreased.

A comprehensive analysis was performed by comparing the  $h_{loc}$  values in Figs. 3 and 4 shows that the heat loads imposed on the reactor vessel are influenced by the crust layer. That the influence of the variation due to thermal boundary condition is more pronounced than that of the variation due to crust thickness.



(a) Local heat transfer coefficient at the curved surface



(b) Local heat transfer coefficient at the top plate

Fig. 4. Comparison of local heat transfer coefficient according to the thickness of crust layer.

#### 4. Conclusions

The natural convection heat transfer of the oxide pool when the crust layer was formed was simulated. Before the design of experiments, we conducted modeling for the crust situation. This is the originality of this study. We investigated the crust layer influence on the heat load imposed on reactor vessel in an IVR condition. The range of  $Ra'_H$  was  $10^{12} - 10^{15}$ .

When the crust layer is formed, thermal boundary condition of oxide pool is varied from the boiling temperature of the external coolant to the melting temperature of the oxide pool. The temperature difference of the system was decreased and the driving force was weakened.

The experimental results presented that the crust layer disturbed the heat transfer at the oxide pool as it works as the thermal insulator. The effect of crust layer thickness on the local heat transfer was small compared to effect caused by the formation of the crust layer. Thus the effect of the crust layer due to the variation of the thermal boundary condition was greater than the effect due to the crust thickness.

#### NOMENCLATURE

$Da$	Damköhler number ( $q'''H^2/k\Delta T$ )
$h$	Heat transfer coefficient [ $W/m^2 \cdot K$ ]
$h_{loc}$	Local heat transfer coefficient [ $W/m^2 \cdot K$ ]
$H$	Oxide pool height [m]
$k$	Thermal conductivity [ $W/m \cdot K$ ]
$Pr$	Prandtl number ( $\nu/\alpha$ )
$q''$	Heat flux [ $W/m^2$ ]
$q'''$	Volumetric heat generation rate [ $W/m^3$ ]
$R$	Position from the center
$Ra_H$	Rayleigh number ( $g\beta\Delta TH^3/\alpha\nu$ )
$Ra'_H$	Modified Rayleigh number ( $Ra_H Da$ )
$\Delta T$	Temperature difference of the system [K]
$\Delta T_1$	Temperature difference of the system in without crust condition [K]
$\Delta T_2$	Temperature difference of the system in with crust condition [K]
$\Delta x$	Crust layer thickness [m]

#### Greek symbols

$\alpha$	Thermal diffusivity
$\beta$	Volume expansion coefficient [ $1/K$ ]
$\delta$	Crust layer thickness of test rigs [m]
$\theta$	Angle [ $^\circ$ ]
$\nu$	Kinematic viscosity [ $m^2/s$ ]
$\rho$	Density [ $kg/m^3$ ]

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