Off-design performance of Supercritical CO₂ Power System for Waste Heat Recovery Application

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1. Introduction

As the global climate change becomes substantial, desire to attain efficient power system increases gradually. Power generation from the waste heat of conventional power system is another increasing market. Supercritical CO₂ cycle is gaining interests with several benefits: (1) high efficiency in the mild turbine inlet temperature range (450-650 °C), (2) simple layout configuration and (3) small foot print incorporated with compact heat exchangers and turbomachineries. On and off-design performance of supercritical CO₂ power system based on the component design variables is discussed in this paper.

2. Supercritical CO₂ Cycle and Performance Assessment

2.1 System and Component Design

Table I. Supercritical CO_2 cycle design condition			
Value			
85%			
80%			
7.739 MPa			
34.1 °C			
90%			
90%			
0.5% (cold side)			
1.5% (hot side)			
4%			
3%			
0.5% (each)			
Value			
70.5kg/s			
566 ℃			
35.5%			
61.6 MWth			
39.7 MWth			

Table I. Supercritical CO₂ cycle design condition

Preliminary design of supercritical CO_2 recuperated for waste heat recovery system is suggested in Table 1 and Fig. 1. The heat source is LM-2500. The compressor inlet condition of supercritical CO_2 cycle is controlled close to the critical point (30.98°C, 7.3773MPa) due to the low compression work. The design variables and operating condition for the supercritical CO_2 cycle is discussed in previous work [1]. With the design variables for the supercritical CO_2 cycle, the sensitivity study of pressure ratio and mass flow rate is conducted and the maximum pressure and flow rate are selected as 20 MPa and 115 kg/s, respectively.



Fig. 1. Simple recuperated layout



Fig 2. Supercritical CO_2 cycle T-s diagram Table II. Supercritical CO_2 cycle T-s diagram

Table II. Supercritical CO ₂ Cycle 1-8 diagram			
Layout	Simple recuperated	Cycle mass flow rate, kg/s	115
Heat in (WHR HX), MW	25.4	Heat out (Precooler), MW	19.7
Heat recuperated (Recuperator), MW	27.3	HX UA, kW/K (WHE / Recuperator, PC)	887.8
Compressor work, MW	3	Exhaust gas Tout, °C	205
Turbine work, MW	8.7	Cycle efficiency, %	22.50

For supercritical CO_2 cycle application, printed circuit heat exchanger (PCHE) in Fig. 3. is widely used for high compactness and wide operational range.

In-house code for PCHE design is developed in previous work [2]. The preliminary design of $S-CO_2$ heat exchangers is shown in Table III.

Based on the pre-designed off-design map of supercritical CO_2 turbine and compressor, on-design

and off-design performance is assessed shown in Fig. 4 and Fig. 5.



Fig. 5. Supercritical compressor performance map

2.2 Off-design performance of supercritical CO2 cycle



Fig. 6. Off-design performance analysis code algorithm

With the preliminary component design and performance parameters, off-design performance analysis code is developed and the code algorithm is shown in Fig. 6. The thermal efficiencies are predicted for the compressor inlet temperature variation as shown in Fig. 4. As the compressor inlet temperature decreases, the thermal efficiency increases.

Off-design performance with the variation of cooling water temperature change is shown in Fig. 7. As the cooling water temperature increases, the cycle mass flow rate and thermal power decreases.



Fig. 7. Off-design performance with cooling temperature variation

3. Summary and further works

Supercritical CO_2 power system for waste heat application is designed to generate marginal power from the flue gas of a conventional gas turbine. The cooling temperature of the area can influence the compressor inlet temperature. To estimate the S-CO₂ cycle performance for various environmental conditions, offdesign performance analysis code is developed.

Further works are required to predict performance under the condition of gas turbine part load and cooling water flow change.

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References

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