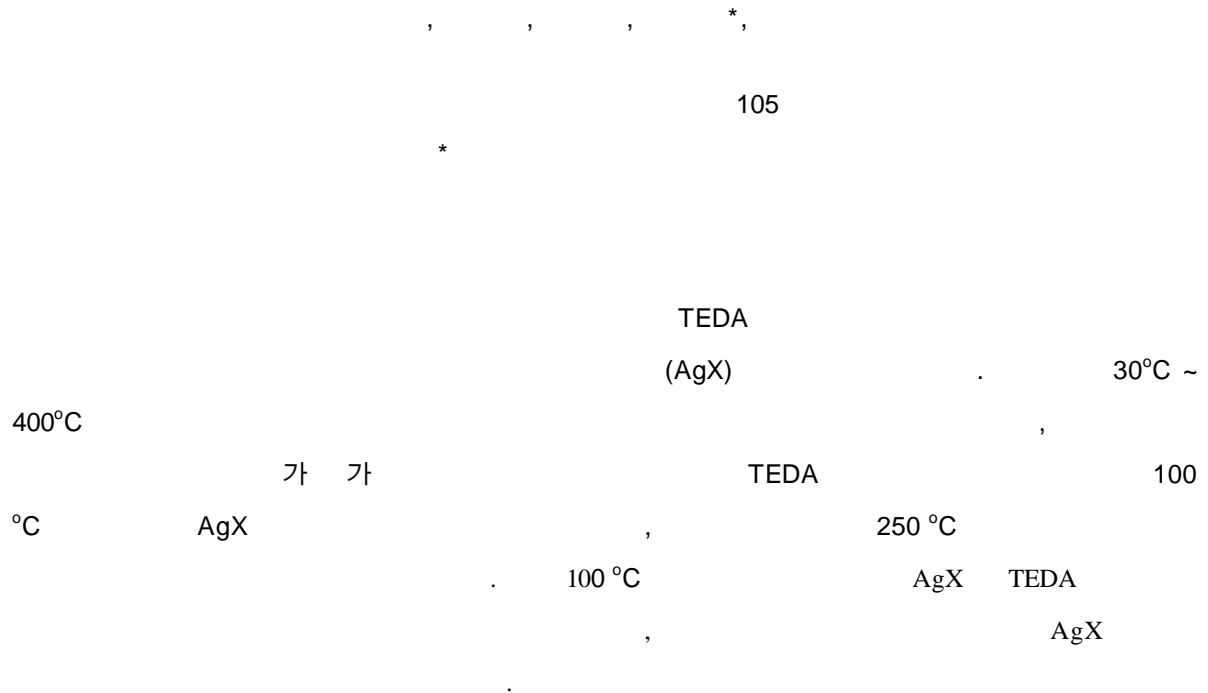


TEDA

Comparison of Removal Efficiency of Organic Iodide Using Silver Ion-exchanged Synthetic Zeolite with TEDA-Impregnated Activated Carbon at High Temperature



Abstract

Removal efficiency of methyl iodide at high temperature process by TEDA-impregnated activated carbon used for radioiodine retention in nuclear facility was experimentally compared with that of silver ion-exchanged synthetic zeolite(AgX). In temperature ranges of 30°C to 400°C, adsorption capacity of un-impregnated carbon was sharply decreased, but TEDA-impregnated carbon showed similar values of adsorption capacity of AgX even around 100°C. Especially, loading amount of methyl iodide on TEDA carbon up to 250°C represented higher values compared to un-impregnated carbon. Breakthrough curves of methyl iodide in fixed bed packed with AgX and TEDA-impregnated carbon at high temperature was compared. Removal mechanism of methyl iodide on AgX was proposed, based on analysis of by-product gas generated from adsorption reaction.

1.

가
가
[1~5].
()
가 Spray 가 가 KI
TEDA [2, 5].
DUPIC I-129
TEDA
가
가
() 가 (13X
(AgX) 가

[6~8].

TEDA
가
10wt% (AgX-10wt%)

2.

TEDA
13X Aldrich(USA) 13X 가
8~16 mesh sieving

13X

TEDA

[9],

TEDA

6.5 wt%

(AgX) AgNO₃

13X가

3

AgNO₃

24

13X

2~3

24

120

AgX

AgNO₃

(ml)/

(g)

1 ~ 1.2

AgX

가

1

가

pyrex glass

GC

GC

가

70

가

18mm,

22mm,

700mm

Pyrex

가

GC

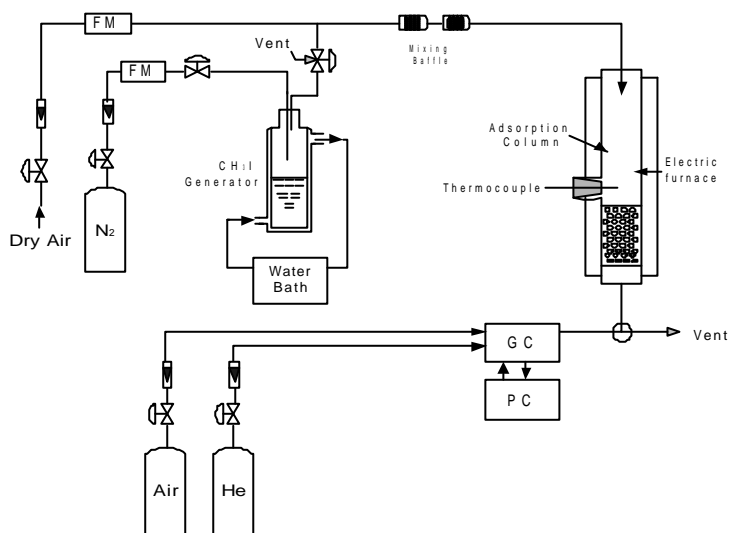
1

Fig. 1. Flow diagram of the experimental apparatus.

Table 2.

GC

Experimental parameters	Operating conditions	Remarks
Process flow (l/min)	4.0	
Superficial velocity (cm/sec)	26	
Bed depth (cm)	2.6 ~ 10	
Input concentration (mol/l)	$10^{-6} \sim 10^{-4}$	
Gas generator temperature (°C)	5 ~ 30	
Bed temperature (°C)	30 ~ 400	
Relative humidity (%)	Dry	Process air
GC analysis conditions		
- Capillary column	GS-Q	* Pulse Discharged Detector
- Detector	PDD*	
- Carrier gas(He) flow rate (ml/min)	6	
- Oven temperature (°C)	140	
- Detector temperature (°C)	160	
- Auto sampler volume (ml)	1.0	
- Sampling interval (min)	5	



3.

, 30 ~ 250

, 13X TEDA

AgX-10wt%

2

가

3

2

가 가

, 70

TEDA

가 가

, AgX-10wt%

, 100

가 가

TEDA

가가

,

TEDA

가

TEDA-

75

, TEDA

250

100

AgX-10wt%

TEDA

30%

150

TEDA

가

가가

가

AgX-10wt%

4~5

, 가 가

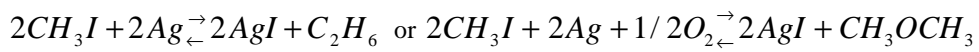
, 400 °C

Ag

CO₂가

(6, 7).

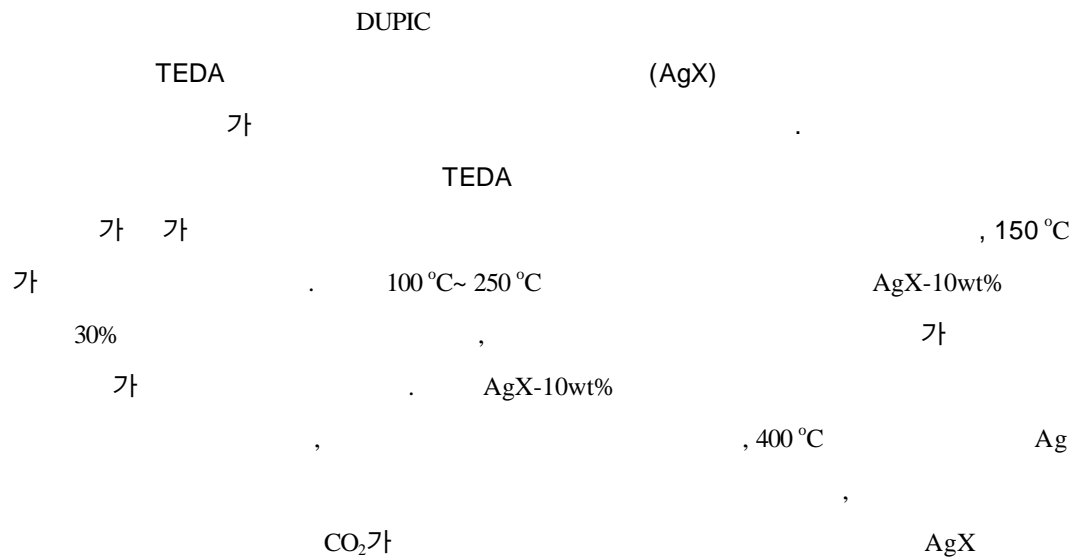
AgX



가 가

AgX

IV.



References

1. D. T. Pence and B. A. Staples, "Solid Adsorbents for Collection and Storage of Iodine-129 from Reprocessing Plants," In Proc. 13th AEC Air Cleaning Conference, CONF-740807, Atomic Energy Commission, Washington, DC, August, p157 1974
2. International Atomic Energy Agency, Design of Off-Gas and Air Cleaning Systems at Nuclear Power Plants, Tech. No. 274, 1987
3. J.G. Wilhelm and J. Furrer, "Iodine Filters in Nuclear Power Stations," In CEC Seminar on Radioactive Effluents from Nuclear Fuel Reprocessing Plants, (Kernforschungszentrum, Karlsruhe, Federal Republic of Germany, 1977
4. R.H. Bellamy, Elemental Iodine and Methyl Iodide Adsorption on Activated Charcoal at Low Concentrations, Nucl. Safety, vol. 15, 16, November, 1974
5. J.C. Wren, C.J. Moore, and M.T. Rasmussen, "Methyl Iodide Trapping Efficiency of Aged Charcoal Samples from Bruce-A Emergency Filtered Air Discharge Systems," *Nuclear Technology*, 125, 28-39, 1999.
6. B.S.Choi, G.I.Park, et al., A Study on the Removal of Radioiodine on Silver-impregnated Adsorbents, Proceeding of the KNS Autumn Meeting, Vol. II, pp. 311-316, Taegu, Korea, 1997
7. G.I.Park, B.S.Choi, et al., Adsorption and Desorption Characteristics of Methyl Iodide on Silver Ion-

8. B.S.Choi, G.I.Park, et al., Adsorption Equilibrium and Dynamics of Methyl Iodide in a Silver Ion-Exchanged Zeolite Column at High Temperatures, Adsorption, Submitted, 2000.

9. , , , , , TEDA/KI
072819

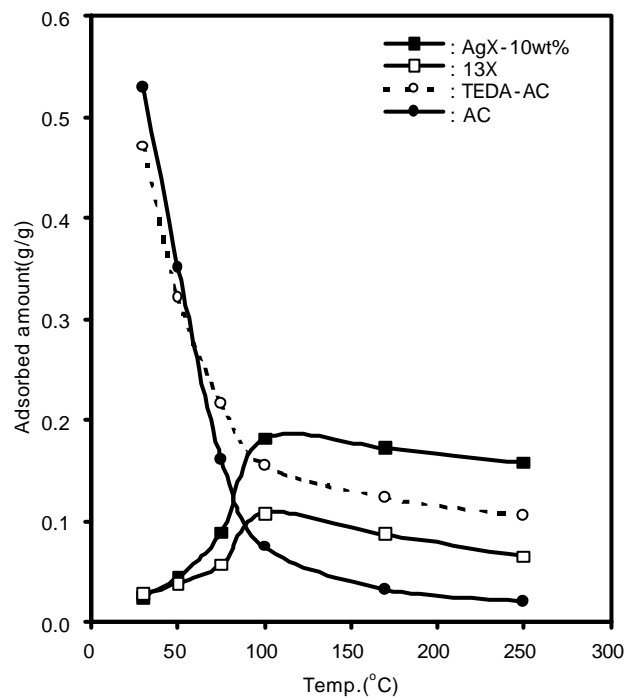


Fig.2. Adsorption amounts of CH₃I with temperature on various adsorbents. (Bed Depth = 3cm, Input conc.= 5×10^{-5} mol/l)

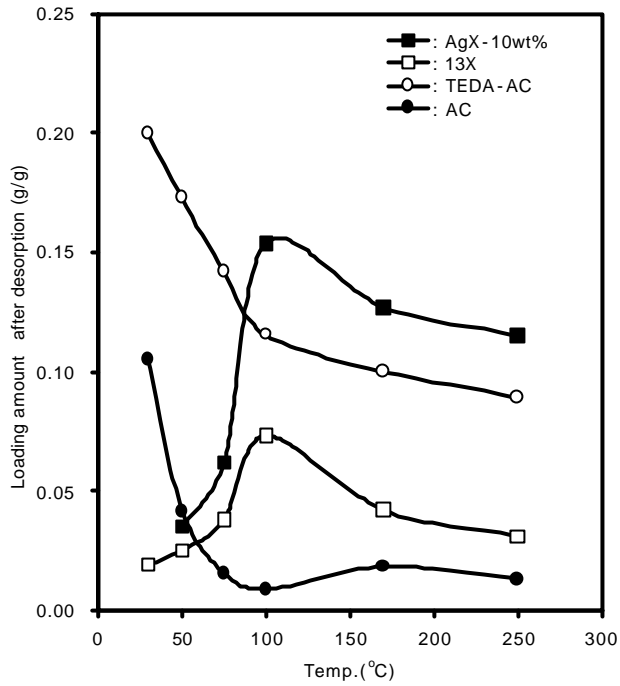


Fig.3. Loading amounts of CH_3I after Desorption with temperature on various adsorbents (Bed Depth = 3cm, Input conc.= 5×10^{-5} mol/l).

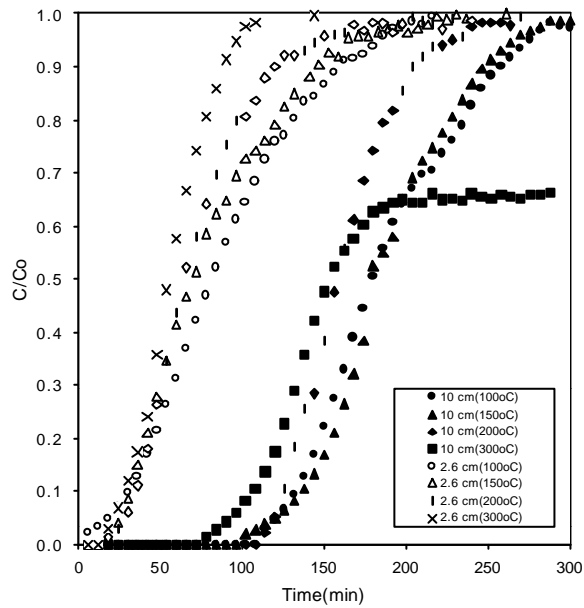


Fig.4. Breakthrough Curves of CH_3I Adsorption with Temperature on AgX-10wt%. (Bed Depth = 2.6, 10 cm, Input conc.= 5×10^{-5} mol/l)

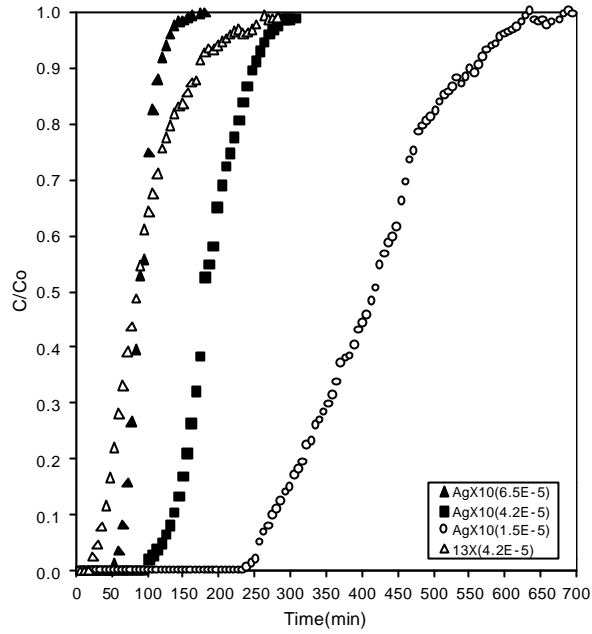


Fig.5. Breakthrough Curves of CH_3I Adsorption with Input Conc. on AgX-10wt%. (Bed Depth = 10 cm, Temp.=150°C)

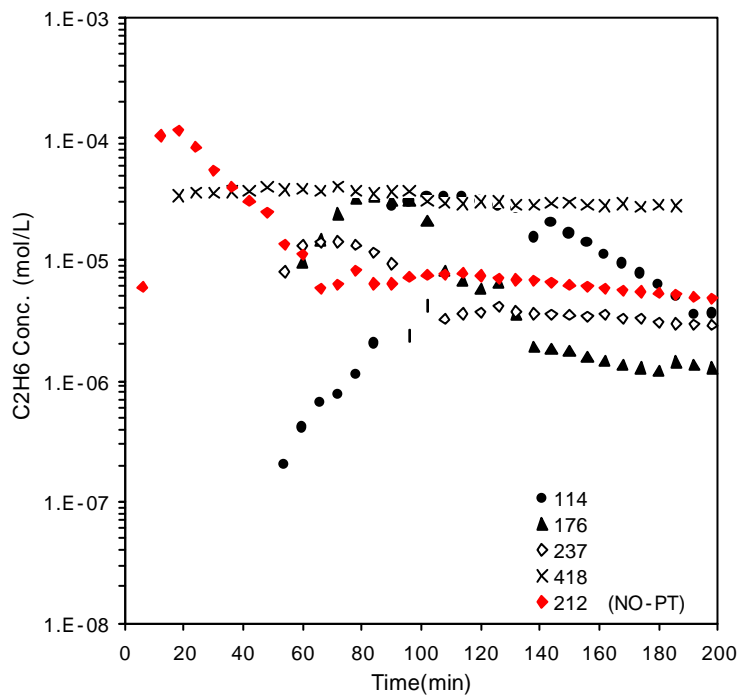


Fig.6. Concentration Profile of Ethane Gas with Adsorption Temperature on AgX-10wt%. (Bed Depth = 10 cm, Temp.=150°C)

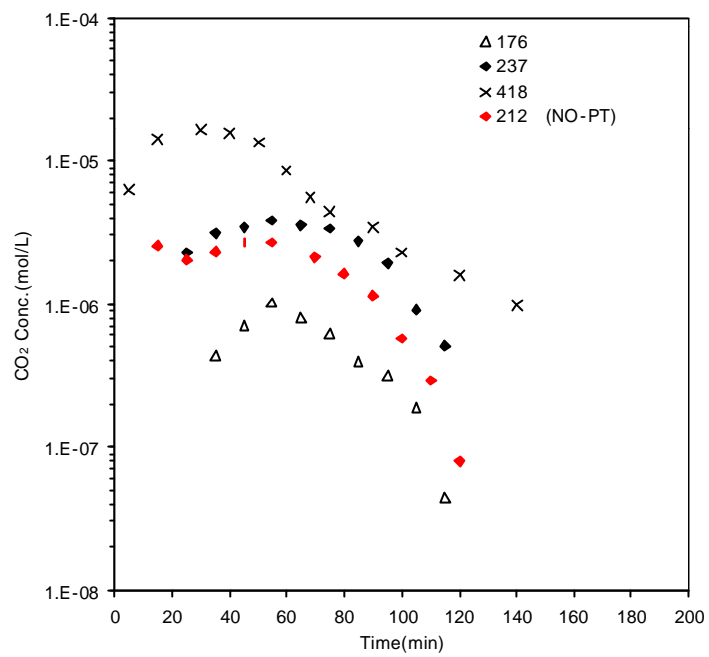


Fig.7. Concentration Profile of Carbon Dioxide Gas with Adsorption Temperature on AgX-10wt%. (Bed Depth = 10 cm, Temp.=150°C)