

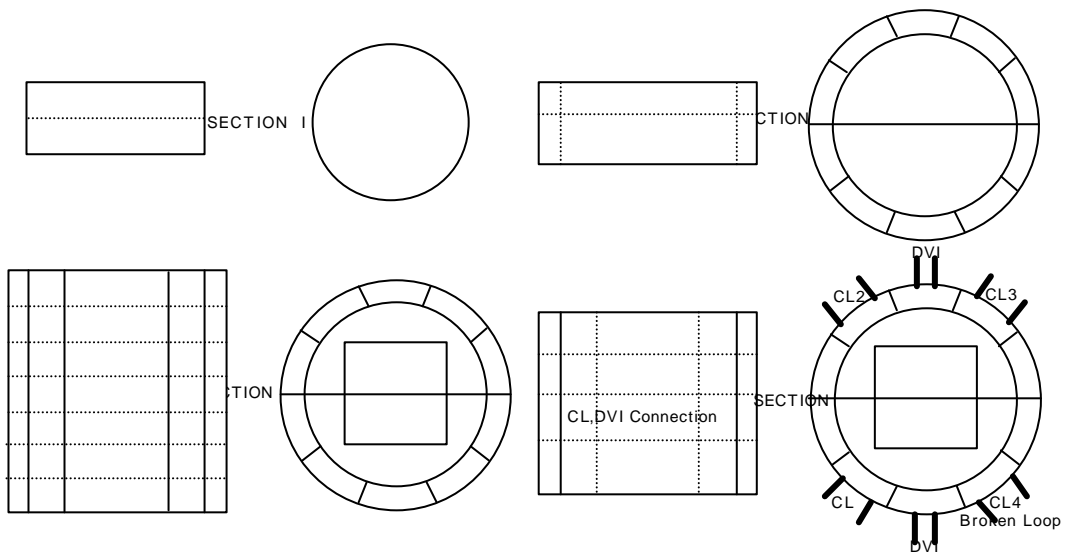
1.

(DVI : Direct Vessel Injection System) 가 DVI UPTF(Upper Plenum Test Facility) Test 21 DVI UPTF DVI 가 UPTF DVI 2 m UPTF DVI 2 UPTF DVI 4 DVI UPTF Full Scale DVI 가 UPTF Test 21 DVI 4 (Phase A, B, C, D) Phase A B (LBLOCA ; Large Break Loss-of-Coolant Accident) EOB(End of Blowdown (Accumulator) (Lower Plenum) Refill Phase A 117 °C , Phase B , Refill , Phase C Upper Core Plate Entrainment , Phase D LBLOCA (Reflood) Downcomer Entrainment MARS(Multi-dimensional Analysis of Reactor Safety) 2.0 UPTF DVI LBLOCA EOB Test 21 Phase A 가 2 UPTF Test 21 Phase A MARS 3 , 4

2. UPTF Test 21 Phase A

UPTF DVI 1300 Mwe, 4-Loop Babcock & Wilcox 가 Downcomer, , 4 Feedback 1 1 UPTF 21A LBLOCA EOB 가 Downcomer DVI 31 37 (315 kg/s)

Nodalization 2 CHANNEL , 1 SECTION SECTION I
 , 1 CHANNEL, 2 NODE SECTION II
 Lower Core Plate , Barrel Downcomer
 Downcomer 4 DVI 2 10 CHANNEL
 SECTION III IV , SECTION IV
 NODE DVI
 Nodalization MARS 2.0
 MARS 2.0 , 가 가



1. UPTF Test 21

MARS Nodalization

4. MARS 가

MARS 2.0 (4~7) 2 가

(1) (2)

Penetration

(50%)

가 Downcomer Annulus

DVI CHANNEL

DVI Penetration ,

DVI 50 %

Broken Cold Leg

2가

'Pool' 'Inverted Pool' Interfacial Friction Model

DVI Water가

Channel

Channel

2

Cell

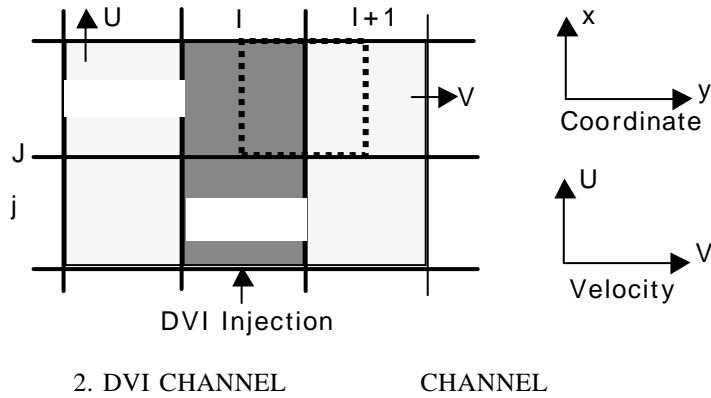
가

MARS 3D

'Pool'

'Inverted Pool'

, Interfacial Friction Force



MARS Interfacial Friction Force Bubbly Flow Regime
 Coefficient 2 DVI Water Injection Channel
 Bubbly Flow Channel Bubbly Flow Film Flow 가
 Friction Force MARS
 [8]. MARS Bubbly Flow Film Flow
 Regime (1), (2) Liquid Vapor Interfacial Friction Coefficient(K_{Ivl})

- Bubbly Flow

$$K_{IBvl} = 0.375 \times \frac{C_D}{r_b} a_v r_l U_r$$

$$\text{where, } C_D = \frac{24}{Re_b} (1.0 + 0.1 \times Re_b^{0.75}) \quad (1)$$

$$r_b = \min(0.5 \frac{We_b s}{r_l U_r^2}, 0.5 D_H, 0.02), \text{ if } a < 0.2$$

- Film Flow

$$K_{IFvl} = 2.0 \times \frac{f_l}{D_H} \sqrt{a_v} r_v U_r \quad (2)$$

$$\text{where, } f_l = 0.005 \times (1.0 + 75 \times a_l)$$

MARS Interfacial Term Small Bubble Flow Stable Film Flow Large Bubble Flow
 Unstable Film Flow Flow Regime Term Factor
 0.4 Small Bubble Flow Large Bubble Flow
 2 Flow Pattern Bubbly Flow Film Flow 가
 Flow Regime
 Interfacial Friction Coefficient (1) Momentum Cell
 Cell (2) Interfacial Friction Force (1) (2)
 (3)

$$K_{Ivl} = (1 - \mathbf{a}_{\max})(1 - \frac{0.25\mathbf{a}_l}{\mathbf{a}_v})K_{IBvl} + \mathbf{a}_{\max} \frac{0.25\mathbf{a}_l}{\mathbf{a}_v} K_{IFvl} \quad (3)$$

where, $\mathbf{a}_{\max} = 0.5 \times \max(\mathbf{a}_l, \mathbf{a}_{l+1})$

Wall Friction Factor

MARS 3D Wall Friction, 1D/3D, 3D
 Wall Friction . MARS
 3D Pressure Drop 1D Pressure Drop
 Wall Drag Pressure Drop . 3D Bubbly Flow
 Regime Wall Friction Factor (4)

$$f_k = \max\left(\frac{64.0}{Re_k}, \frac{1.691}{Re_k^{0.43}}, \frac{0.117}{Re_k^{0.14}}\right) \quad (4)$$

3 (4) 가 Reynolds Number 600 Lamina Flow Region, 600
 10000 Laminar-Tubulent Transition, 10000 Tubulent Region
 Friction Factor Downcomer

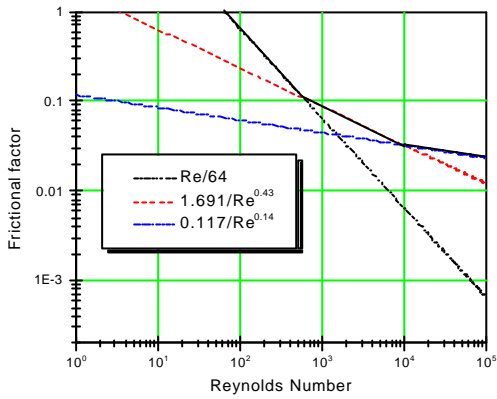
Hydraulic Diameter가

MARS 1D Wall Friction Factor 가 Laminar Flow Reynolds
 Number 2200, Transition 2200 3000, 3000 Tubulent flow 가
 Friction Factor

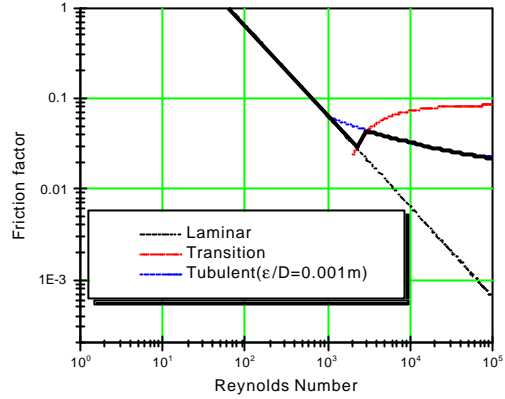
$$f_k = \begin{cases} \frac{64.0}{Re_k}, & \text{for laminar region,} \\ (3.75 - \frac{8250}{Re_k})(f_{T,3000} - f_{L,2200}) + f_{L,2200}, & \text{for transition region,} \\ \left[-2 \log \left\{ \frac{e}{3.7D} + \frac{2.51}{Re_k} \left(1.14 - 2 \log \left(\frac{e}{D} + \frac{21.25}{Re_k^{0.9}} \right) \right) \right\} \right]^{-2}, & \text{for tubulent region} \end{cases} \quad (5)$$

(5) Transition, Tubulent Friction Factor (5)

MARS 3D Friction Factor, Wall Roughness Default Value
 0.0001 m 가
 MARS 1D/3D Momentum Equation 1D Energy
 Mass Equation 1D/3D
 . 1D 3D
 1D 3D Cell Cross, 3D Gap
 (Channel Horizontal Junction) Gap
 가 3D



Base Model



Modified

3. MARS 3D

MARS 3D Interfacial Term
 3D Vapor Phase Steam
 Fraction (6) Density
 Density Fraction

Friction Factor

Vapor Phase Density 가
 Density Mass
 Vapor Phase Density
 Interfacial Term Steam Phase

$$r_n = r_v \frac{M_n}{M_n + M_s}, \quad r_s = r_v \frac{M_s}{M_n + M_s}$$

where, r_v : Vapor Phase Total Density

r_n : Noncondensable gas Density

r_s : Steam Density

M : Mass

(6)

MARS (1) MARS 3D
 Momentum Cell
 Section(Elevation Channel)
 Loss Coefficient Horizontal Momentum Cell
 Friction Wall (Roughness)
 Channel

Gap Loss Coefficient Horizontal
 Gap
 Wall
 Default 0.0001 m가

(1) Gap Loss Coefficient Cell
 Table Table , 6060tt00
 6060ttdd Gap

6050ccxx Channel Variation
 Word (-) cc

(2) Wall Friction Factor
 Word . Default

6020cc00 Channel Data

5. MARS 가

MARS 2.0

가

가

4.6 bar

가 80

5.2 bar

52

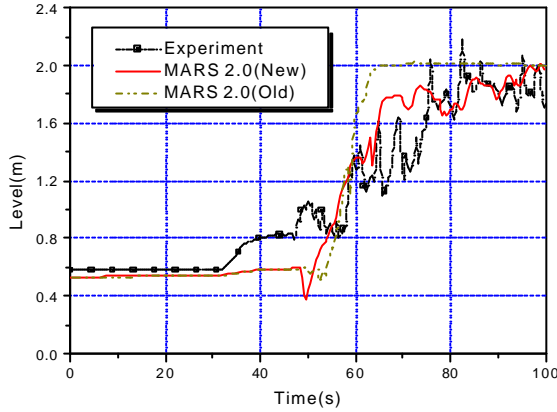
57

가

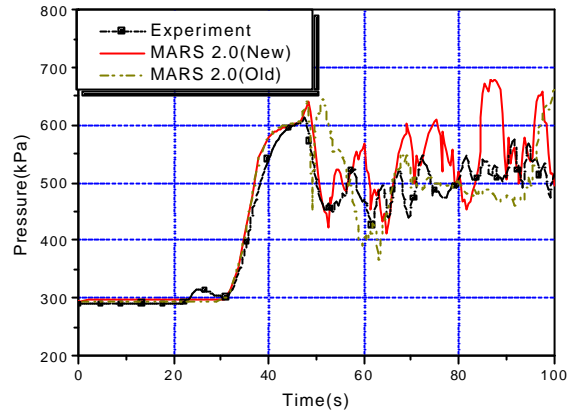
80

1.8 m

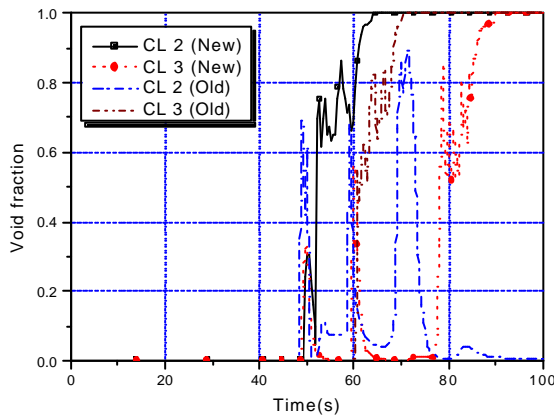
65



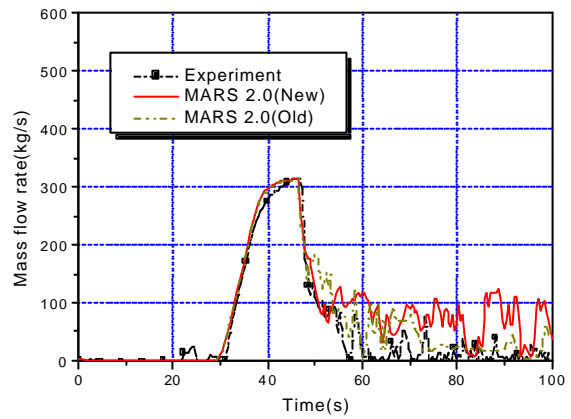
4.



5. Downcomer



6. 3



7.

, 4

, MARS

MARS 2.0

Phase A 가

(80 ~100)

1.8 m

MARS 2.0

DVI

, 60 80

(ECC Penetration)

MARS 2.0

, 70

가

(Loop 2 3)

Downcomer

가

4.

UPTF DVI MARS 2.0
 LBLOCA EOB 가
 Refill . 4 (Phase A, B, C, D) , Phase A MARS 2.0
 가
 Phase A MARS 2.0 가
 () 가 MARS 3D Interfacial Friction
 Force Wall Friction Factor MARS
 , MARS
 LBLOCA EOB MARS DVI
 , UPTF DVI B, C D 가 , DVI MARS
 가가

K_{IW} : Interfacial friction coefficient

: Void fraction

: Phase density

Re : Reynolds number

: Surface tension

f : Friction factor

C_D : Interfacial Drag Coefficient

r_b : Bubble radius

U_r : Relative Velocity

We : Weber number

D_H : Hydraulic diameter

: Wall roughness

5.

- [1] , , , , “ MARS 1.3 ”, KAERI/TR-1108/98 (1998)
- [2] J.-J. Jeong, K.S. Ha, B.D. Chung and W.J. Lee, “Development of a multi-dimensional thermal-hydraulic system code, MARS 1.3.1”, ANE, Vol. 26 No. 18 (1999)
- [3] U.S. NRC, “RELAP5 Code Manual Volume”, NUREG/CR-5535 (1998)
- [4] M.J. Thurgood, et.al., “COBRA/TRAC Manual”, NUREG/CR-3046 (1983)
- [5] Jae-Jun Jeong, et. al., “MARS/MASTER Solution to OECD Main Steam Line Break Benchmark Exercise III”, J. of KNS, Vol. 32, No. 3, (2000)
- [6] , , , “MARS 1.3 System Analysis Code Coupling with CONTEMPT4/MOD5/PCCS Containment Analysis Code using DLL”, Proc. KNS '98 Autumn Meeting (1998)
- [7] UPTF Team, “Experimental Data Report, Test No. 21, Downcomer Injection Test”, SIMENS AG, KWU (1990)
- [8] J.J. Jeong, I. Dor, and D. Bestion, “Improvement and Assessment of the CATHARE 2 Three-dimensional Module Compared with the UPTF Downcomer Test 7”, Nuclear Technology, Vol. 117 (1996)