

ABSTRACT

The objective of this study is to establish evaluation and verification guideline for the APR 1400 and to investigate the thermal-hydraulic characteristics for reactor vessel are analyzed using FLUENT. The scope and major results of research are thermal-hydraulic characteristics for reactor vessel. The reactor vessel design data of APR-1400 are surveyed to develop numerical model. Porous media model is applied for fuel rod bundle, and full-scale, three-

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dimensional simulation is performed at actual operating conditions. Distributions of velocity, pressure and temperature are well agreed with those of design data for ARP-1400.



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(Upper), , (Cor (Lower), (Cold leg), (Hot Leg) , (Core), APR- 1400 1 , [2,3]. 가 . 가 16 × 16 . , $166.6 \times 10^{\circ} \text{ lbm/hr} (17.91 \text{ m/s})$, 555 F (563.7 K) 18.19 psi, 9.08 psi . 12.97 psi , 1.35906 × 10¹⁰ Btu/hr (Heat Flux) $1.273945 \times 10^{8} \text{ W/m}^{3}$ [4].

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(1) , (1) , (2) , (1) (2) , (1) (2) , (1) (2) , (2) , (2) (3) . (3) . (3) . (3) . (3) . (3) . (3) . (3) . (3) . (3) .

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$$k - \varepsilon \qquad \text{RNG } k - \varepsilon \quad \text{, Reynolds Stress}$$

$$k - \varepsilon \qquad k - \varepsilon$$

$$k \qquad \varepsilon \qquad (4), (5) \quad .$$

$$U_k \frac{\partial k}{\partial x_k} = \frac{\partial}{\partial x_k} \left[(v + \frac{v_i}{\sigma_k}) \frac{\partial k}{\partial x_k} \right] + P + G - \varepsilon$$
(4)

$$U_k \frac{\partial \varepsilon}{\partial x_k} = \frac{\partial}{\partial x_k} \left[(v + \frac{v_t}{\sigma_k}) \frac{\partial k}{\partial x_k} \right] + \frac{\varepsilon}{k} (C_1 (P + G) - C_2 \varepsilon)$$
(5)

Two-equation $k - \varepsilon$ modelRNG $k - \varepsilon$ modelReNormalizationGroup method

semi-empirical approach가

model

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$$7^{1}$$
,(low Reynolds number). $k - \varepsilon$, strained, swirling, turbulent Prandtl numberanalytical formula($k - \varepsilon$ turbulent Prandtl number 7^{1} ., RNG $k - \varepsilon$ model

, RNG

compressibility 7 (6), (7) .

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$$U_k \frac{\partial k}{\partial x_k} = \nu_t S^2 - \varepsilon + \frac{\partial}{\partial x_k} a \nu_t \frac{\partial k}{\partial x_k}$$
(6)

$$U_{k}\frac{\partial\varepsilon}{\partial x_{i}} = C_{1\varepsilon}\frac{\varepsilon}{k}\nu_{t}S^{2} - C_{2\varepsilon}\frac{\varepsilon^{2}}{k} - R + \frac{\partial}{\partial x_{k}}\alpha\nu_{t}\frac{\partial\varepsilon}{\partial x_{k}}$$
(7)

Reynolds Stress

. RSM Isotropic eddy viscosity 7,

Reynolds

Reynolds-averaged Navier-Stokes

(8), (9) .

$$\frac{\partial(\rho U_k u_i u_j)}{\partial x_k} = \rho(P_{ij} - \varepsilon_{ij} + \phi_{ji} + d_{ijk})$$
(8)

$$\frac{\partial (U_k \varepsilon)}{\partial x_k} = C_{\varepsilon} \frac{\partial}{\partial x_k} \left(\frac{x}{\varepsilon} \overline{u_i u_i} \frac{\partial \varepsilon}{\partial x_i} + \frac{1}{2} C_{\varepsilon,1} \frac{x}{\varepsilon} P_{kk} - C_{\varepsilon,2} \frac{\varepsilon^2}{x} \right)$$
(9)

2.

$$(10) \qquad .$$

$$\frac{\partial}{\partial x_{k}}(\rho U_{k}\phi) = \frac{\partial}{\partial x_{k}}(\Gamma_{\phi}\frac{\partial\phi}{\partial x_{k}}) + S_{\phi} \qquad (10)$$

$$, \qquad , \qquad S_{\phi} \qquad . \qquad \phi = 1$$

$$, \quad \phi = U_{i} \qquad , \quad \phi = T$$

$$, \quad \phi = k \quad \varepsilon \qquad . \qquad S_{\phi}$$

$$(FVM : Finite Volume of the set of$$

Method) (11) .

$$\phi_p \sum_i (A_i - S_p) = \sum_i (A_i \phi_i) + S_c$$
(11)

FLUENT
(11)

FLUENT(11).FLUENT,,GAMBIT, SolverFLUENT(fully implicit scheme)Code(non-staggered grid),,,power-law,2,QUICK
$$k - \epsilon$$
RSM(Reynolds Stress Model)RNG(Renormalization Group)SIMPLESMMPLEC.power-law scheme, $k - \epsilon$, RNG $k - \epsilon$, SIMPLE algorithm,

10⁻⁶ 가

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$$\overline{R} = \frac{\sum_{nodestP} \left| \left[A_{E}\varphi_{E} + A_{W}\varphi_{W} + A_{N}\varphi_{N} + A_{S}\varphi_{S} + S_{C} - A_{P}\varphi_{P} \right] \right|}{\sum_{nodestP} \left| (A_{P}\varphi_{P}) \right|} \leq 10^{-6}$$
(12)

Porous Media ,,Porous Media. PoroMediapacked bed, filter paper,, flow distributor, tube bank . Porous . Porous Media 가 Porous zone , Porous zone 가 . Porous Media (13), . (14)

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$$S_{i} = \sum_{j=1}^{3} D_{ij} \mu U_{j} + \sum_{j=1}^{3} C_{ij} \frac{1}{2} \rho |U_{j}| U_{j}$$
(13)

$$\frac{\partial}{\partial t} (\psi \rho_f h_f + (1 - \psi) \rho_s h_s) + \frac{\partial}{\partial x_i} (\rho_f u_i h_f) =$$

$$\frac{\partial}{\partial x_i} \left(k_{eff} \frac{\partial T}{\partial x_i} \right) \cdot \psi \frac{\partial}{\partial x_i} \sum_{j'} h_{j'} J_{j'} + \psi \frac{Dp}{Dt} + \psi \tau_{ik} \frac{\partial u_i}{\partial x_k} + \psi S_f^h + (1 - \psi) S_f^h$$
(14)

Porous Media		Porous Media	
		. Porous Media	
(effective conductivity) k_{eff}	(15)		

$$k_{eff} = \phi k_f + (1 - \phi) k_s$$
(15)

 ψ Porous media porosity, k_f , k_s

		2			,
	1/4		,		3%
	가				
			,		,
				,	(downcomer)
	가				
				,	Porous
Media		,			(Heat
Source)			[5].		

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3 (core support barrel)

가 , 가 . 가 가 4 5 가 , (Bypass) 가 , 6 . 가 , 가 .

가

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2.			
7			, 8
			(563.7 K)
가		가	(593.4 K)
	가		가 593.4 K

APR-1400 597 K (615 F)

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3.

9 가	,			7	ŀ	
		·	가		10	

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0.506 MPa

・ APR-1400 7 FLUENT ・ 7 7 (Poros Media) 7 3 ,

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(Bypass) 기

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2.

[1]	FLUENT	User's Guide,	Version 5, 1998		
[2]		, "APR 1400		", 2000.	
[3]		, "	2	, NSSS	", 1997
[4]		"			", KAERI/TR-735/96,
	1996.				
[5]		· · · · · · · · · · · · · · · · · · ·			가", KINS/HR-405, 2001.





























