

Development of a Numerical Analysis Code for Natural Convection

150

FVM(Finite Volume Method)
Rayleigh $10^4 \sim 10^6$, 1~20
Rayleigh

ABSTRACT

Numerical simulations of the two-dimensional, steady state, incompressible flow in a rectangular enclosure with a variety of aspect ratios, have been accomplished using a FVM (Finite Volume Method) based code. Computations cover Rayleigh numbers from 10^4 to 10^6 , aspect ratios from 1 to 20. Results show that the aspect ratio, the Rayleigh number, are the key parameters to determine the heat transfer and fluid flow characteristics in an enclosed rectangular cavity. By comparing them, the calculated results with a developed code are well similar with previous literatures.

1.

SMART 가

가 가

[1]. 가
 Eckert Carlson[2], MacGregor Emery[3], Yin et al.[4],
 Bejan[5], De Vahl Davis[6], Hortmann et al.[7]

Bejan

. Hortmann et al.

FVM

가 (A > 10)

Ra

2.

가 Boussinesq , 2 , 가

$$\frac{\partial}{\partial x_j}(\mathbf{r}U_j) = 0 \quad (1)$$

$$\frac{\partial}{\partial x_j}(\mathbf{r}U_j U_i) = -\frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_j}(\mathbf{m} \frac{\partial U_i}{\partial x_j}) + \mathbf{r}g_i \mathbf{b}(T - T_\infty) \quad (2)$$

$$\frac{\partial}{\partial x_j}(\mathbf{r}U_j T - \frac{\mathbf{m}}{\text{Pr}} \frac{\partial T}{\partial x_j}) = 0 \quad (3)$$

\mathbf{r} , U_i Cartesian , T , \mathbf{b} , Pr Prandtl
 g_i 가 ∞ (Non-staggered grid)

SIMPLE [8]

QUICK scheme , Stone SIP(Strongly Implicit Procedure)[9]

[10]

residual 10^{-8} 가

3.

Lid-driven cavity flow Skewed cavity flow
 Cavity 가

1 (a) Ghia[11]
 (Re=400) 1(b)
 80x80
 가 Lid-driven skewed cavity flow
 가 45° Re 100
 Demirzic [12]
 가 가
 2(a)-(b)

3 가

1 가
 Hortmann [7] Ra=10⁵ 10⁶

4 5 가 가 가 가
 Ra Nu Nu 2

$$\overline{Nu} = Q / Q_c \tag{4}$$

Q 가 heat flux Q_c heat flux

$$Q_c = \frac{m}{Pr} \frac{T_H - T_c}{L} H \tag{5}$$

3 Ra=10⁶ 80x80
 가 (L) 80
 (H)가 가 6 Ra
 Ra 가 Nu 가
 가 가 가
 A=5, 10

4.

FVM(Finite Volume Method)

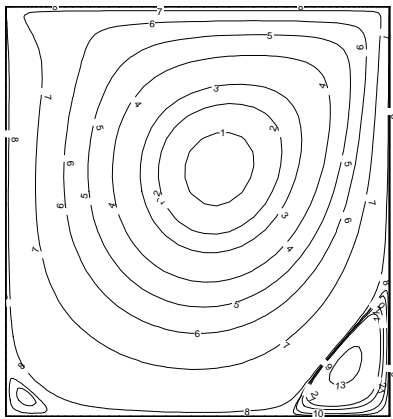
Lid-driven cavity flow Skewed cavity flow

1~20

(A) Rayleigh (Ra)

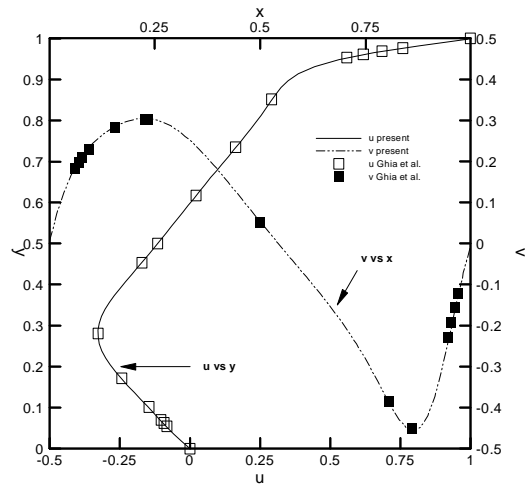
Rayleigh $10^4 \sim 10^6$

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2. Eckert, E. G., and Carlson, W.O., “Natural convection in a layer enclosed between two vertical plates with different temperatures,” *Int. J. Heat Mass Transfer*, Vol. 2, pp. 106-120, 1961.
3. McGregor, R. K., and Emery, A. F., “Free convection through vertical plane layers - moderate and high Prandtl number fluids,” *J. Heat Transfer*, Vol. 91, pp. 391-402, 1969.
4. Yin, S. H., and Wung, T., Y., and Chen, K., “Natural convection in an air layer enclosed within rectangular cavities,” *Int. J. Heat Mass Transfer*, Vol. 21, pp. 307-315, 1978.
5. Bejan, A., “Note on Gill’s solution for free convection in a vertical enclosure,” *J. Fluid Mech.*, Vol. 90, pp. 561-568, 1978.
6. De Vahl Davis, G., “Natural convection of air in a square cavity: a benchmark numerical solution,” *Int. J. numer. Methods fluids*, Vol. 3, pp. 249-264, 1983.
7. Hortmann, M., and Peric, M., and Scheuerer, G., “Finite volume multigrid prediction of laminar natural convection: Bench-mark solutions,” *Int. J. Numerical Methods in Fluids*, Vol. 11, pp. 189-207, 1990.
8. Partankar, S. V., *Numerical heat transfer and fluid flow*, Hemisphere, 1983.
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10. Rhie, C. M., and Chow, W. L., “A numerical study of the turbulent flows past an isolated airfoil with trailing edge separation,” *AIAA Journal*, Vol. 21, pp. 1525-1532.
11. Ghia, U. Ghia. K. N., and Shin, C. T., “High-Re Solutions for Incompressible Flow Using the Navier-Stokes Equations and a Multigrid Method,” *J. of Comp. Physics*, Vol. 48, pp. 387-411, 1982.
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Level f	Value
13	0.0005
12	0.0001
11	5E-05
10	1E-05
9	1.79486E-06
8	-0.0001
7	-0.01
6	-0.03
5	-0.05
4	-0.07
3	-0.09
2	-0.1
1	-0.11

(a)

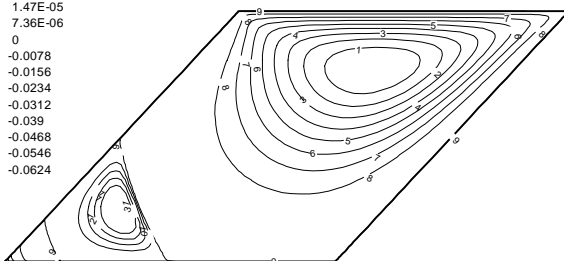


(b)

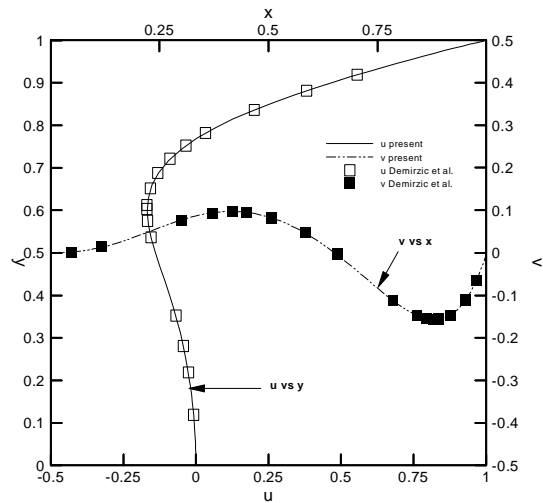
1 (a) , Re=400 (80x80); (b)

(u vs y, v vs x)

Level f	Value
13	2.94E-05
12	2.2E-05
11	1.47E-05
10	7.36E-06
9	0
8	-0.0078
7	-0.0156
6	-0.0234
5	-0.0312
4	-0.039
3	-0.0468
2	-0.0546
1	-0.0624



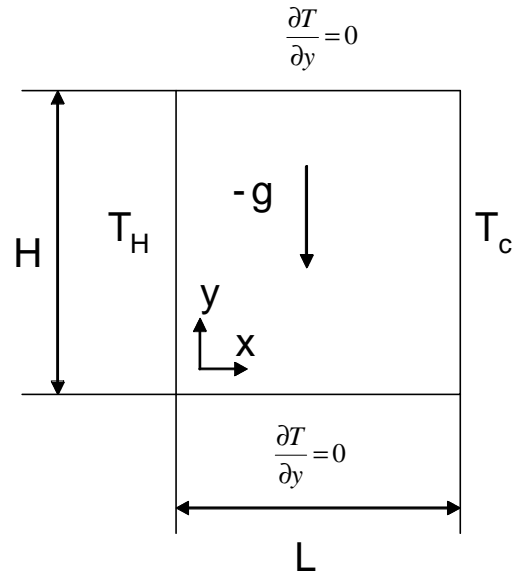
(a)



(b)

2 (a) , Re=100 (80x80); (b)

(u vs y, v vs x)



3

1

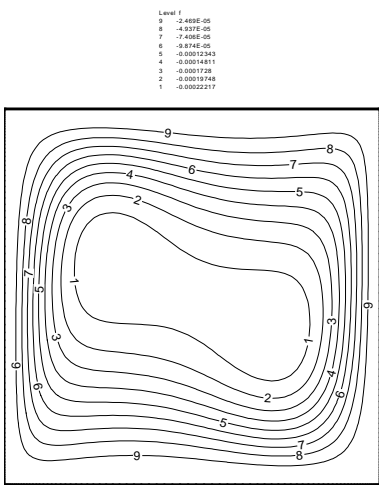
Ra	r	m	b	Pr	g	T_H	T_C	L	H
10^4	1.19	1.8×10^{-5}	0.00341	0.71	9.81	12	2	0.021277	0.021277
10^5	1.19	1.8×10^{-5}	0.00341	0.71	9.81	12	2	0.045841	0.045841
10^6	1.19	1.8×10^{-5}	0.00341	0.71	9.81	12	2	0.098761	0.098761

2

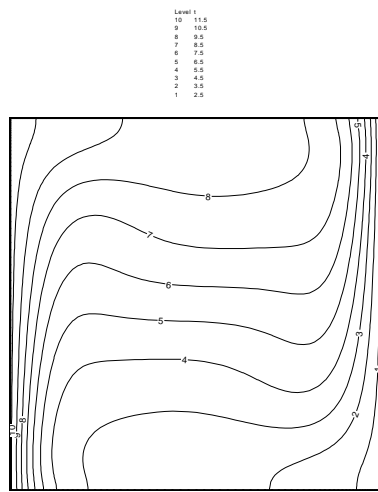
Ra	\overline{Nu} (Hortmann et al.)	\overline{Nu} (Present)	Error (%)
10^4	2.24475	2.23995	0.2
10^5	4.52164	4.52295	0.03
10^6	8.82513	8.82042	0.05

3

$(Ra = 10^6)$	\overline{Nu}
40x40	8.80204
80x80	8.82042
160x160	8.82678

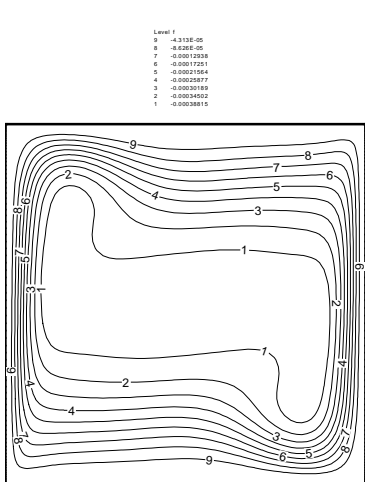


(a)

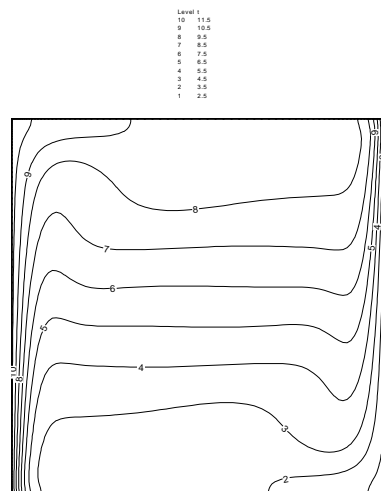


(b)

4 (a) ($Ra=10^5$, 80×80); (b)

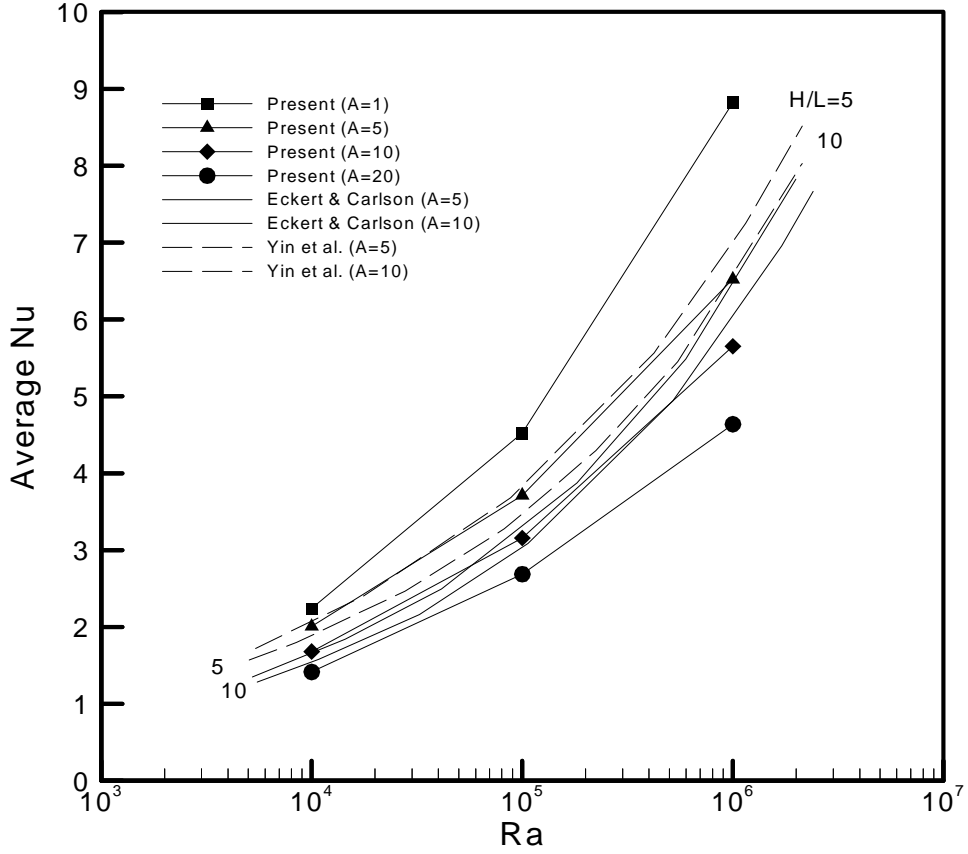


(a)



(b)

5 (a) ($Ra=10^6$, 80×80); (b)



6 Nu Ra