

Numerical Analyses of Flow Structure and Heat Transfer Downstream of Mixing Vane of Spacer Grid in Fuel Assembly

*,

253

RANS

Split vane

, SG1 SG2

k - ϵ

Abstract

The present work analyzed the effect of mixing vane shape on the flow structure and heat transfer downstream of mixing vane in a subchannel of fuel assembly, by obtaining velocity and pressure fields, flow-mixing factors, heat transfer coefficient and friction factor using three-dimensional RANS analysis. Split vane as a typical mixing vane and SG1 and SG2, which are designed by the authors, were tested to evaluate the performances in enhancing the heat transfer. Standard k- ϵ model is used as a turbulence closure model, and, periodic and symmetry conditions are set as boundary conditions. It reveals that heat transfer rate is affected significantly by swirl and cross-flow as well as by the flow blockage.

1.

가

(turbulence)

(spacer grid) (mixing vane)

Rehme^[1] 가 Shen

[2] LDV 가 ripped -open 25 °

Chun Choi^[3]

가 (CFD)

In^[4,5,6] CFD CFX-4.2 가

[7] 가 CFD Gu

FLOW3D CFD CFDS-

CFD In^[8] CFD Split vane 30 °-35 ° Swirl vane

35 °-40 ° In^[9] CFD 가

3

가, 2

CFD CFX-TASCflow^[10] split vane

SG1 SG2

2.

2.1

가

가

Fig.1

40mm 600mm (D_h)

11.468mm (D) 9.5mm 12.7mm

$40 D_h$ $3.5 D_h$ (40mm)

$50 D_h$ (560mm)
 Fig.2 371 (SG1,
 SG2 Split vane) SG1
 15 ° SG2
 SG1 15 °
 25 ° Split vane 25 °
 10mm SG1, SG2 Split vane CFD 180
 3 150,000 Fig.3 371

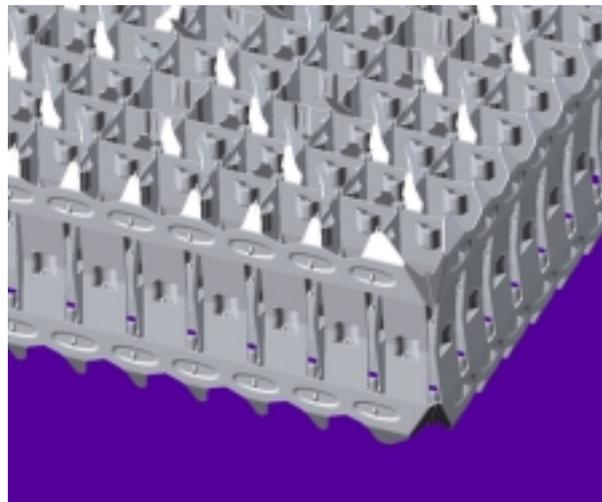


Fig. 1 Detail of the spacer grid with mixing vanes

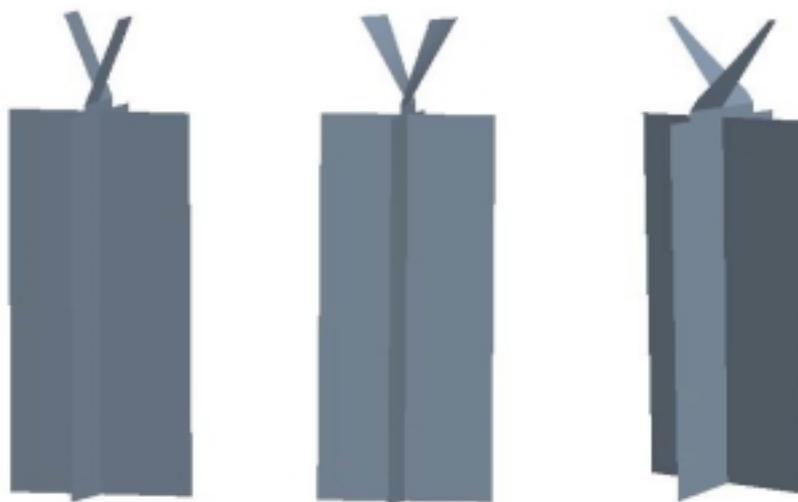


Fig. 2 Spacer grid CFD models: SG1, SG2, and split vane(from left)

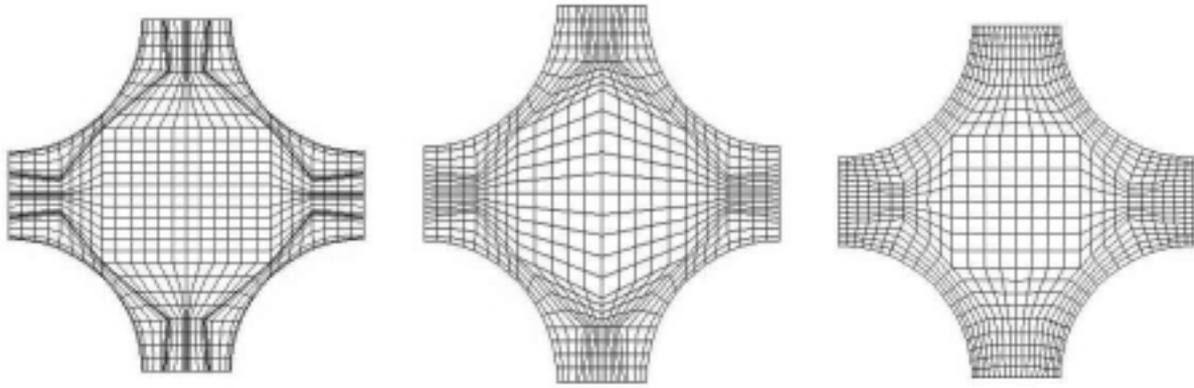


Fig. 3 Subchannel cross-sectional grids: SG1, SG2, and split vane(from left)

2.2

(no-slip)
(heat flux; $30000 W/m^2$)

(periodic condition)

가

가

$6.79 m/s$ (Re=80,000)

2.3

CFD CFX-TASCflow

LPS(Linear Profile Skewed Upstream Differencing Scheme)

Launder Spalding^[11]

k - ε

(Residual) 10^{-3}

가

3

3.

3.1

Fig.4

$Z/D_h = 2$

$Z/D_h = 30$

3가

($Z=0$)

$2 D_h$

SG1

SG2

Tip

()

()

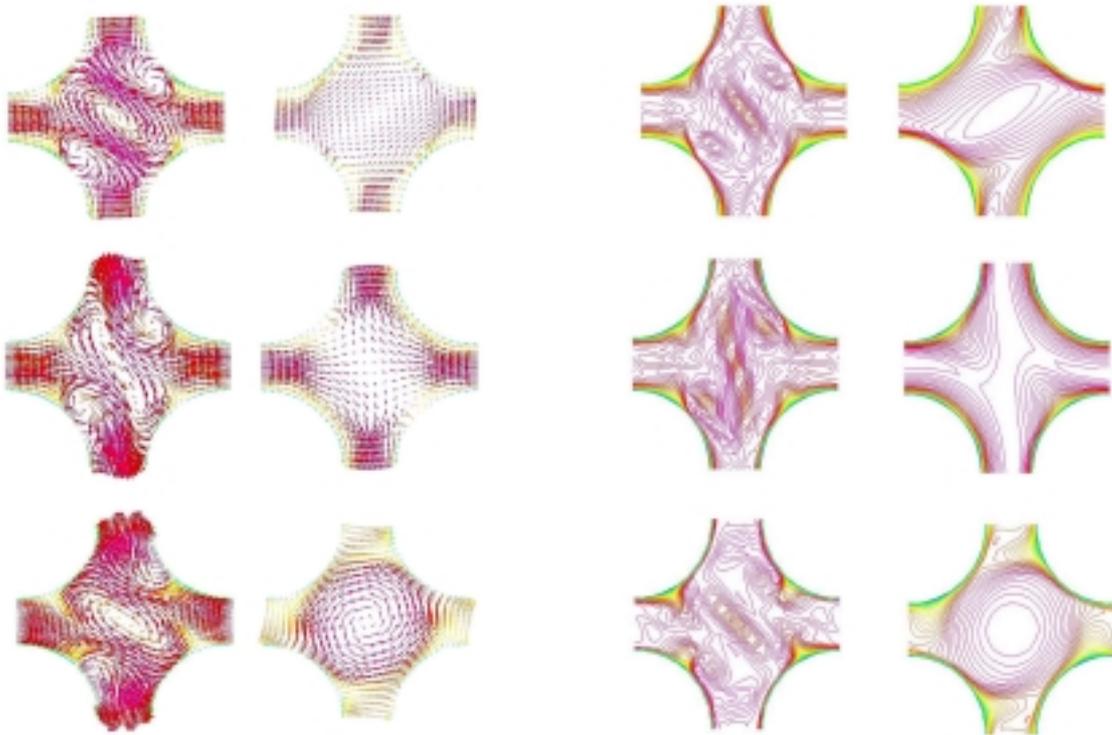
Split vane

$30 D_h$

SG2

가

SG1



$Z/D_h = 2$

$Z/D_h = 30$

$Z/D_h = 2$

$Z/D_h = 30$

Fig.4 Velocity vectors and contours in the subchannel: SG1, SG2, and split vane(from top)

가

Split vane

SG2

가

3.2

Fig.5

$Z/D_h = 2$

$Z/D_h = 30$

3가

가

$2D_h$

가

$30D_h$

SG1

Split vane

SG2

가

가

$30D_h$

SG2

가

Split vane

Fig.6 3가

가

Split vane

25°

가

가

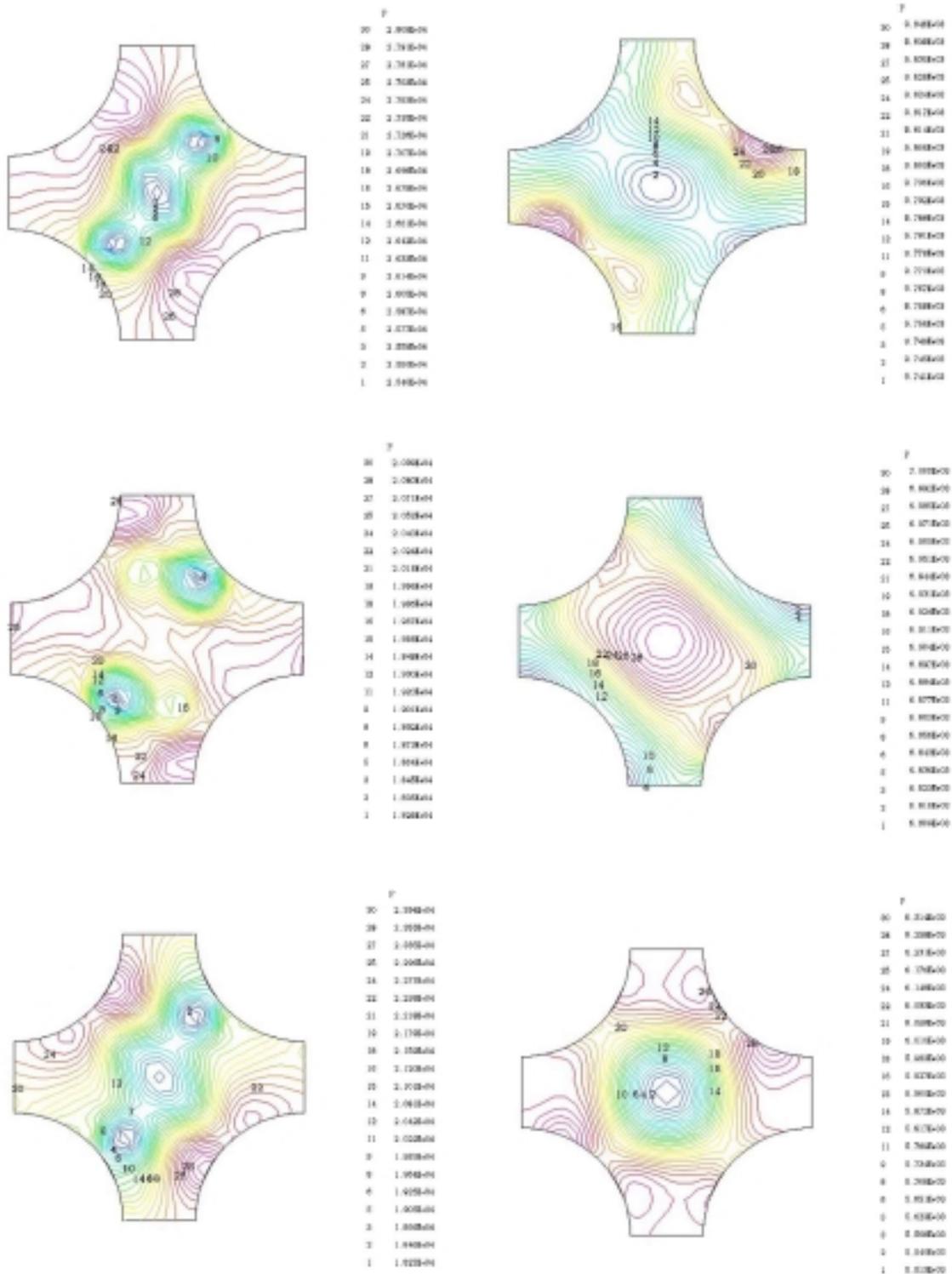
Split vane
(Blockage Ratio) 가

SG1

가

SG1

가



$Z/D_h = 2$

$Z/D_h = 30$

Fig.5 Pressure contours in the subchannel: SG1, SG2, and split vane(from top)

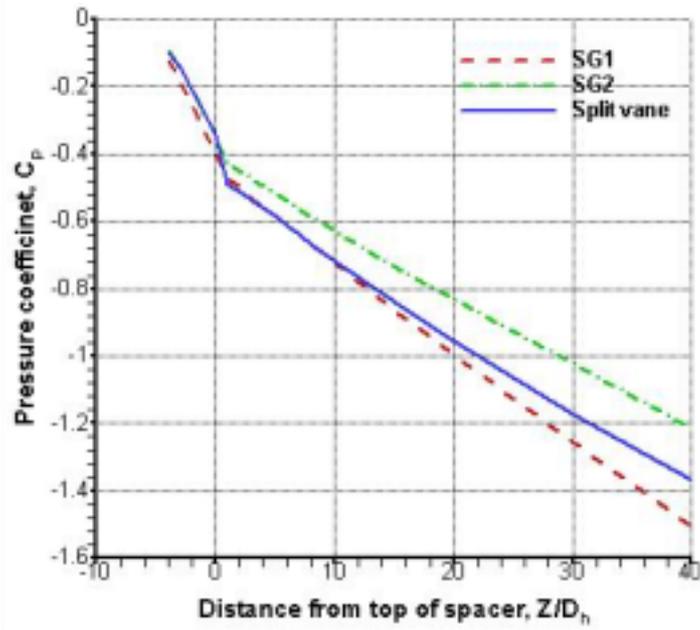


Fig.6 Pressure distributions in subchannel

3.3

가 (swirl factor)

$$S_M = \frac{\int_0^{R_s} r^2 V_{lateral} U dr}{R_s \int_0^{R_s} r U^2 dr} \quad (1)$$

$V_{lateral}$ U r R_s

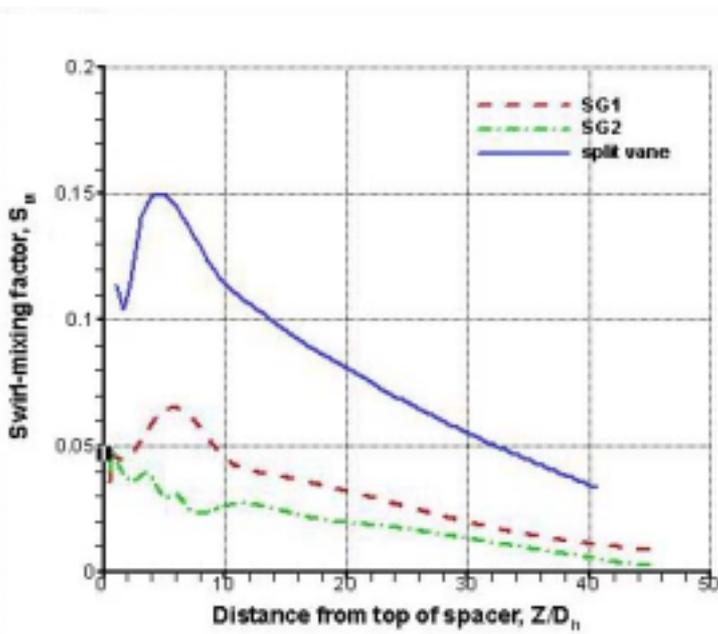


Fig.7 Axial variation of swirl-mixing factor

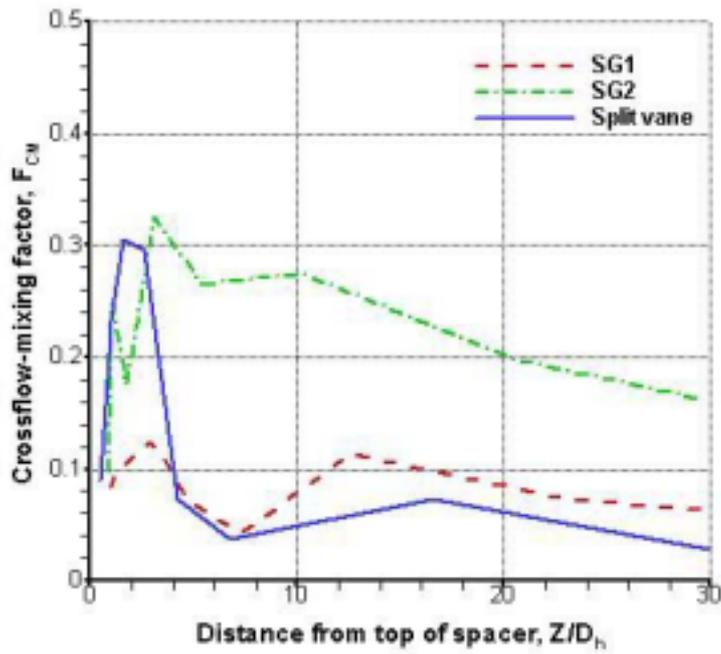


Fig.8 Axial variation of crossflow -mixing factor

Fig.7 . Split vane 가
 가 SG2 가 .
 가 (cross-flow factor)

$$F_{CM} = \frac{1}{s} \int \frac{|V_{cross}|}{V_{bulk}} dy \quad (2)$$

Fig.8 V_{cross} . SG2 V_{bulk} 가
 Split vane $3D_h$ 가

, Split vane SG2

3.4

가 가
 Nusselt 가 (SG1, SG2, Split vane) 가

$$\frac{Nu}{Nu_0} = \frac{T_{b_0} - T_{w_0}}{T_b - T_w} \quad (3)$$

T_{b_0} T_{w_0} 가

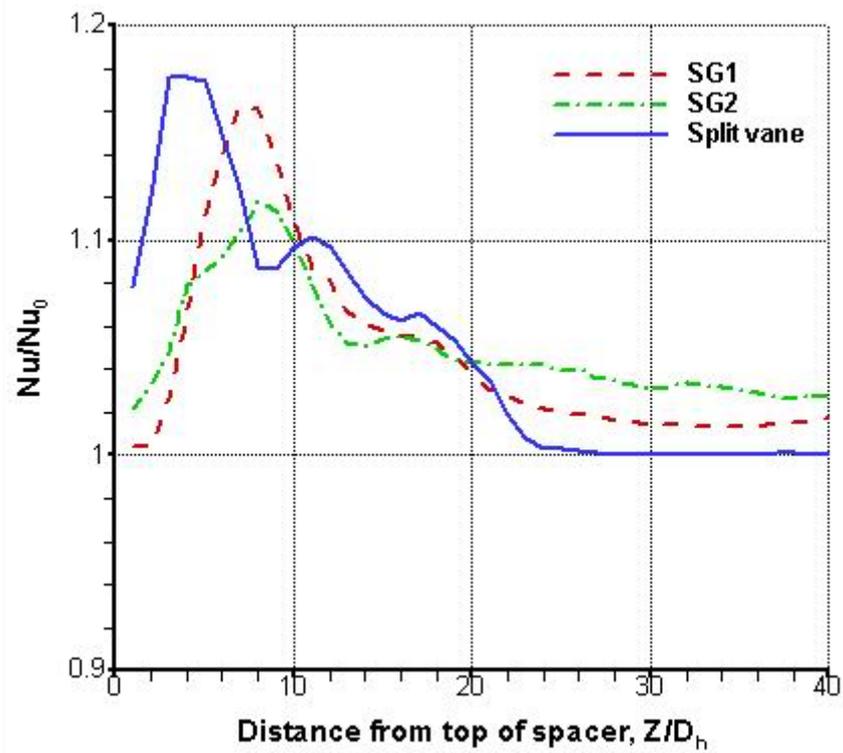


Fig.9 Nusselt number distributions for the different three mixing vanes

(Bulk temperature) , T_b T_w 가

(Bulk temperature)

Fig.9 3가 . Split vane

가 $3 D_h$ 가 $22 D_h$. $22 D_h$

가 . SG1 $7 D_h$

$22 D_h$. SG2 SG1

. 3가 $20 D_h$ Split vane

가 $20 D_h$ SG2 가 가 $20 D_h$

. Split vane

가 SG1 SG2 가

Yao [12]

(Blockage Ratio)

$$\frac{Nu}{Nu_0} = \left[1 + 5.55 \beta^2 e^{-0.13(z/D_h)} \right] \left[1 + S_w^2(z/D_h) \right]^{0.4} \quad (4)$$

β S_w Z/D_h

. Fig.10 (5) 3가

Fig.9

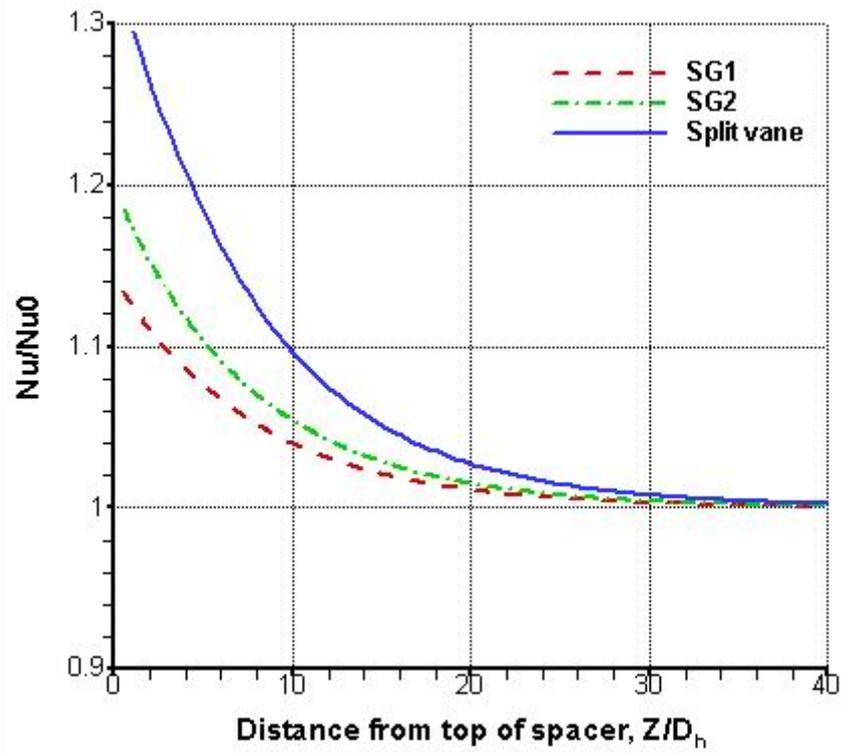


Fig.10 Nusselt number distributions for the different three mixing vanes calculated by Yao et al. correlation

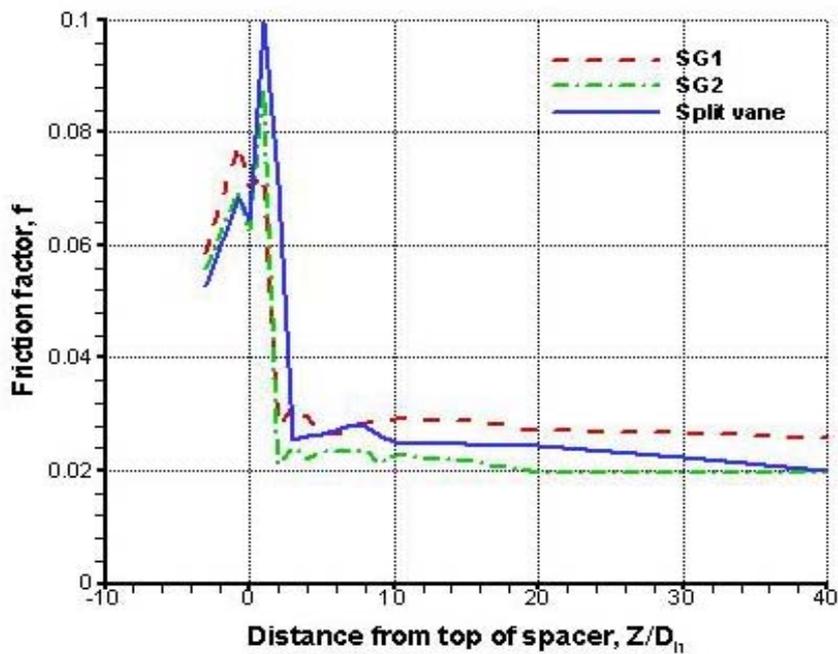


Fig.11 Friction factor distributions for the rod bundles

