



**1.**

dry-out

(CNSC: Canadian Nuclear Safety Commission)

가

가

가

가

MODTURC\_CLAS

2

가

1995 CNSC

가

CANDU

가 3

(AECL: Atomic

Energy of Canadian Limit)

CANDU-9

가

3

CRL(Chalk River Laboratory)

1/4-scale 3

가

CANDU-9

CANDU

CNSC가

MODTURC\_CLAS

3

CANDU-9

FLUENT, CFX

가

[1, 2]

SPEL

[1]

FLUENT

SPEL

**2. SPEL**

2.1 SPEL

SPEL CANDU

CANDU

CANDU

가

가

2

1-a

SPEL

1 SPEL  
 Boussinesq 가  
 $k$   
 52  
 SPEL 1-b  
 2  
 가

2.2 SPEL

0.5kg/s 10kW , SPEL 가  
 (buoyancy dominated flow) 2  
 ( 2-a, b) PHOENICS  
 SPEL  
 2DMOTH SPEL  
 가 ( 2-c, d)  
 가  
 가  
 SPEL  
 2.5

2.3

SPEL 가 ,  
 3가 (momentum dominated flow, mixed type  
 flow, buoyancy dominated flow) 3  
 (momentum dominated flow, 3-a),  
 (buoyancy dominated flow, 3-b),  
 (mixed type flow, 3-c).

2.4

4, 5, 6, SPEL ( )

( 4 )

(5, 10, 20kW) mixed type flow가 가

가

가

( 5 )

(5, 10, 20kW)

가

(momentum dominated flow) ( 6 ) 가

가

7, Ar, SPEL, Ar

가 0.5, buoyancy dominated flow mixed type flow 가

Ar 0.08, mixed type flow momentum dominated flow

Ar 가 가

8 2 가 Case 1 ( , )

8-a , 1,200

Case 2

3가 8-b 가

가 가,

3.

가 , ,  
 3 FLUENT .  
 SPEL ,  
 .  
 1. , ( momentum )  
 ) 3가 , momentum  
 dominated flow, mixed type flow buoyancy dominated flow .  
 2. ( ) 가 ,  
 가 가 .  
 3. 가 가 ,  
 가 , (5, 10, 20kW) ,  
 .  
 4. 가 가 가  
 , 가  
 가 가  
 5. 가 ,  
 .

[1] K. H. Bang, J. Y. Lee, S. O. Yu, M. W. Kim, and H. J. Kim, "A Three-Dimensional Analyses of Fluid Flow and Heat Transfer for Moderator Integrity Assessment in PHWR," Proceedings of the KNS Spring Meeting, May, Gwangju, 2002.

[2] C. Yoon, B. W. Rhee and B. J. Min, "Validation of a CFD Analysis Model for Predicting CANDU-6 Moderator Temperature Against SPEL Experiments," Proceedings of ICONE10, April 14-18, Virginia, USA, 2002.

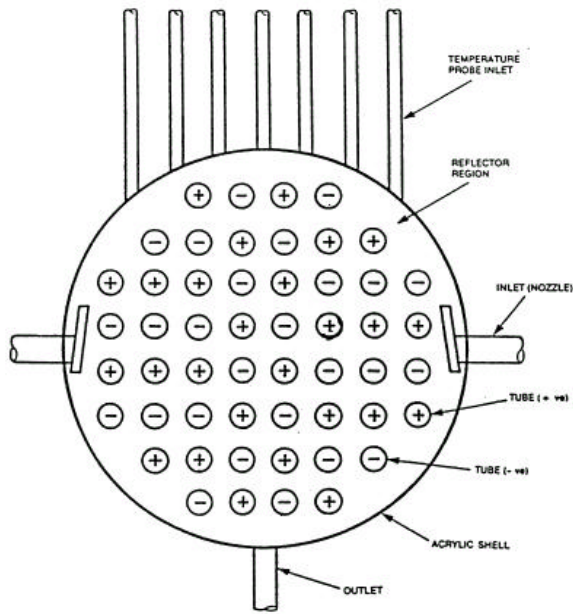
[3] D. Koroyannakis, R. D. Hepworth and G. Hendrie, "An Experimental Study of Combined Natural and Forced Convection Flow in a Cylindrical Tank," TDVI-382, AECL, 1983.

### 1. SPEL

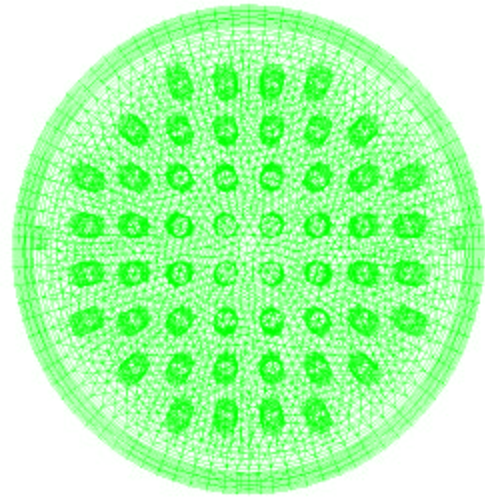
	ID, [m]	OD, [m]	L, [m]	Number	Comment
Test Vessel	0.74	0.775	0.254	1	
Heater Tubes		0.038	0.254	52	0.075m square pitch

### 2.

Case	T <sub>in</sub> , [ °C ]	V <sub>in</sub> , [m/s]	Heat Load, [kW]	Time, [sec]
1	30	0.13	10	0~2,500
2	30	$-1.311 \times 10^{-5}t + 4.567 \times 10^{-3}t + 0.11$	10	0~3,000



(a) SPEL

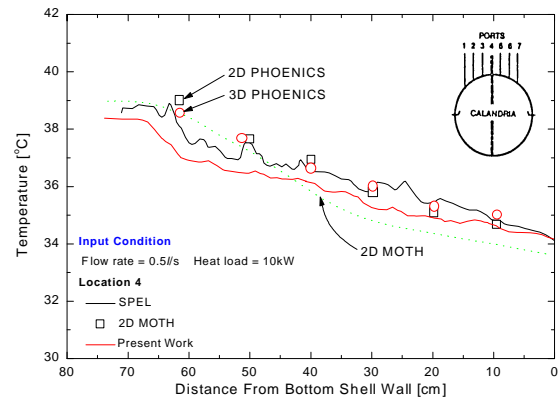
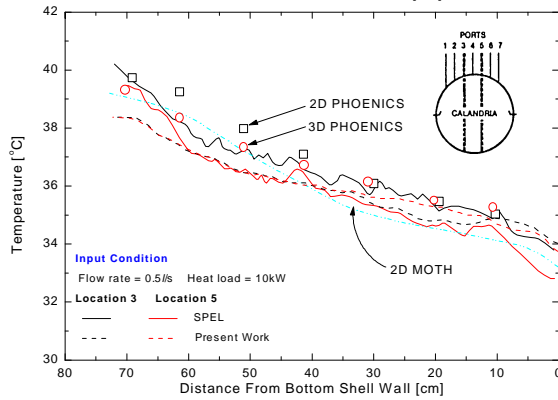
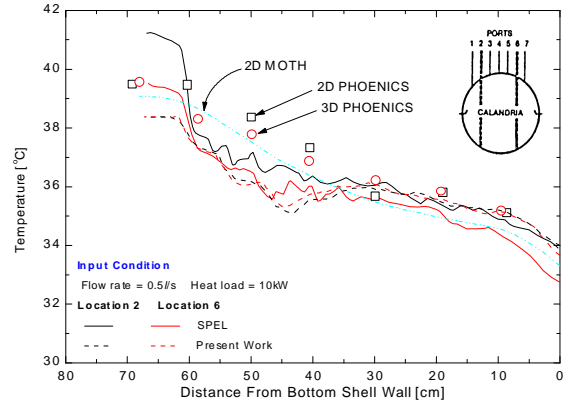
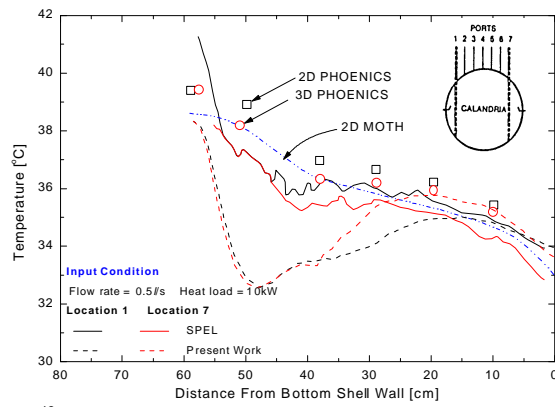


(b)

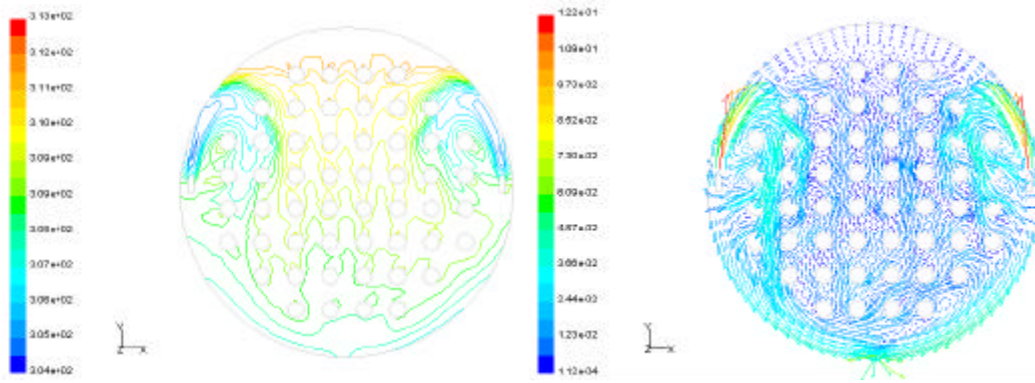
mesh

## 1. SPEL

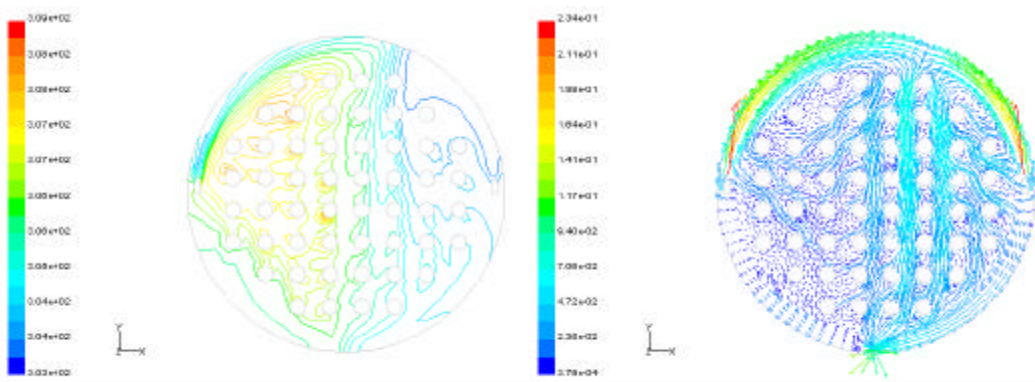
## mesh.



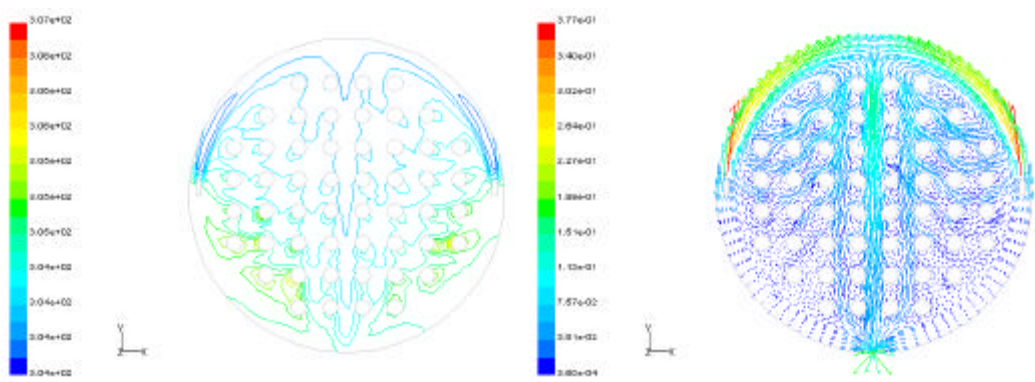
## 2. SPEL



(a) buoyancy dominated flow ( $V_{in}=0.13\text{m/s}$ ,  $T_{in}=30$  , Heat Load=10kW)

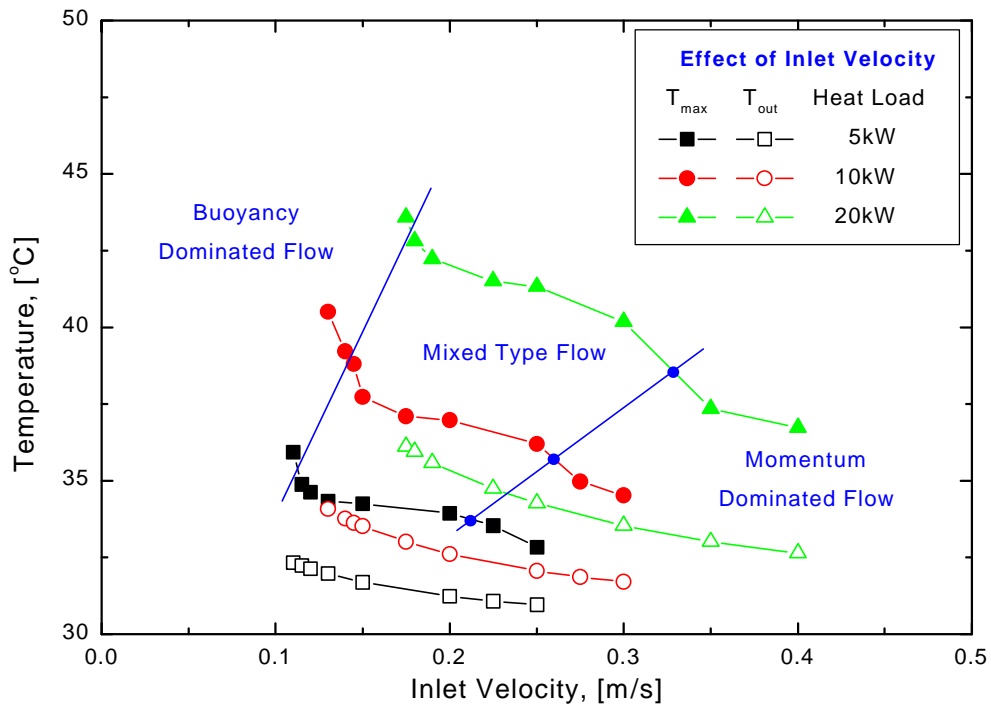


(b) mixed type flow ( $V_{in}=0.25\text{m/s}$ ,  $T_{in}=30$  , Heat Load=10kW)

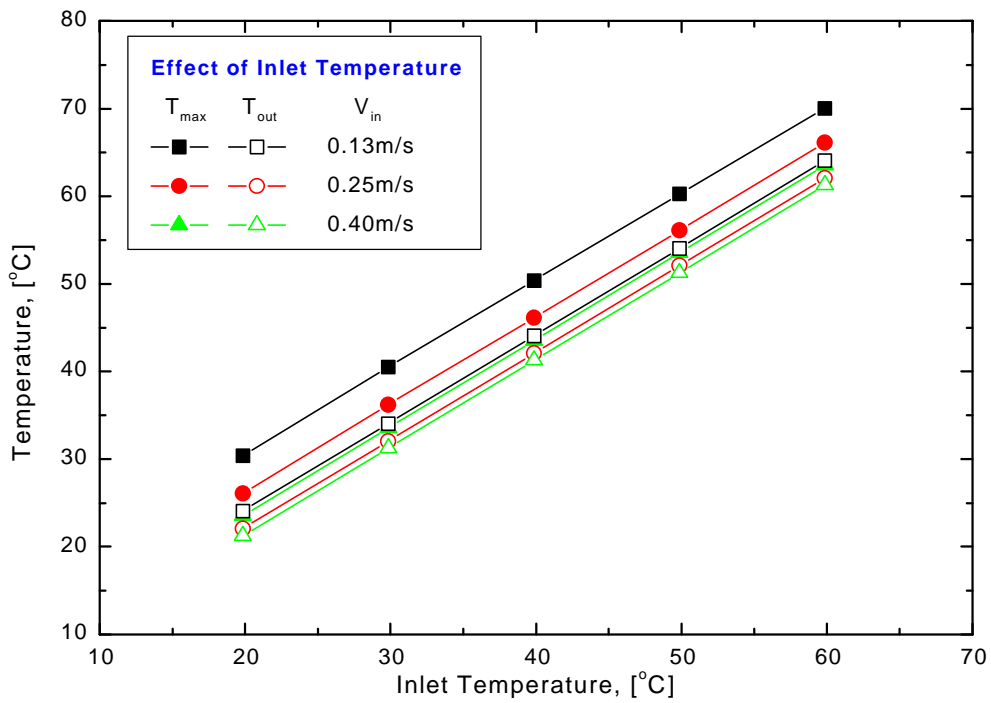


(c) momentum dominated flow ( $V_{in}=0.40\text{m/s}$ ,  $T_{in}=30$  , Heat Load=10kW)

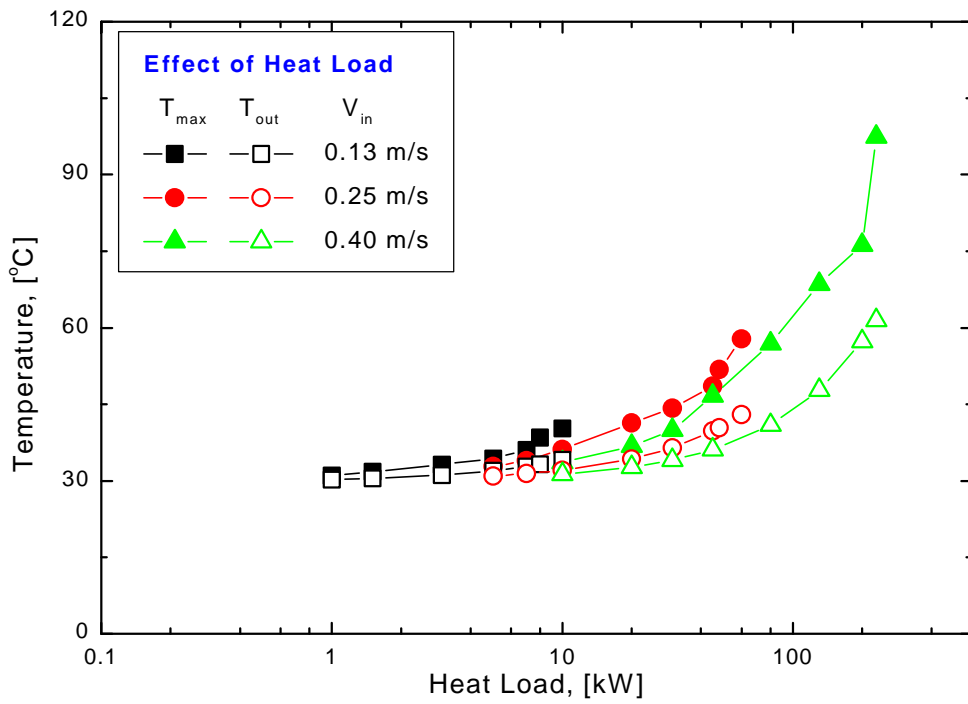




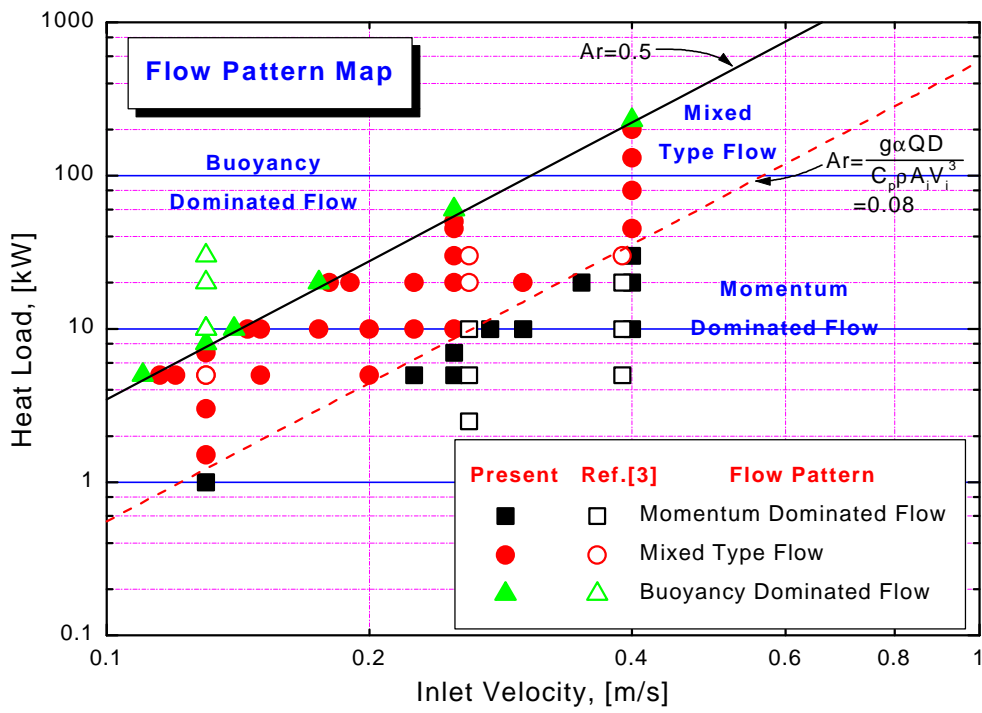
4.



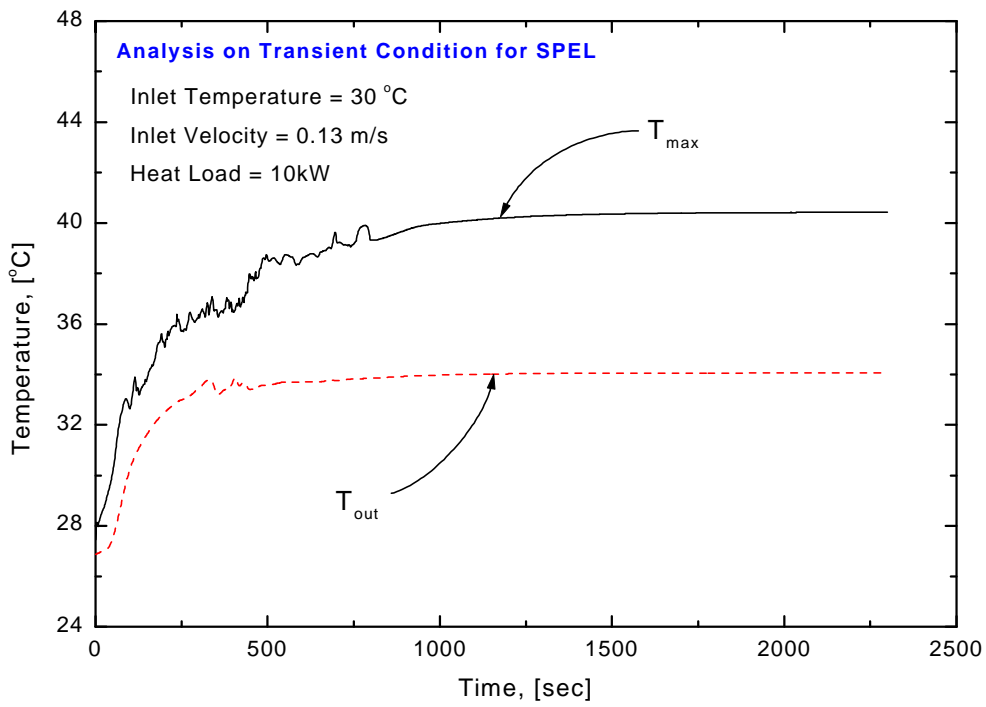
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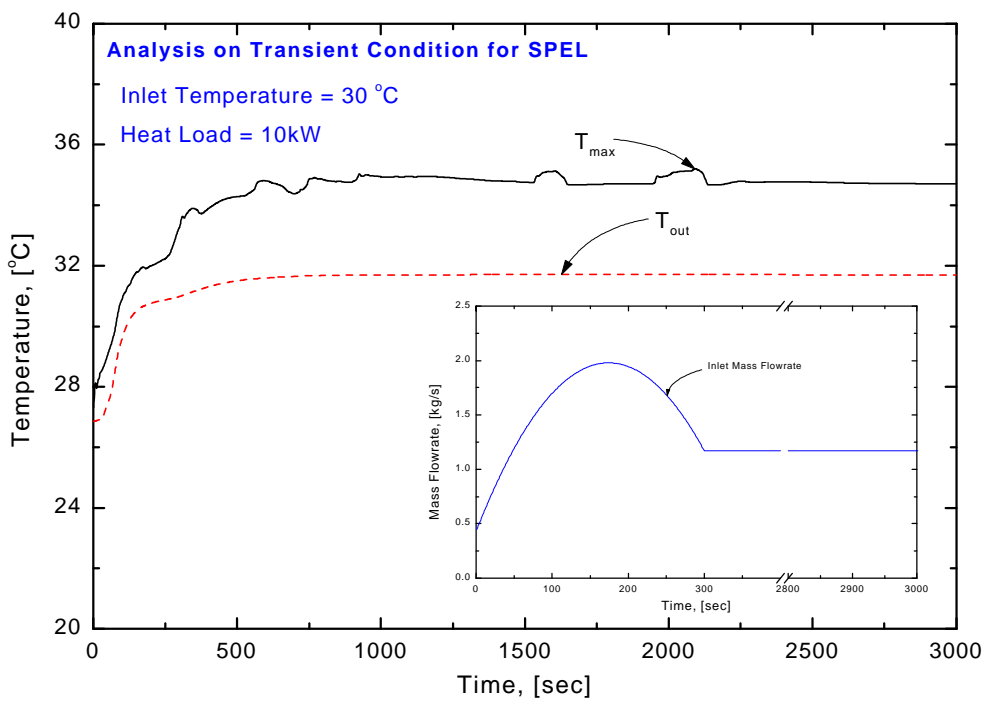
6.



7.



(a) Case 1



(b) Case 2