

× 가 가

Pressure Drop Performance Evaluation for Test Assemblies with the Newly Developed Top and Bottom Nozzles

, , , , ,

493

가 가 1
, 1 2

60.9 %, 90.4 %

가 가

가

가 A B 14.2 % 21.9 % , 가
10 %

A 가 B

Abstract

To perform the hydraulic test for the newly developed top and bottom nozzles, two kinds of test assemblies were manufactured i.e. one is the test assembly which has the newly developed top and bottom nozzles and the other is Guardian test assembly which is commercially in mass production now. The test results show that the test assembly with one top nozzle and two bottom nozzles has a greater pressure loss coefficient than Guardian test assembly by 60.9 % and 90.4 % at the bottom nozzle location. This cause is due to the debris filtering plate for bottom nozzle to improve a filtering efficiency against foreign material. In the region of mid grid and top nozzle, there is no difference in pressure loss coefficient between the test assemblies since the component features in these regions are very similar or same each other. The loss coefficients are 14.2 % and 21.9 % for model A and B respectively in the scale of test assembly, and the value would be within the 10 % in the scale of real fuel assembly. As a result of hydraulic performance evaluation, Model A is superior to Model B.

1.

1 10

가

78mm×78mm

15.88mm

DF1

가

DF2 ~DF7

가

가

DF4 ~DF7

가

DF2

, DF3 ~DF7

가

5×5

DF8 ~ DF10

가

DF8

가

DF9

, DF10

SIEMENS

가

3

2

(2)

[1,2].

가

1

(3)

[3].

가

2

3

4

가

가

(NFI)

NFI 가
가

2.

2.1

NFI Kumatory

5

6

가 70 °C

가

40 °C

1

(pressure tap)

7

21

(differential pressure transducer output) 10

가

3

2

3

가

2

[4]

2.2

8

[5].

$$\frac{p_1}{\rho} + \frac{1}{2} \mathbf{a}_1 V_1^2 + gz_1 = \frac{p_2}{\rho} + \frac{1}{2} \mathbf{a}_2 V_2^2 + gz_2 + h_{losses}$$

(1)

p , ρ , V , g , z

1, 2

가

가

\mathbf{a}

(roughness)

60°C

Reynold (Re)

40°C,

47,000 ~ 148,000

(1)

$$V_{in} = FR * 0.001 / (60 * S_{in}) \quad (2)$$

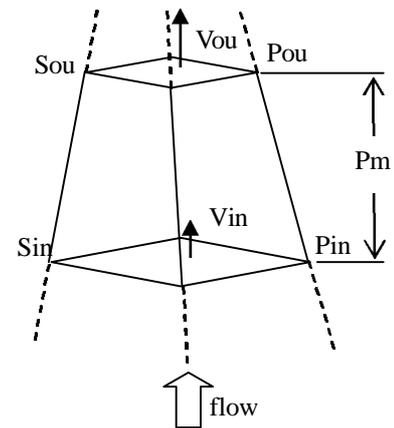
$$V_{out} = FR * 0.001 / (60 * S_{out})$$

$$P = (P_{in} + V_{in}^2 / 2g) - (P_{out} + V_{out}^2 / 2g) \quad (3)$$

$$= (P_{in} - P_{out}) - (V_{out}^2 - V_{in}^2) / 2g$$

$$= P_m - (V_{out}^2 - V_{in}^2) / 2g$$

$$K_{in} = P * 2g / V_{in}^2 \quad (4)$$



P: static pressure drop(kgf/m²)

P_m: measured pressure drop(kgf/m²)

ρ: water density depended on the temperature(kg/m³)

g: gravity (m/sec²)

P_{in}: static head in the upstream region (kgf/m²)

P_{out}: static head in the downstream region (kgf/m²)

V_{in}: axial flow velocity in the upstream region (m/sec)

V_{out}: axial flow velocity in the downstream region (m/sec)

S_{in}: cross-sectional flow area in the upstream region (m²)

S_{out}: cross-sectional flow area in the downstream region (m²)

FR: flow rate (litter/min.)

3

2

$$K_x = DP_x \frac{2gA^2}{\rho Q^2} - f \frac{l_x}{De} + \left[\left(\frac{A}{A_d} \right)^2 - \left(\frac{A}{A_u} \right)^2 \right] \quad (5)$$

A : Test flow area of FA (cross-section area of flow housing cross section area of rods in bare rodded region), cm²

ρ : Fluid density, kg/cm³

ν : Fluid viscosity of area A, m^2/sec

Q : Fluid flow rate, /min

Re: Reynolds Number

De: Equivalent hydraulic diameter of cross-section area A, cm

f : Friction factor, $0.186 * Re^{-0.2}$ (Re : Reynolds number)

DP_x : Pressure differential measured by differential pressure transducer "x", kg/cm^2

K_x : Pressure loss coefficient derived from DP_x

A_U : Flow area at upstream pressure tap of DP_x

A_D : Flow area at downstream pressure tap of DP_x

가

(Re)

$$Re = \frac{Q De}{A \nu} \quad (6)$$

(curve fitting)

$$K = a * Re^b \quad (7)$$

a, b (7)

2

3.1 (Inlet Region)

7

가

A

B

A

B

, 가

가

9

가 500,000

A

60.9%,

B

90.4%

가

가

A

가

B

가

가

$$V_2 = \frac{S_1}{S_2} V_1 \quad (8)$$

S

가

, 1, 2

a 가

, (8) (1)

A

B

(5)

$$K_x = DP_2 \frac{2gA_2^2}{rQ^2} - f \frac{17.43}{1.1379} + 0.7807 \quad (9)$$

3.2 (Inlet Region)

[(ΔP-10) - (ΔP-9) + (ΔP-8)] 가 7 가
 가 A B
 가
 10 3
 가 500,000 A 가 0.9 %, B
 0.1%

(5)

$$K_{outlet} = DP_{outlet} \frac{2gA_3^2}{rQ^2} - f \frac{14.43}{1.1235} + 0.5283 \quad (10)$$

3.3

가 500,000
 A 가 14.2 %, B 21.9 %

$$K_{10} = DP_{10} \frac{2gA_3^2}{rQ^2} - f \frac{129.87}{1.1235} + 0.2728 \quad (11)$$

가

3.1

A

B

4.

가 ,
 가 1 가 1
 가 2 가
 , NF1
 가

가
 가 14.2 % 21.9 %
 10 % [6]
 가 가
 A 가 B

5.

[1] “ ”, 2001
 , 2001.

[2] “ 가”, 2001
 , 2001.

[3] “ 가”, 2002
 , 2001.

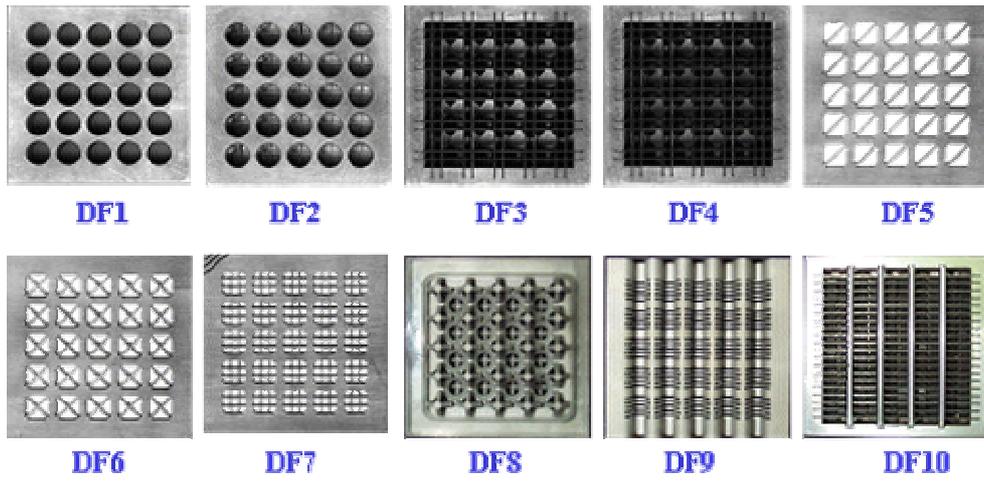
[4] NFK-MM-0210037, “The Test Report of the Debris Filter Test and Pressure Drop Test for KNFC Newly Developed Top and Bottom Nozzle”, Nov., 2002, NFI

[5] F.M. White, “Fluid Mechanics”, 1995, McGraw-Hill

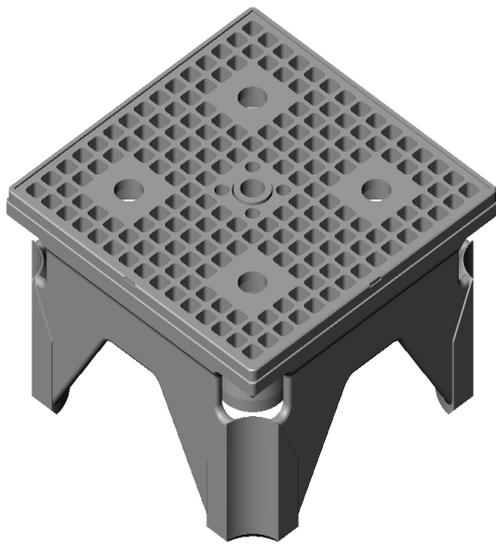
[6] “ ”, 2003
 , 2003. 5.

1.

Item		Setting Value
Temperature (° C)		40, 60
Pressure		Atmospheric
Flow Rate (litter/min)	During flow rate up	4000 to 9000 (increase by 500)
	During flow rate down	8750 to 4250 (decrease by 500)
Reynold ' s Number		Around 47,000 ~ 148,000



1.



2-A.



2-B. Type A(



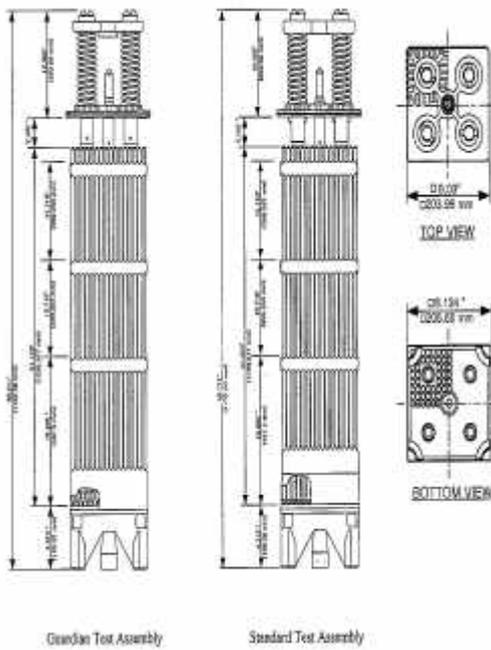
2-C.

2.

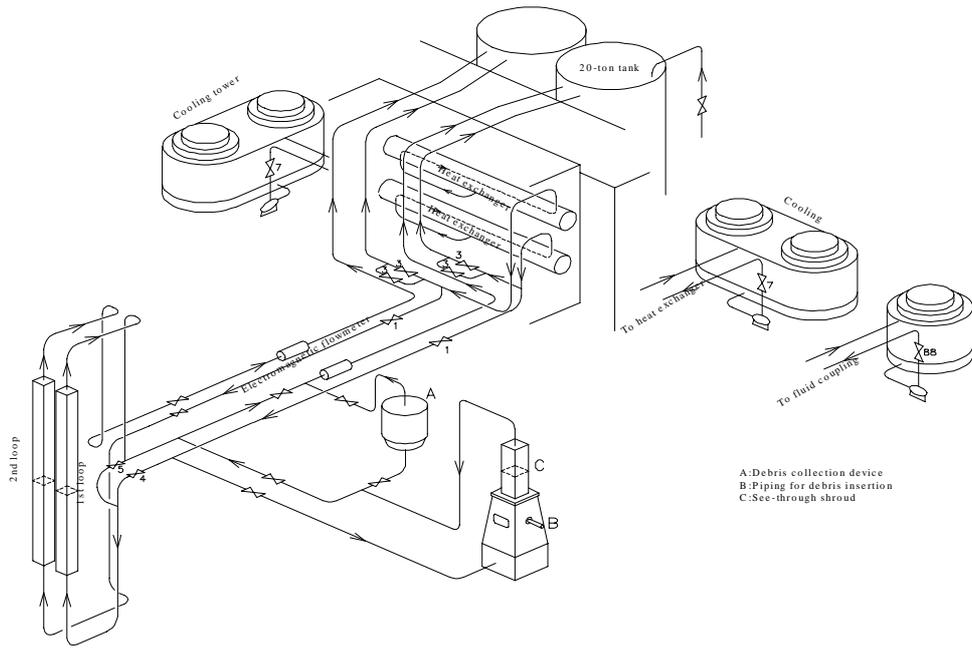
가



3.

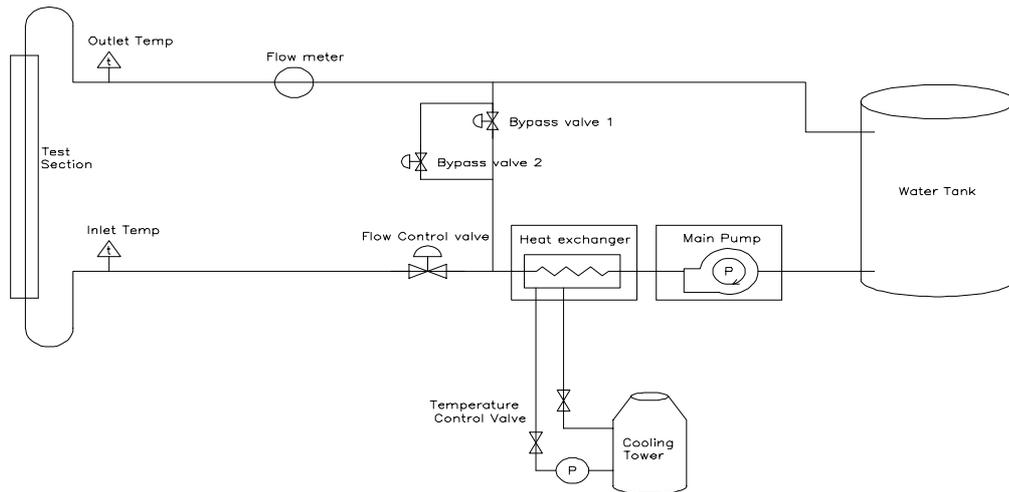


4.

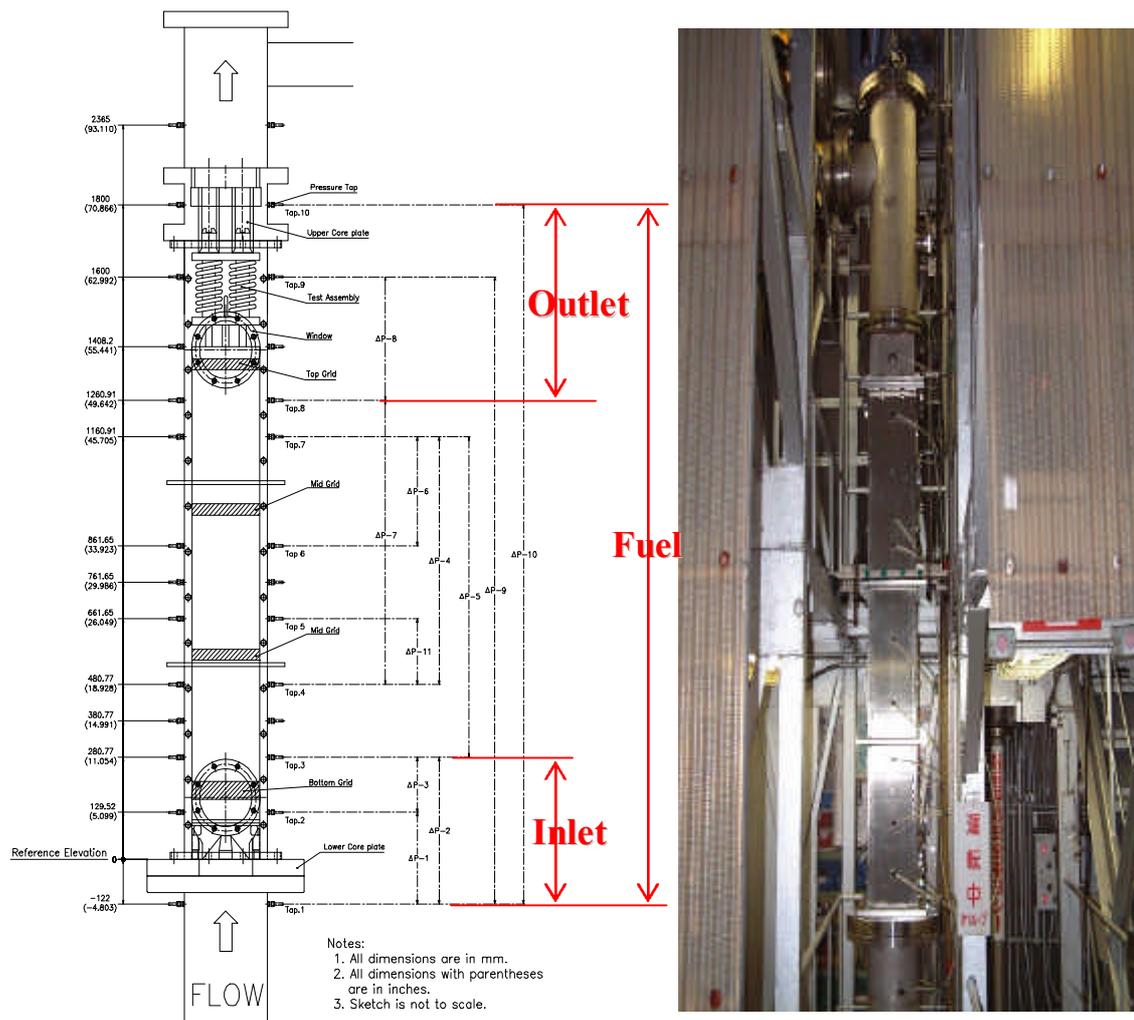


5.

FLOW DIAGRAM of NFI Kumatori Loop



6.



7. Pressure tap installation location and measurement region.

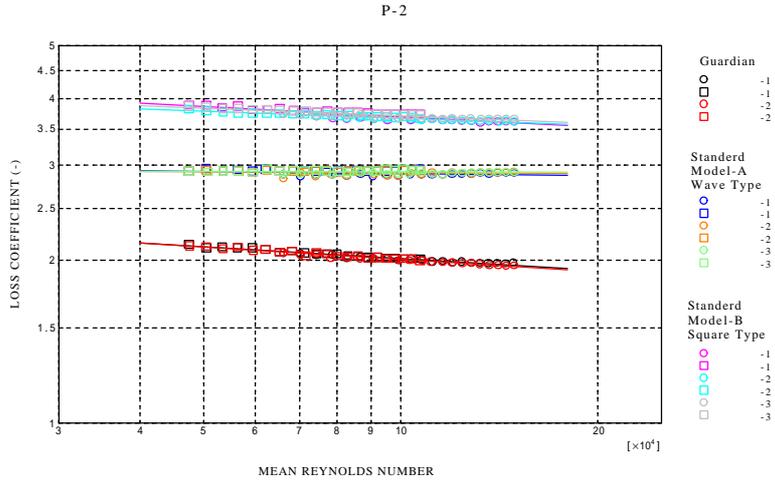


8-A. Pressure drop measurement

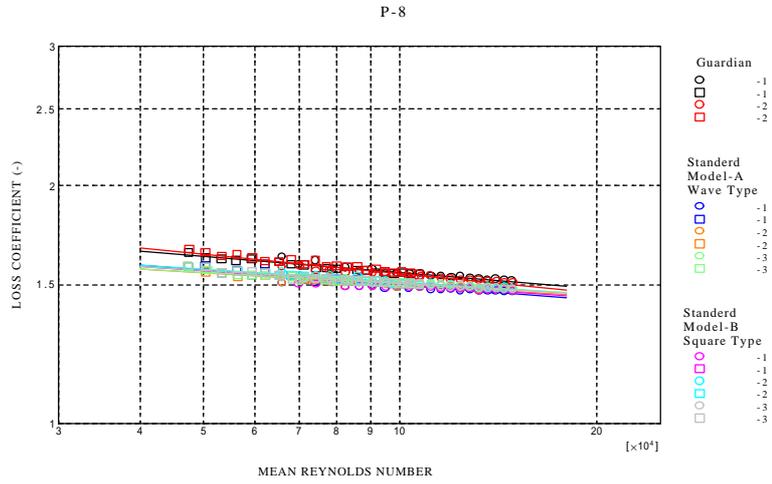


8-B. Flow rate measurement

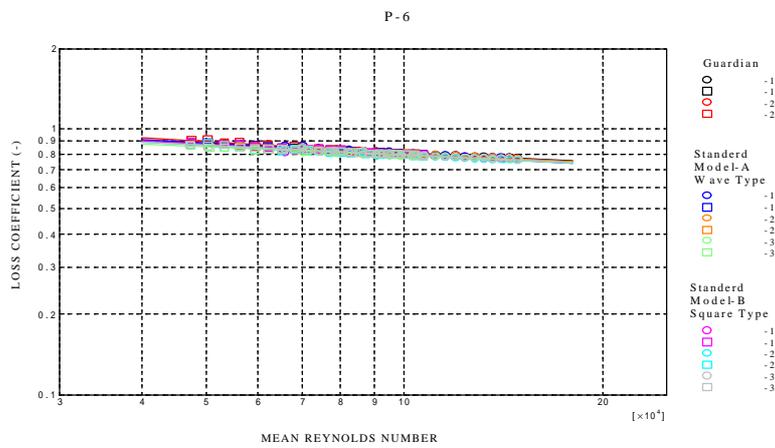
8. Flow Chart of Data acquisition system



9. (P-2,)



10. (P-8,)



11. (P-6,)