

## Optimal Air Flow Rate and O<sub>2</sub> Concentration of UO<sub>2</sub> Pellet Vol-oxidation

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### 1. Introduction

In the ACP (the Advanced Spent Fuel Conditioning Process), UO<sub>2</sub> pellet is converted into U<sub>3</sub>O<sub>8</sub> powder since U<sub>3</sub>O<sub>8</sub> powder is much desirable form for the following metallization process. The 20 kg UHM/batch size voloxidizer is under development in KAERI. Prior to the bulky and tricky 20 kg batch experiment, we tried to find the optimal condition of air flow rate and O<sub>2</sub> concentration, which provides the maximum oxidation rate and prevents scattering of the fine U<sub>3</sub>O<sub>8</sub> powder in the reactor caused by the excessive air flow rate, by using the small sized oxidation reactor. This reactor is similar in structure with the full sized one. Also the particle size of oxidized U<sub>3</sub>O<sub>8</sub> powder was measured using the particle size analyzer.

### 2. Experiment and Result

#### 2.1 Experiment setup

Experiment setup of vol-oxidation device and its schematics are shown in Fig. 1 and Fig. 2. The reactor is made by SUS 304L, and its size is 100 mm in radius and 210 mm in height. It is temperature controlled up to 1200°C. It is equipped with the impeller and handle which simulate the motorized impeller of the full sized voloxidizer [1]. This motorized impeller makes the over 99% recovery rate of U<sub>3</sub>O<sub>8</sub> powder.



Figure 1. Experimental setup

#### 2.2 Experimental method

The irradiated natural uranium pellets of CANDU fuel are used [2]. A temperature is controlled to keep 500°C which is revealed as the best temperature to obtain the maximum oxidation rate [2]. The oxidation time is

measured while varying the air flow rate and O<sub>2</sub> concentration.

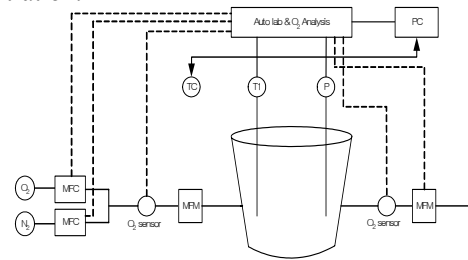


Figure 2. Schematics of the experiment setup

Also to check the powder scattering, the outlet port made by visible plastic pipe is monitored whether the scattered powder exists while varying the air flow rate. O<sub>2</sub> concentration was varied in the range of 21% to 40%. The theoretical amount of air required to oxidize five pellets is calculated to be 35,520 cc. Also from a series of experiments the oxidation time was revealed to be roughly 10-40 min. The logical air flow rate was assumed to be 1500 cpm (=35,520 cc / 24 min). Thus, the air flow rate was varied 500 through 2500 cpm.

#### 2.3 Experimental result

Fig. 3 shows UO<sub>2</sub> pellets and oxidized U<sub>3</sub>O<sub>8</sub> powder. Fig.4 shows the oxidation time with various O<sub>2</sub> concentrations and the air flow rates. As can be seen in the figure the oxidation time is reduced as the O<sub>2</sub> concentration increase. However the excessive O<sub>2</sub> concentration may cause safety problem and in this regards, the optimal concentration was set 40% [2]. The oxidation time decreases with the increased flow rate and the optimal flow rate is revealed to be 2000 cpm regardless of changing O<sub>2</sub> concentration. On the contrary, the oxidation time increases with larger flow rate of 2000 cpm. This can be explained that thin oxidation film is formed at the surface of pellets due to rapid oxidation and it interferes with the direct contact of O<sub>2</sub> with the inner part of the pellet.

Throughout the experiments, the visible outlet port was monitored whether the powder scatters. No scattering was monitored. This shows that the powder does not scatter in the given geometry of the reactor throughout the range of the air flow rates.

Whether the UO<sub>2</sub> pellet is fully changed to U<sub>3</sub>O<sub>8</sub> powder, XRD (X-Ray Diffraction) and TGA (Thermogravimetric Analysis) [4] have performed. The results are shown in Fig.5 and 6. The pattern shown in Fig.5 represents the typical XRD of U<sub>3</sub>O<sub>8</sub>, which shows

that the  $\text{UO}_2$  pellets are fully converted to  $\text{U}_3\text{O}_8$ . Also as can be seen in Fig.6, the weight change of the sample powder can not be found while heating it up to  $700^\circ\text{C}$ . This shows that the powder has already been fully changed to  $\text{U}_3\text{O}_8$ .



Figure 3.  $\text{UO}_2$  pellets and  $\text{U}_3\text{O}_8$  powders of a vol-oxidation experiment

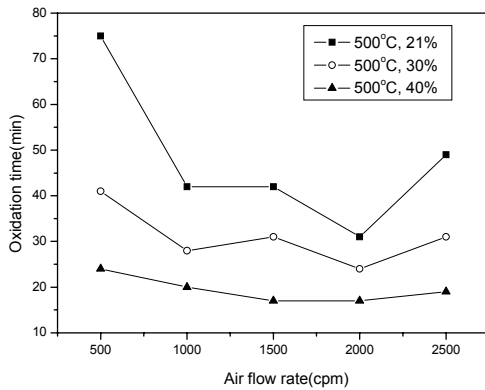


Figure 4. The oxidation time classified by the air flow rate and  $\text{O}_2$  concentration

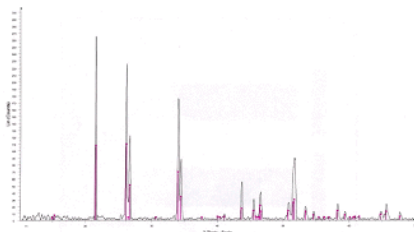


Figure 5. The analysis result of XRD in a vol-oxidation experiment

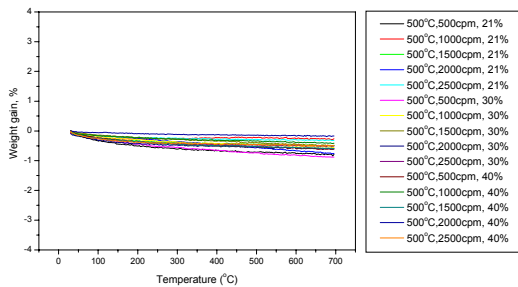


Figure 6. The analysis result of TGA in a vol-oxidation experiment

The particle size of  $\text{U}_3\text{O}_8$  powder is shown in Fig 7. The average particle size is about  $50 \mu\text{m}$ . In the metallization process, the desirable particle sizes of  $\text{U}_3\text{O}_8$  powder is in the range of  $20 \mu\text{m}$  to  $60 \mu\text{m}$  [1,5].

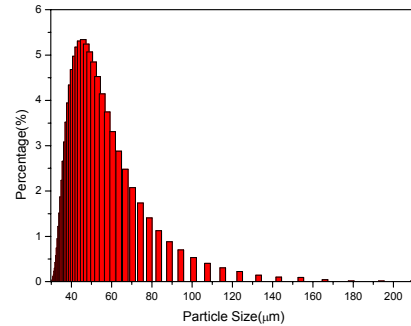


Figure 7. The average particle sizes of  $\text{U}_3\text{O}_8$  powders

### 3. Conclusion

The optimal air flow rates and the  $\text{O}_2$  concentration for vol-oxidation process has been investigated from a series of the oxidation experiments of  $\text{UO}_2$  pellets using the small reactor. Also TGA and XRD analysis performed to check whether the  $\text{UO}_2$  pellets are fully oxidized. The results shows that the optimal condition, which minimizes the oxidation time, are 2000 cpm of air flow rate and 40% of  $\text{O}_2$  concentration at  $500^\circ\text{C}$ . Also all the  $\text{UO}_2$  pellets were found to be fully oxidized to  $\text{U}_3\text{O}_8$ . This will be used to find out the optimal condition of the 20 kg/batch size vol-oxidation reactor.

### Acknowledgement

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