

[원전 적용을 위한 CFD 스케일 해석 기술 및 실험]

CFD Scale Analysis Techniques and Experiments for Nuclear Applications

원자로계통 고정밀 열수력 실험 및 모델 검증 연구

High-precision TH Experiments and Model Validation for Nuclear Reactor System

2023. 5. 17.

김석



Korea Atomic Energy
Research Institute

OUTLINE



01 Introduction

02 Natural Convection in a Pool

03 Rod-bundle Flow Behavior

04 Summary

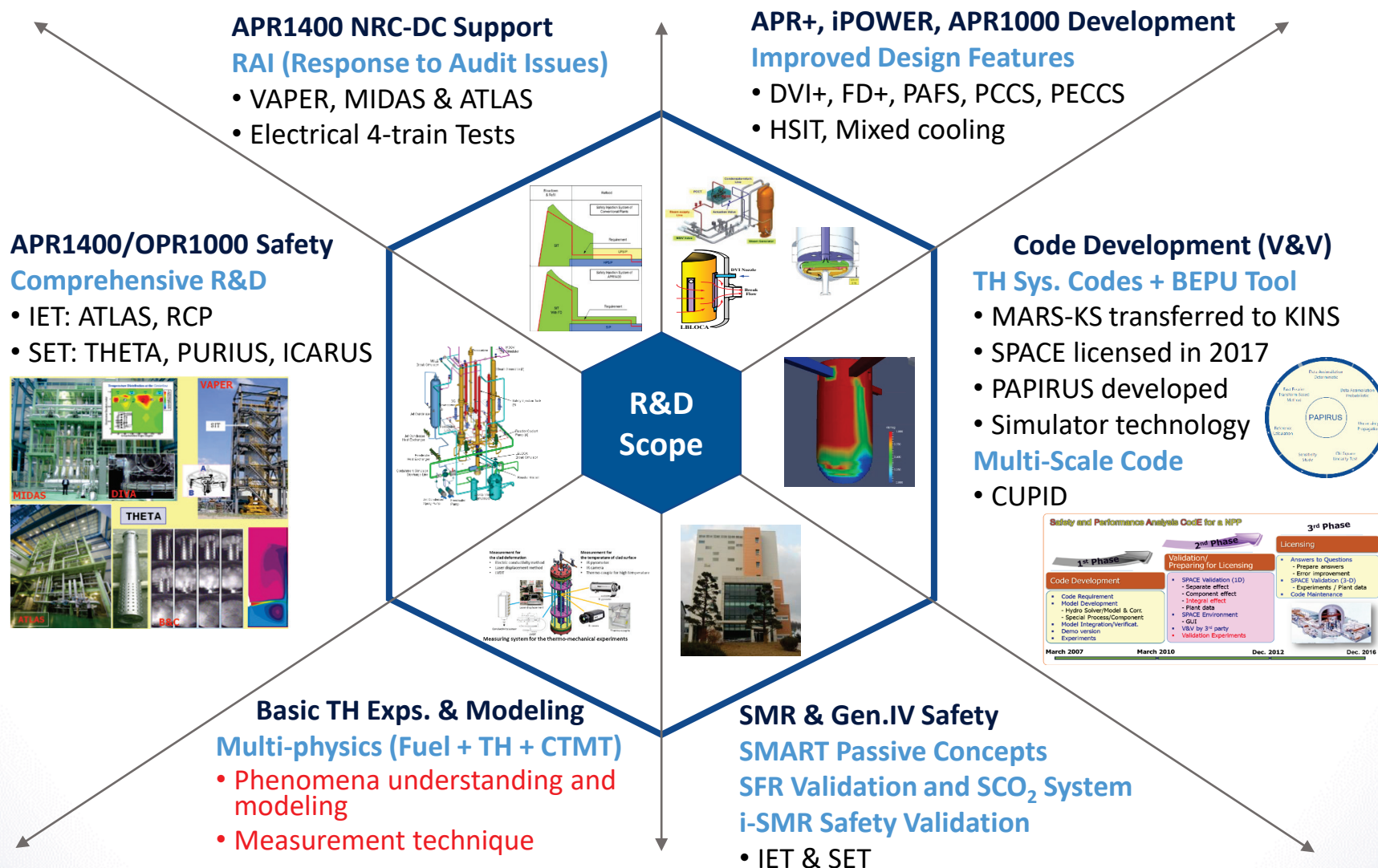
Introduction |

Thermal-Hydraulics R&D

Requirements for CFD-grade experiments for TH

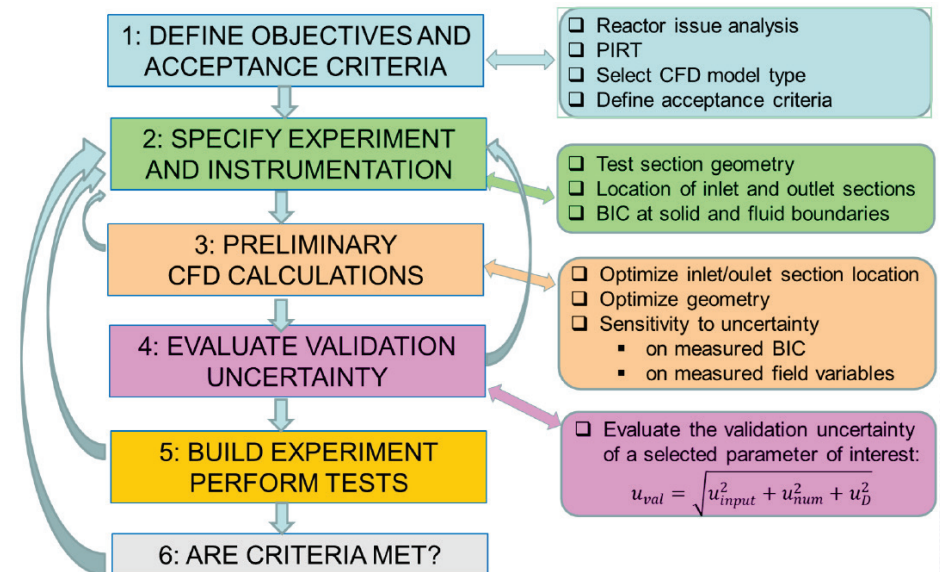
01 Introduction (1)

❖ Thermal-Hydraulics R&D of RSSRD



❖ Requirements for CFD-grade experiments for TH

- What is a CFD-grade experiment?
 - Validate of CFD: give an information on the quality of physical models
 - Determine CFD model uncertainty
 - Allow BEPU
- Scope
 - BIC and physical properties of fluid and solid
 - Flow parameter measurement
 - Measurement uncertainty



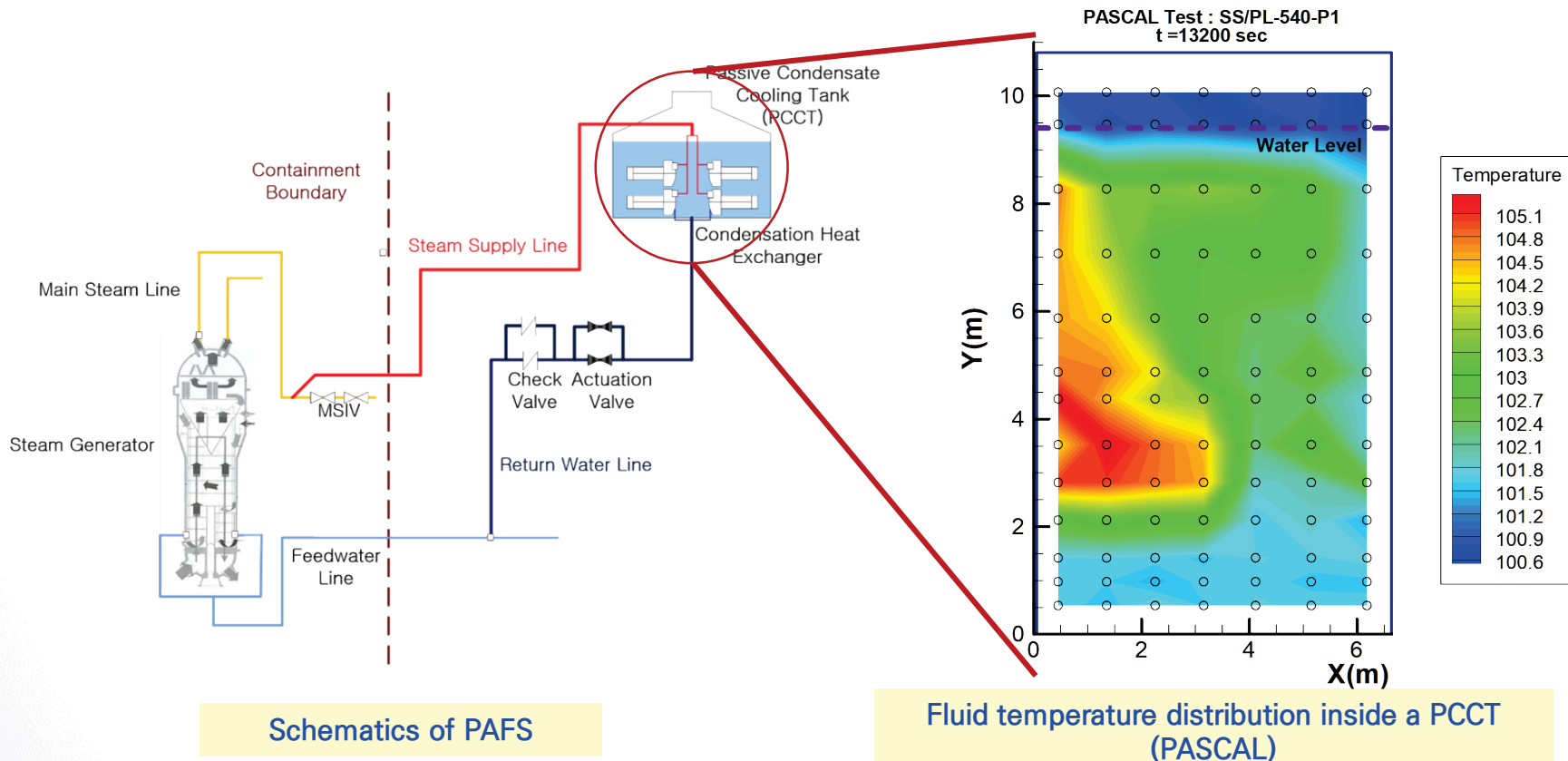
Natural Convection in a Pool

Local Thermal Mixing Characteristics inside a
PCCT

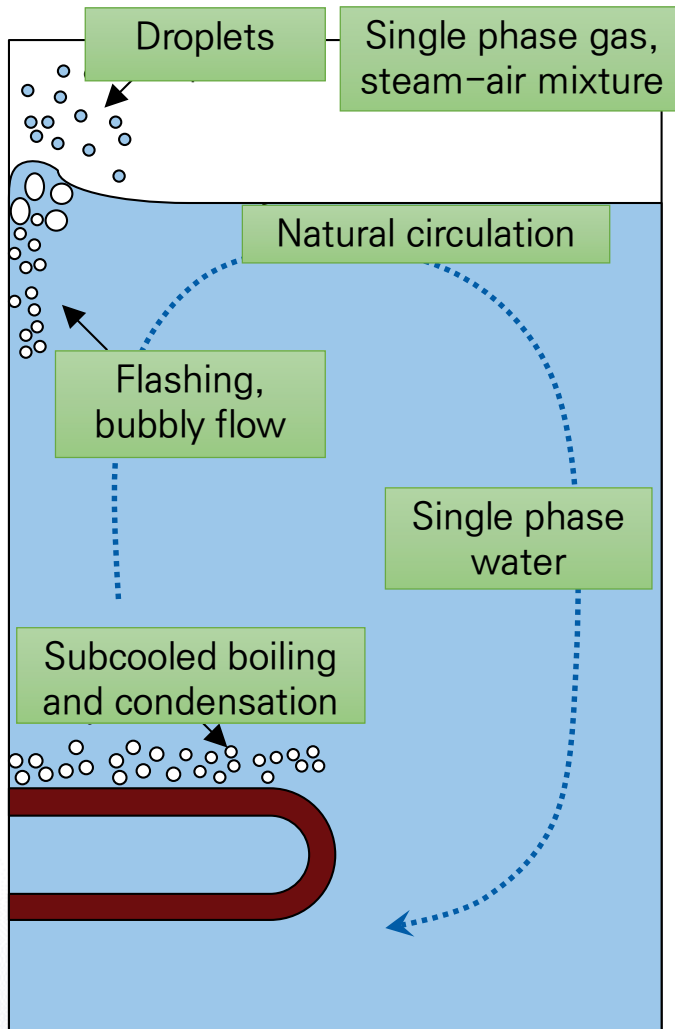
CUPID Code Analysis

Small-sized Pool Experiment

❖ Local Thermal Mixing Characteristics inside a PCCT



❖ Local Thermal Mixing Characteristics inside a PCCT

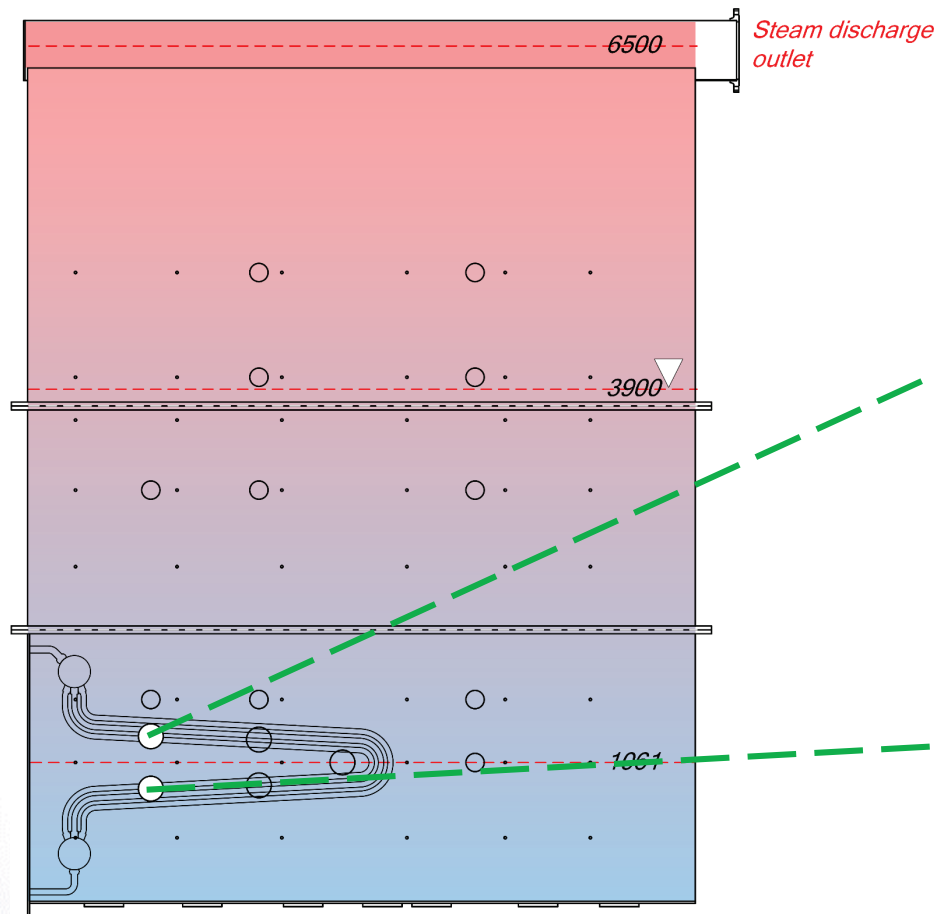


- Complexity in physical phenomena
 - Single- and two-phase natural circulation
 - Subcooled boiling and condensation
 - Flashing
 - Evaporation on the free surface
- Difficulty in numerical analysis
 - Various flow patterns
 - Phase change under low pressure state
 - Long transient time over 30,000 sec.
 - Complicated geometry of the heat exchanger and its supporting structure

Numerical Analysis of the Passive Condensation Cooling Tank (PCCT) using the CUPID Code, S.J. Lee et al., CFD4NRS-4, 2012

02 Natural Convection in a Pool (2)

❖ Local Thermal Mixing Characteristics inside a PCCT



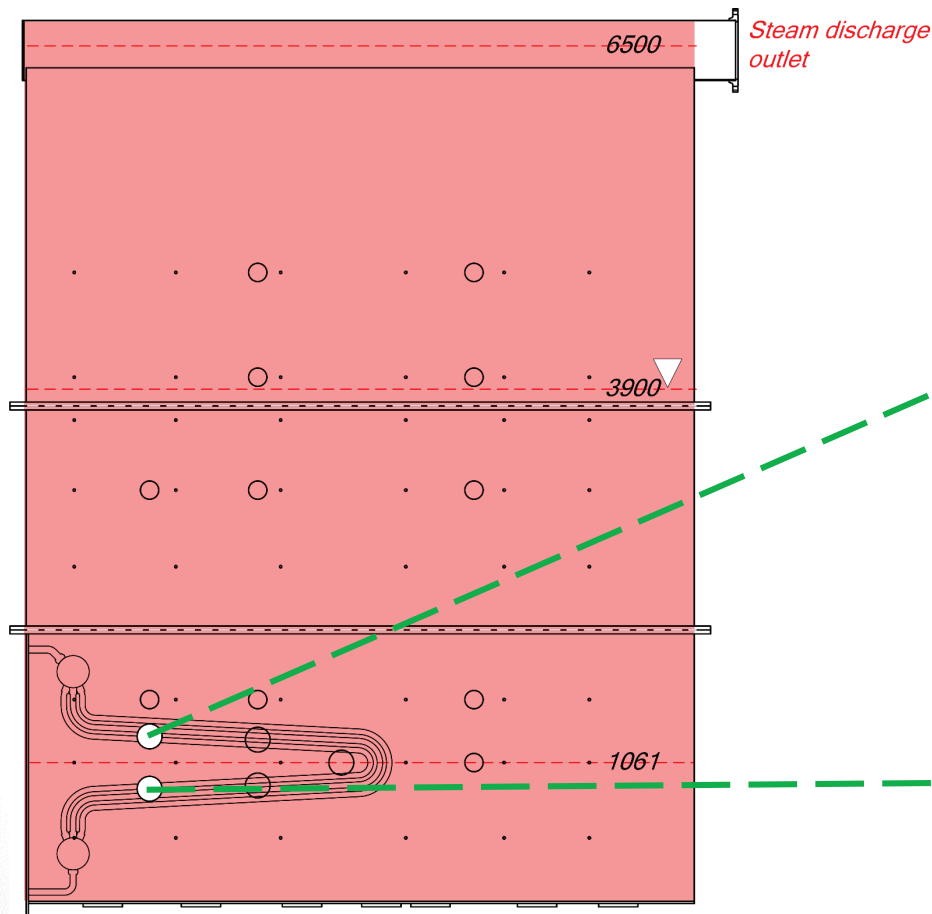
Schematics of ATLAS-PAFS PCCT

Subcooled boiling and condensation

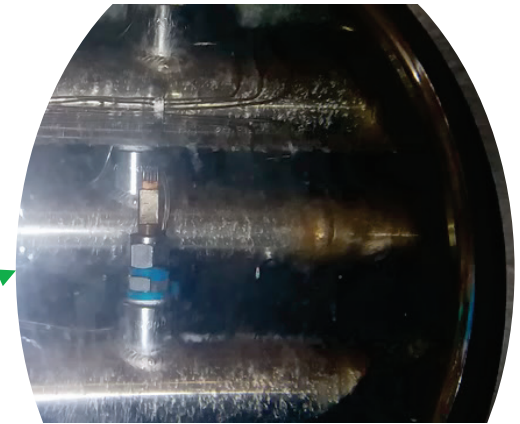
Fluid temperature around the PCHX : $\sim 82^{\circ}\text{C}$

02 Natural Convection in a Pool (2)

❖ Local Thermal Mixing Characteristics inside a PCCT



Schematics of ATLAS-PAFS PCCT



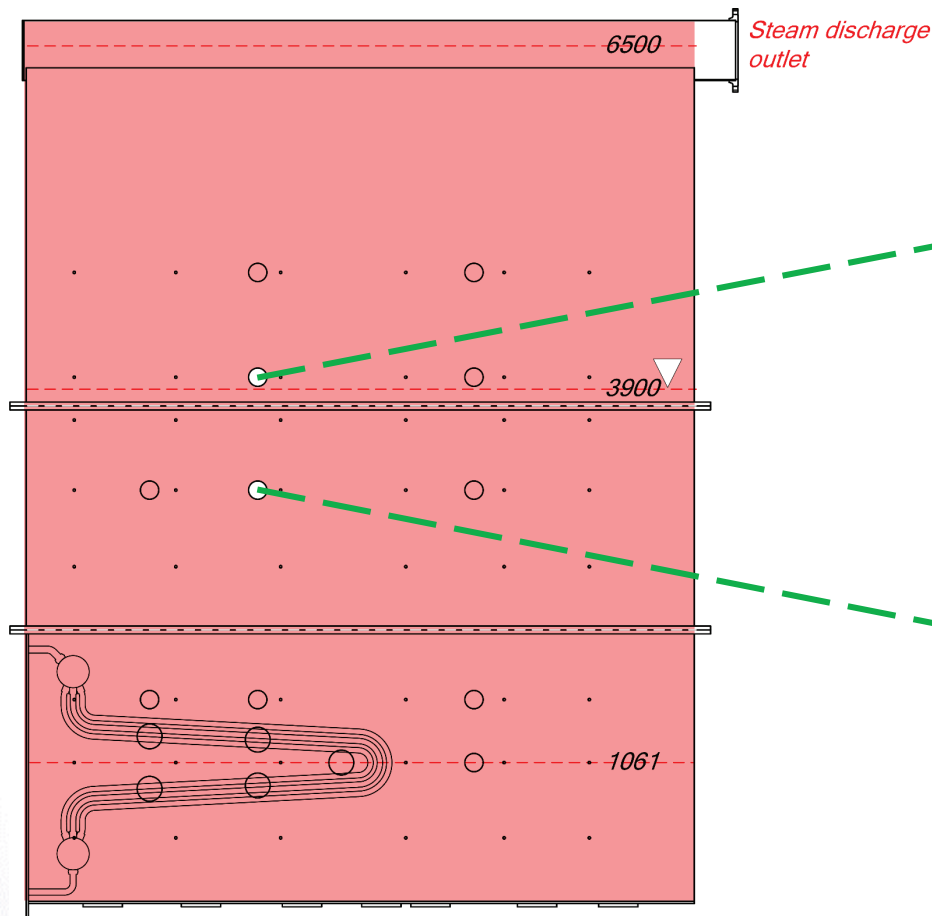
Subcooled boiling and condensation



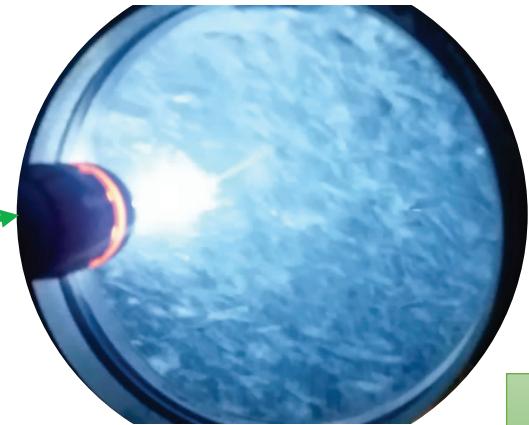
Fluid temperature around the PCHX : $\sim 100\text{ }^{\circ}\text{C}$

02 Natural Convection in a Pool (2)

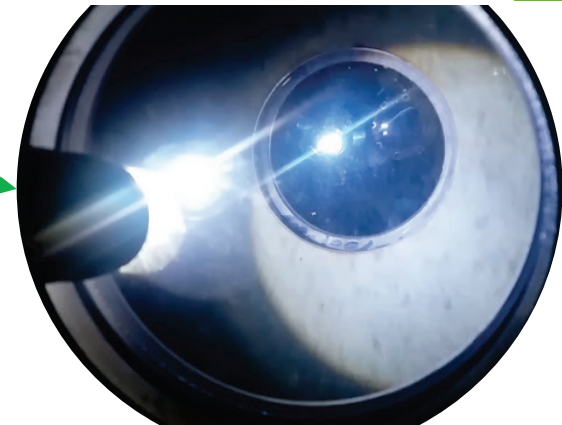
❖ Local Thermal Mixing Characteristics inside a PCCT



Schematics of ATLAS-PAFS PCCT

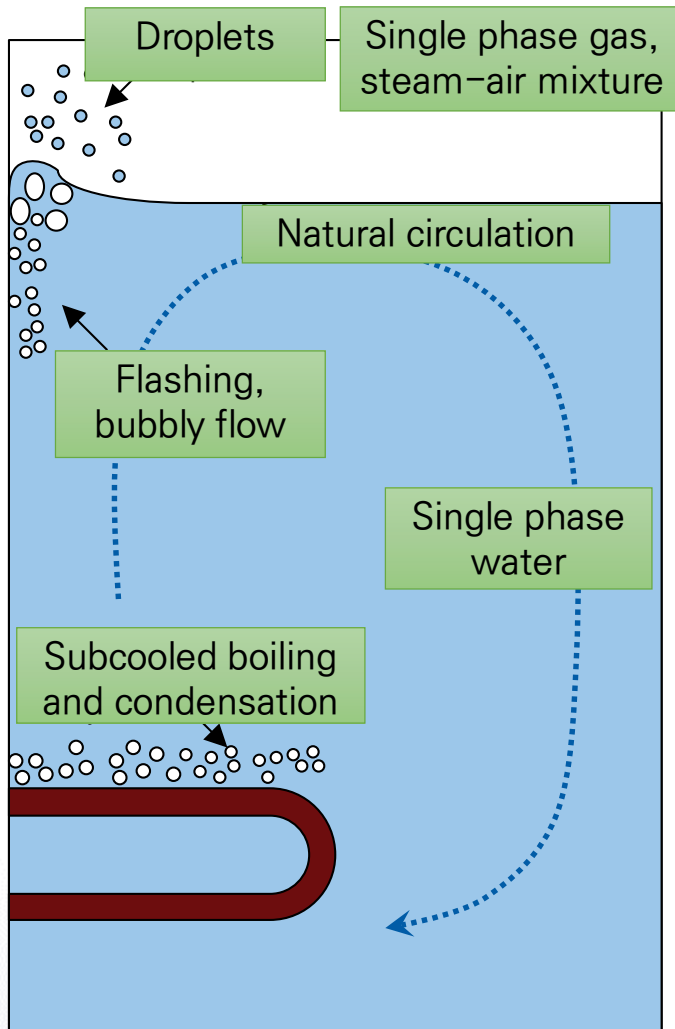


Flashing, bubbly flow



Fluid temperature around the PCHX : ~ 100 °C

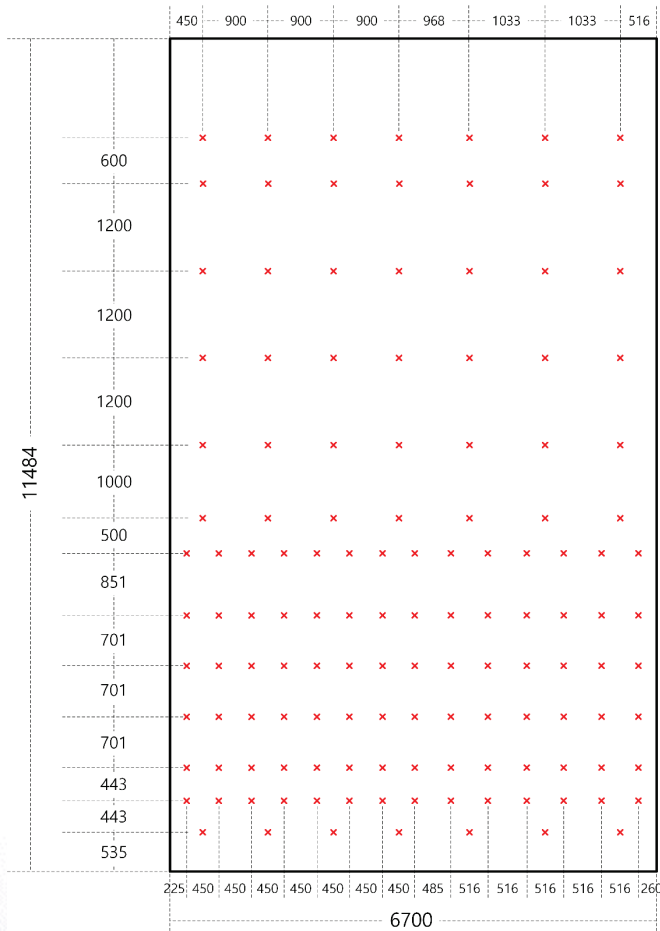
❖ Local Thermal Mixing Characteristics inside a PCCT



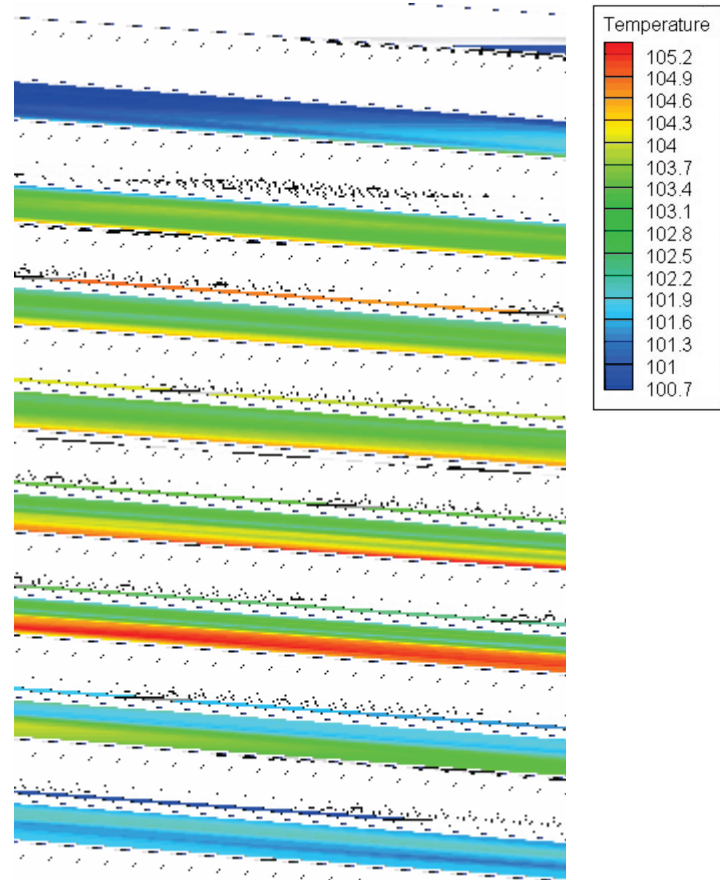
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Numerical Analysis of the Passive Condensation Cooling Tank (PCCT) using the CUPID Code, S.J. Lee et al., CFD4NRS-4, 2012

❖ Local Thermal Mixing Characteristics inside a PCCT



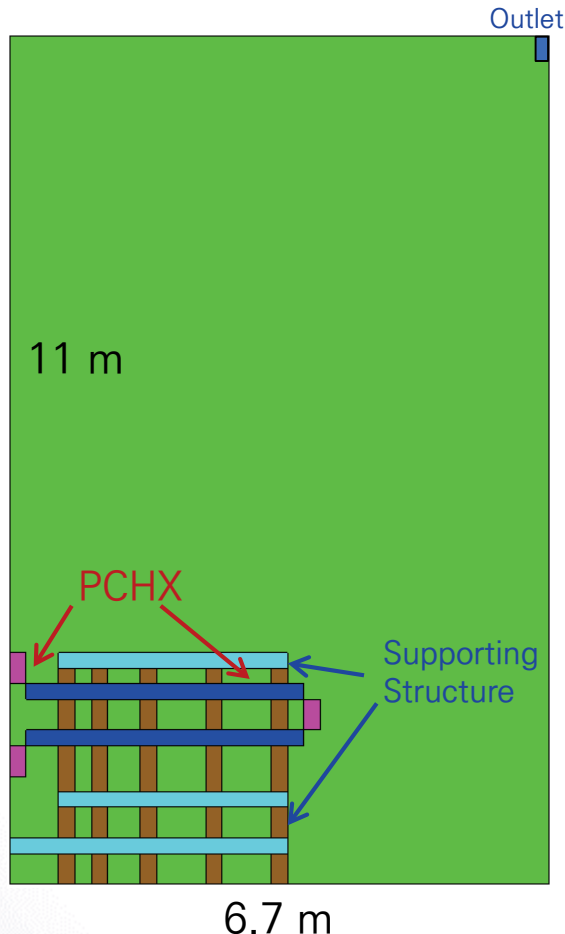
Schematics of PASCAL PCCT
(133 TC installed)



Fluid temperature for 540 kW test condition

❖ CUPID Code Analysis

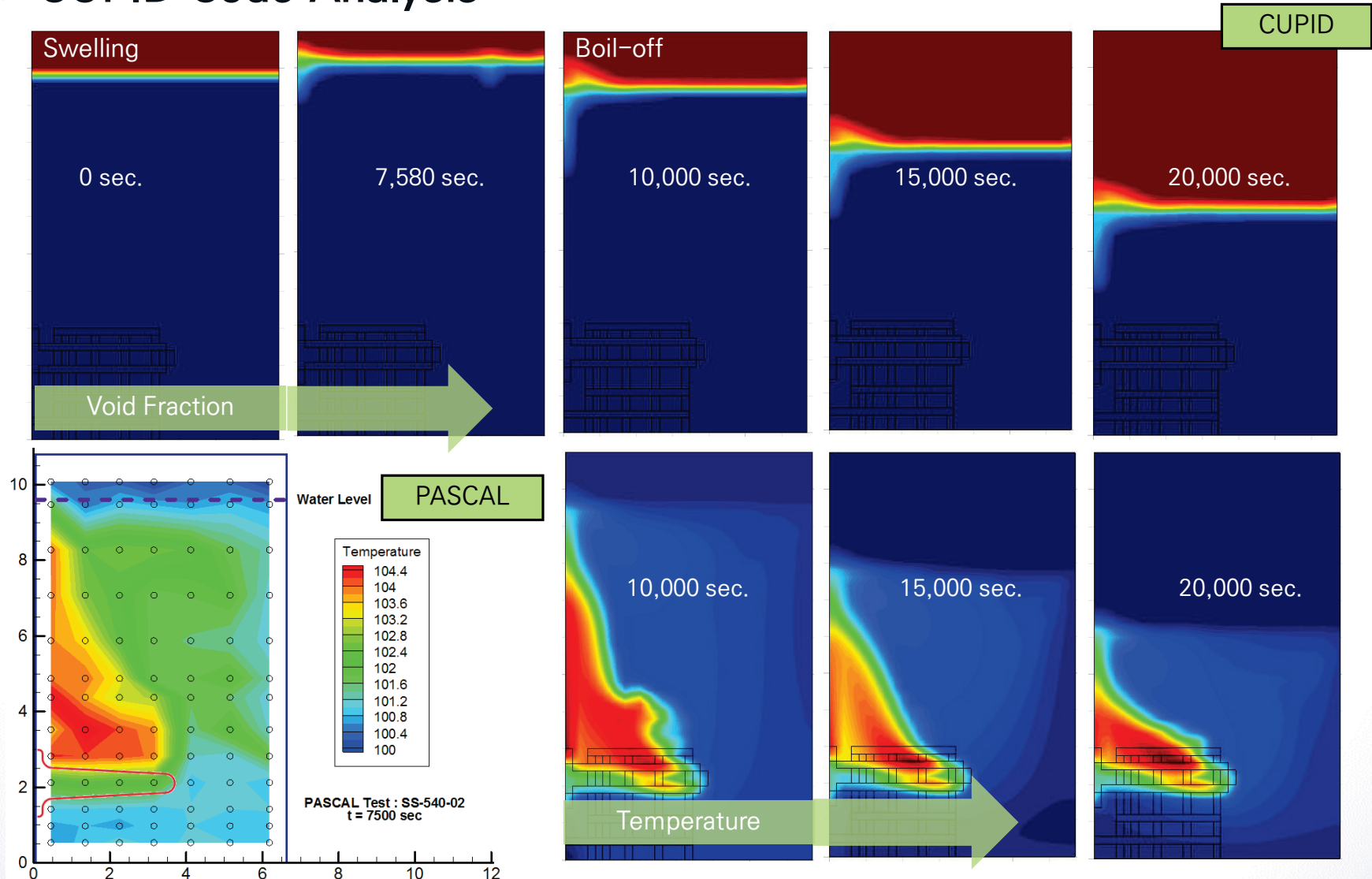
- PASCAL test for SS/PL-540-P1 case



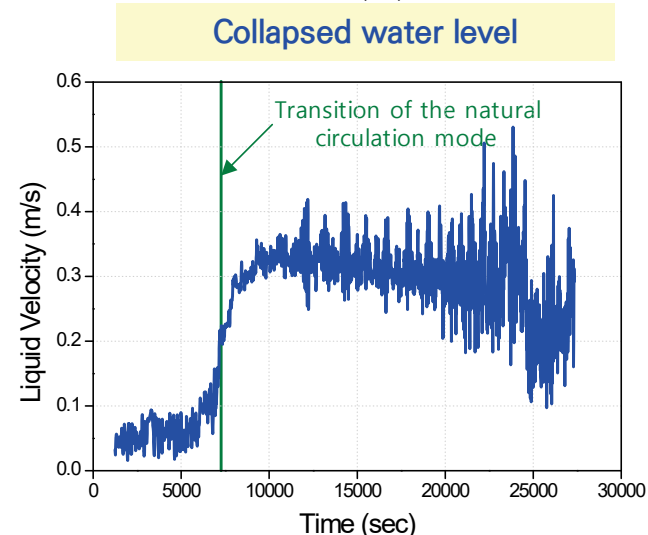
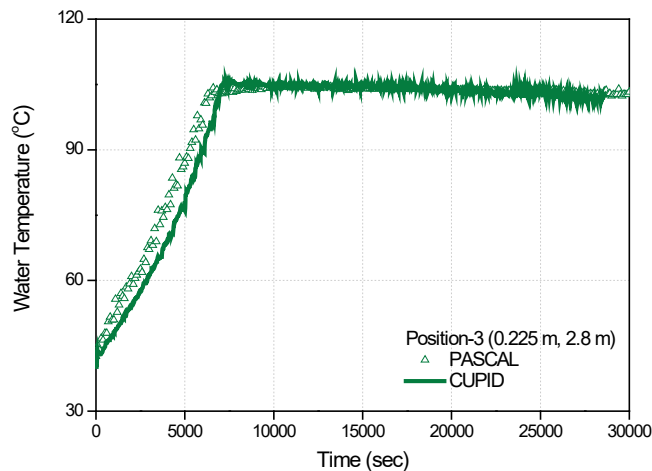
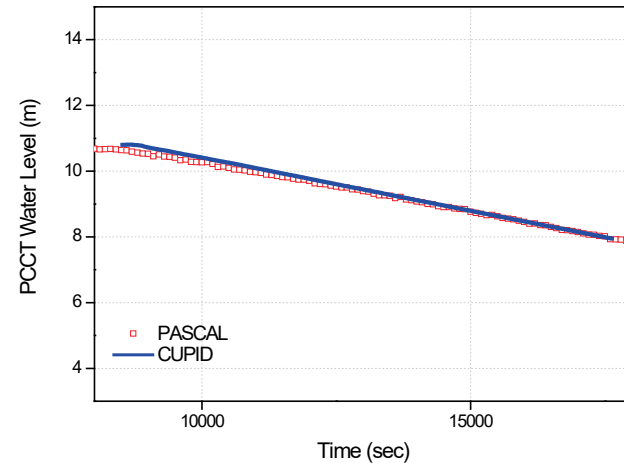
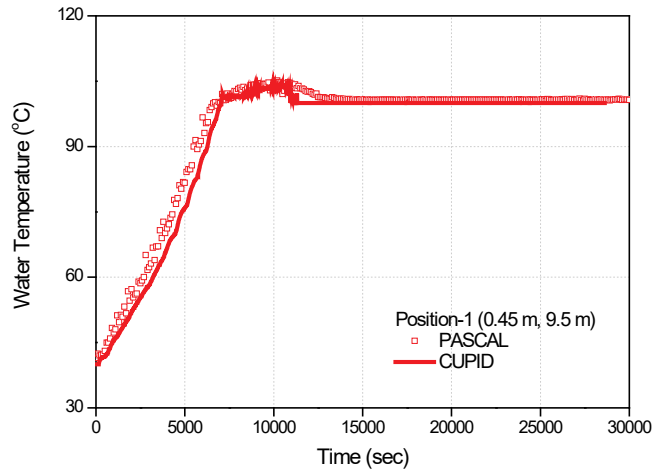
- Geometry: 6.70 m x 11.0 m x 0.112 m
- Approximated in two dimensions
- Grid = 33x55
- Porous media: heat exchanger tube
- Open media: pool-side
- Supporting structure: porous media, no heat
- Heat structure: whole area
- Transient: 30,000 sec
- Heat source boundary condition: 540 kW

02 Natural Convection in a Pool (5)

❖ CUPID Code Analysis



❖ CUPID Code analysis



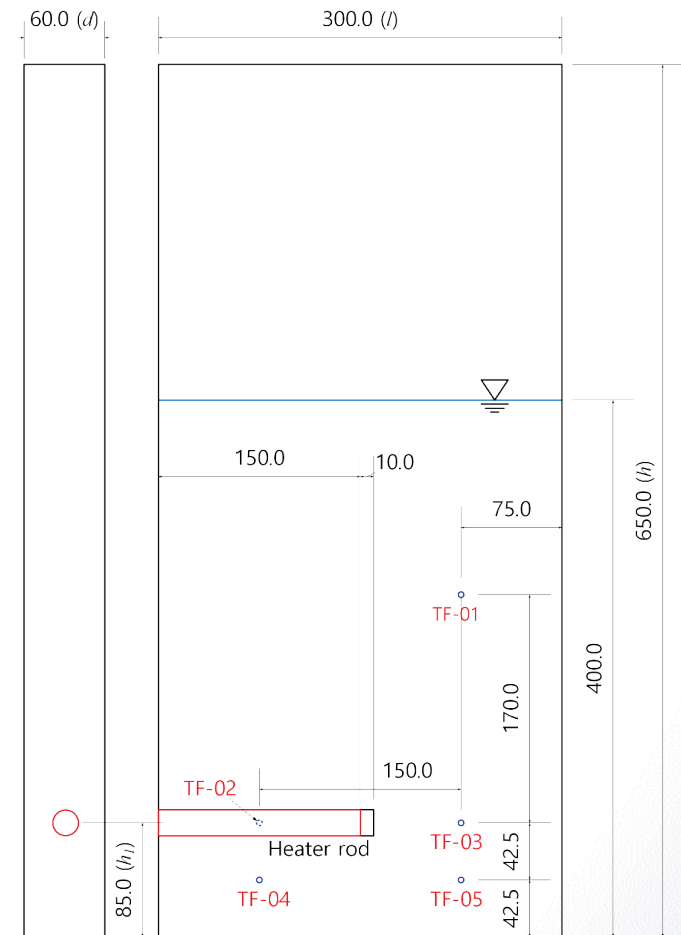
Fluid temperature inside a PCCT

Liquid velocity

❖ Small-sized Pool Experiment

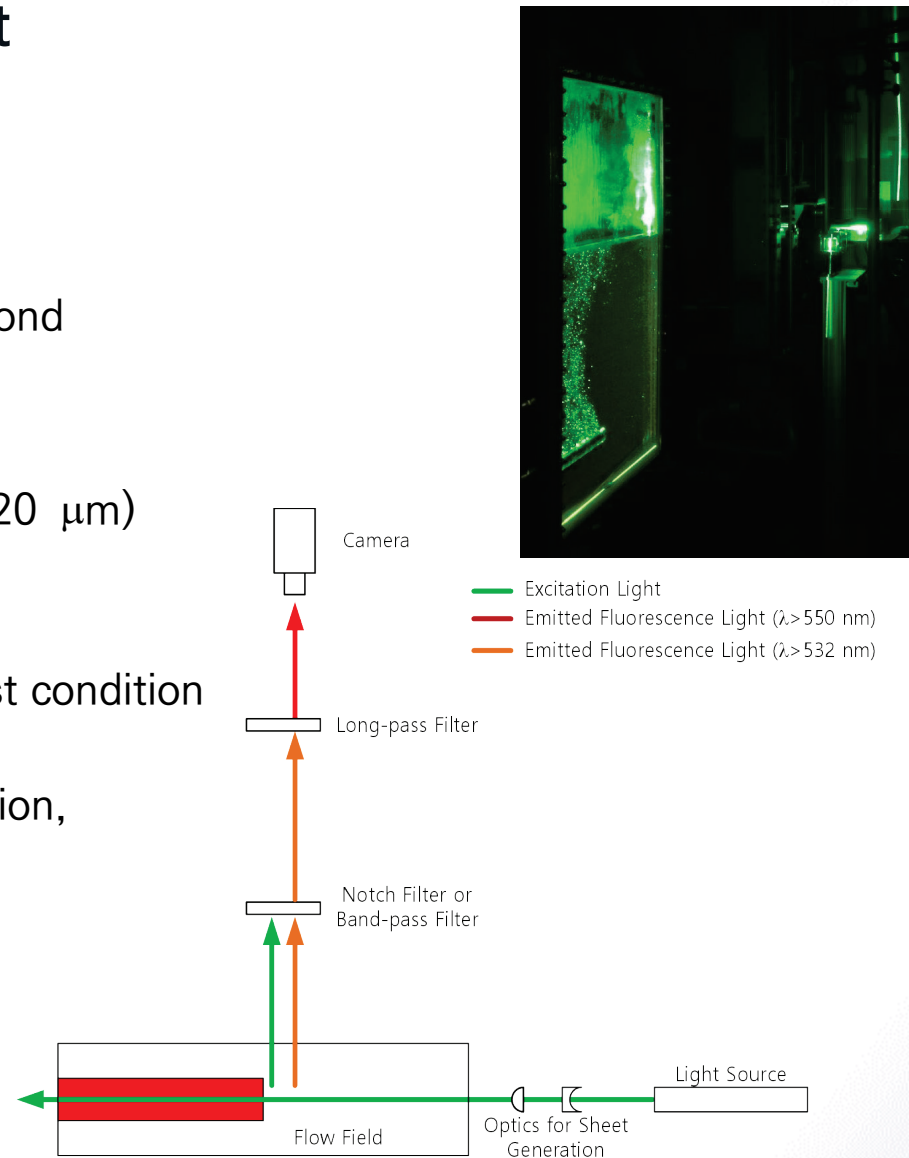
- To obtain the flow velocity information of liquid phase

Size of test rig		$300 \times 650 \times 60 \text{ mm}^3$
Water inventory		$300 \times 400 \times 60 \text{ mm}^3$
Material of test rig	Front	Pyrex (3 mm thickness)
	Back	Polycarbonate (15 mm thickness)
	Left	Stainless steel (20 mm thickness)
	Right	Pyrex (3 mm thickness)
	Bottom	Stainless steel (20 mm thickness)
Heater rod		3/4" diameter, L: 150 mm, 600 W



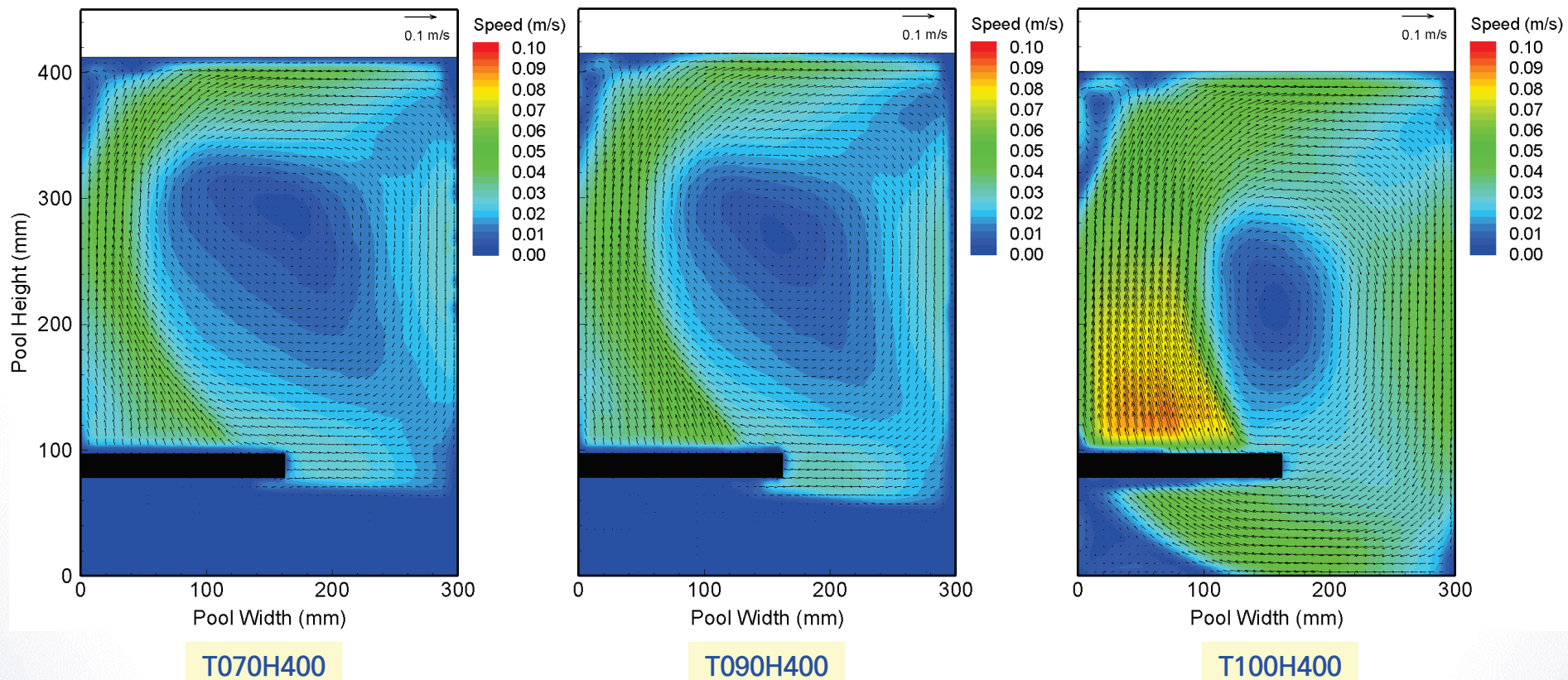
❖ Small-sized Pool Experiment

- PIV system configuration
 - 4M pixels CCD Camera
 - 65 mJ two-head Nd:YAG laser
 - Pulse generator, 8 frames per second
 - Notch filter ($\lambda=532$ nm)
 - Long-pass filter ($\lambda > 550$ nm)
 - Fluorescent polymer particle ($\phi \sim 20$ μm) (SG=1.02)
 - Spatial resolution (Δx): 3 mm
 - 1,000 velocity vector fields per test condition are acquired
 - Ensemble average: mean, fluctuation, turbulence intensity



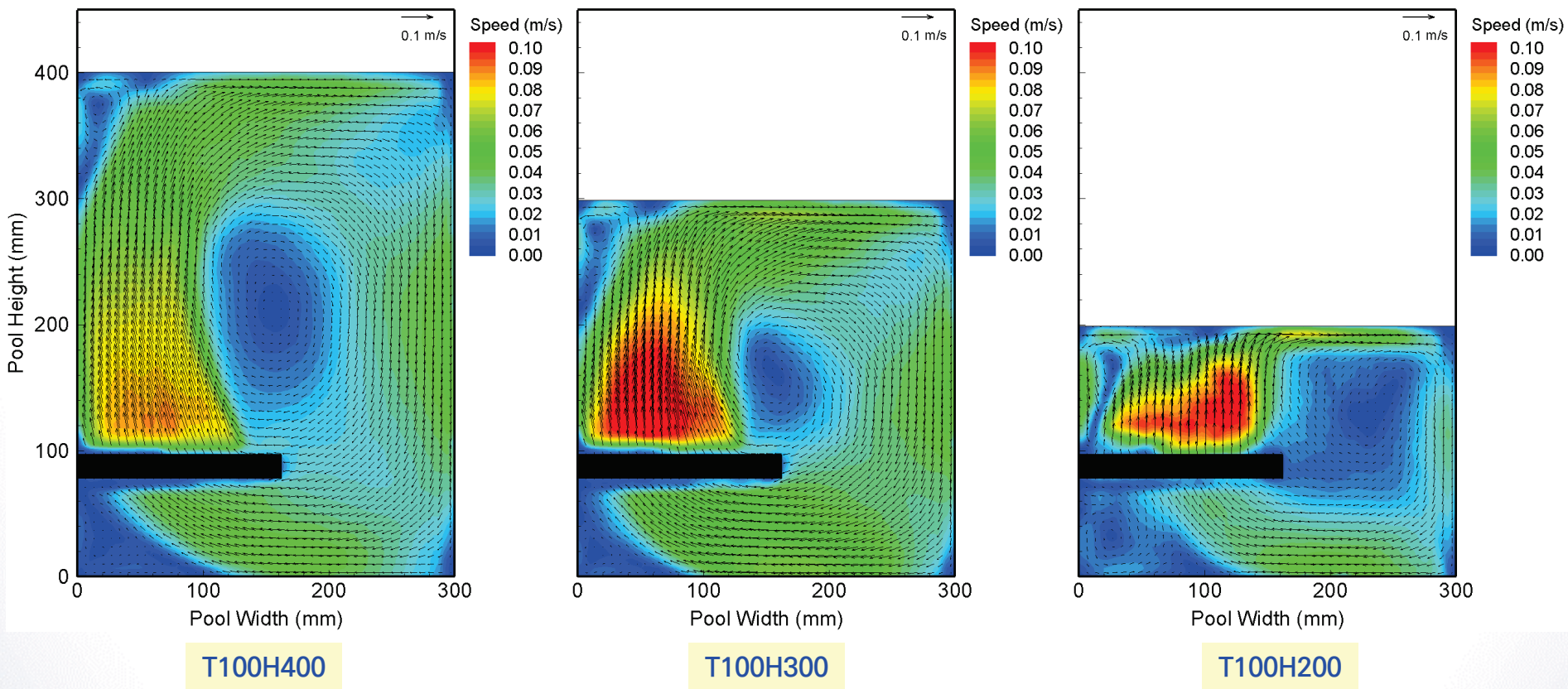
❖ Small-sized Pool Experiment

- Featured mean velocity vector field (with varying pool temperatures)



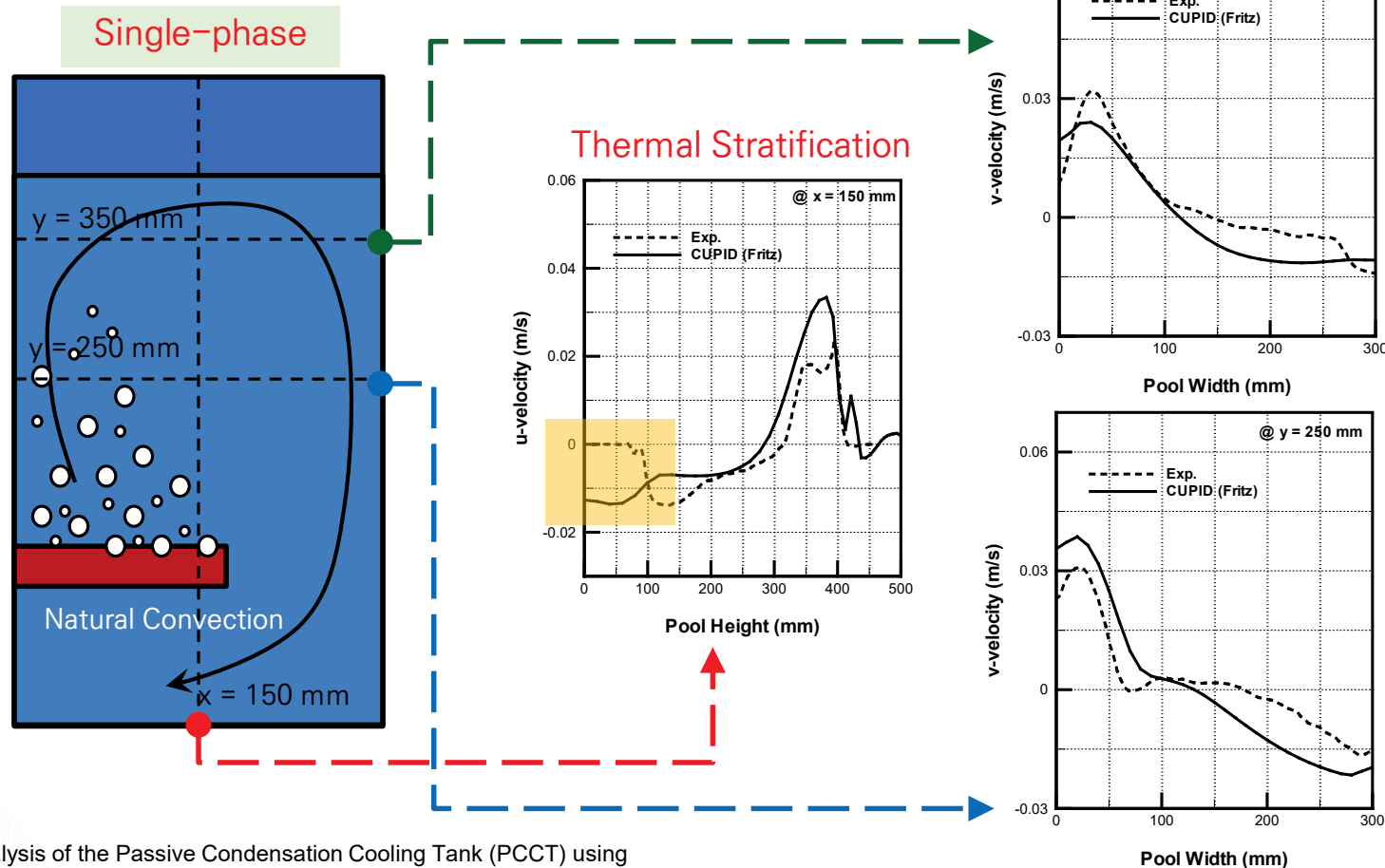
❖ Small-sized Pool Experiment

- Featured mean velocity vector field (with varying pool temperatures)



❖ Small-sized Pool Experiment

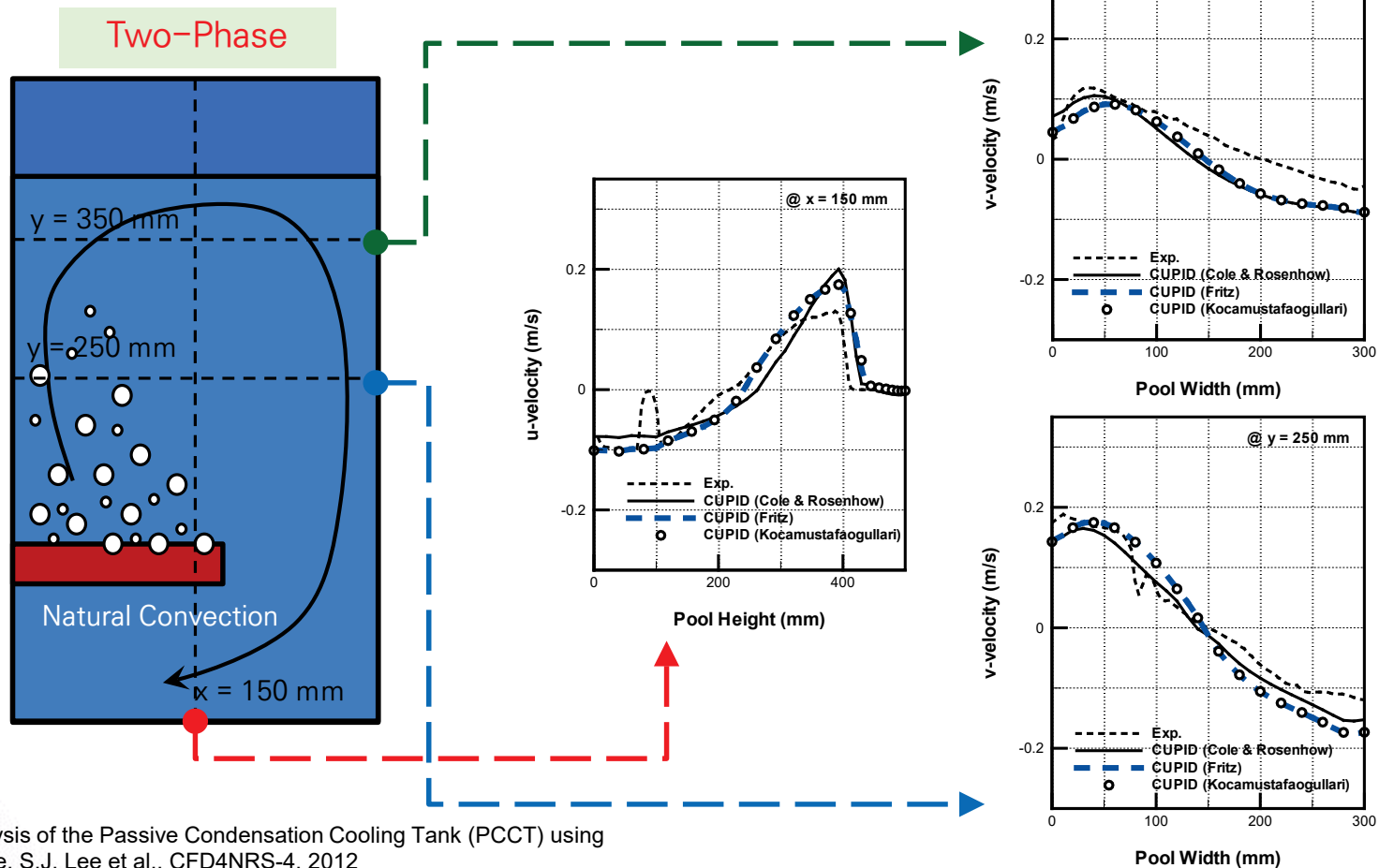
- CUPID code analysis to verify the performance of turbulence model



Numerical Analysis of the Passive Condensation Cooling Tank (PCCT) using the CUPID Code, S.J. Lee et al., CFD4NRS-4, 2012

❖ Small-sized Pool Experiment

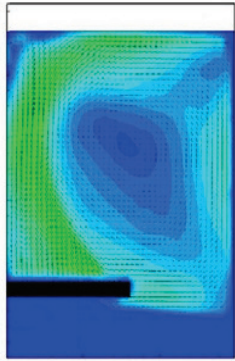
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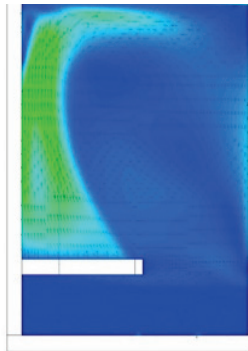
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❖ Small-sized Pool Experiment

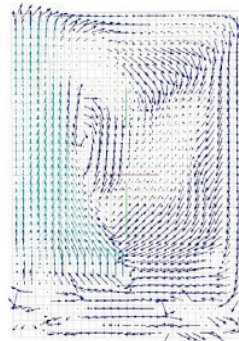
- Assessment using CFD and 3D thermal-hydraulic system code



Experiment

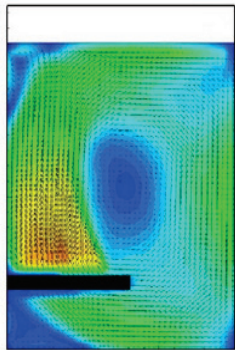


Fluent

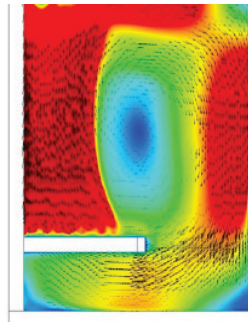


CATHARE

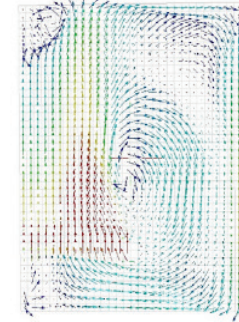
Velocity contour at water temperature 91.3 °C



Experiment



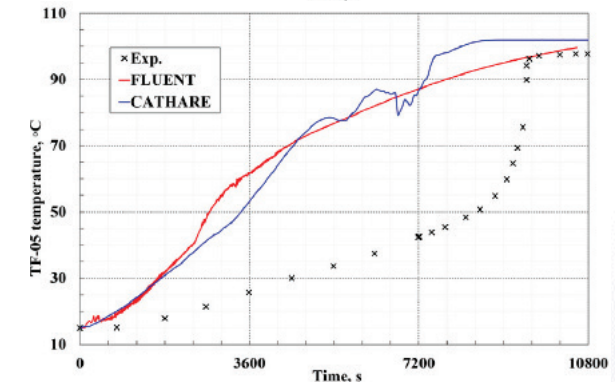
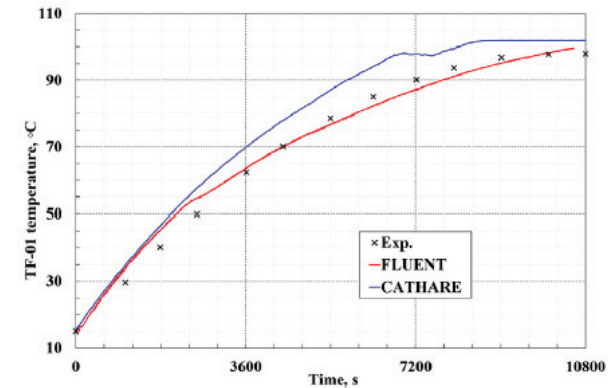
Fluent



CATHARE

Velocity contour at water temperature 98.1 °C

Parameter	Experiment	FLUENT	CATHARE-2
Presence of bottom stratification	Yes	Yes	Yes
Recirculation zone(s)	Yes	Yes	Yes
Stratification break-up	9600 s	4400 s	5600 s
Number of nodes	—	313964	3600
Turbulence model	—	Yes	No
Calculation time CPU	—	504 h	52 h



Comparative study of CFD and 3D thermal-hydraulic system codes in predicting natural convection and thermal stratification phenomena in an experimental facility, Audrius Grazevicius et al., NET, 2023

Rod Bundle Flow Behavior |

Chimney Effect

PRIUS Test Program

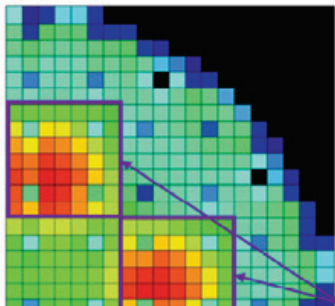
Macroscopic Turbulence Model

CFD code Analysis

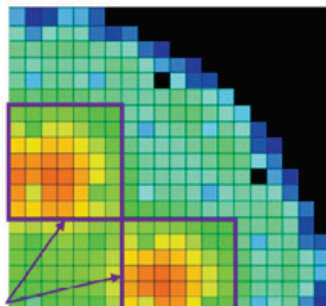
❖ Chimney Effect

- IBLOCA encounter significant 3D effects in core due to the radial power profile, with cross flows and diffusion–dispersion.
 - There are many complicated phenomena during a transient accidents such as chimney effect.

Turbulence dispersion–diffusion model (X)



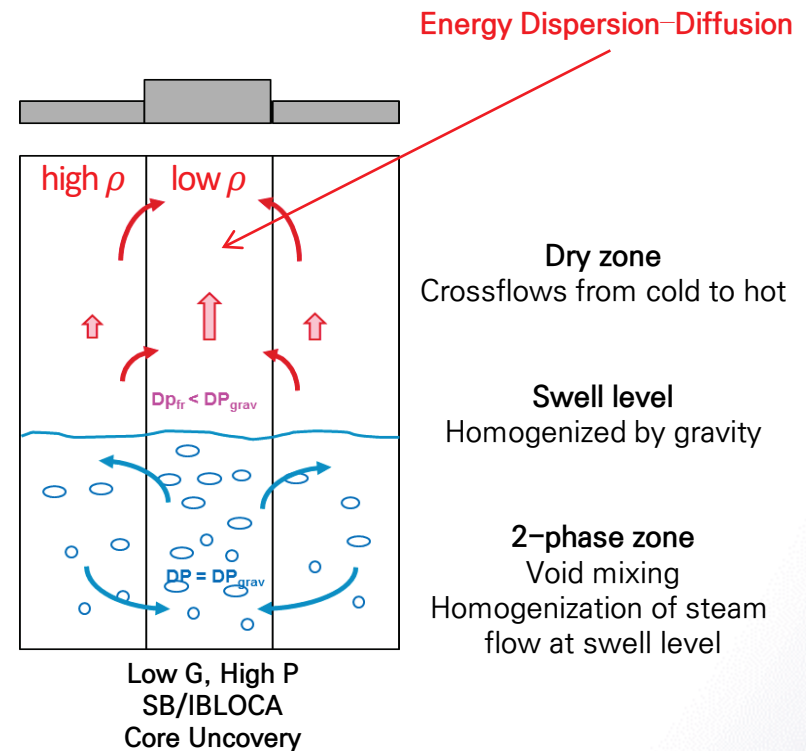
Turbulence dispersion–diffusion model (O)



Max. steam flow temperature
(CEA, CATHARE-3D Analysis)

Important radial transfers may have a significant impact on PCT in SB/IBLOCA

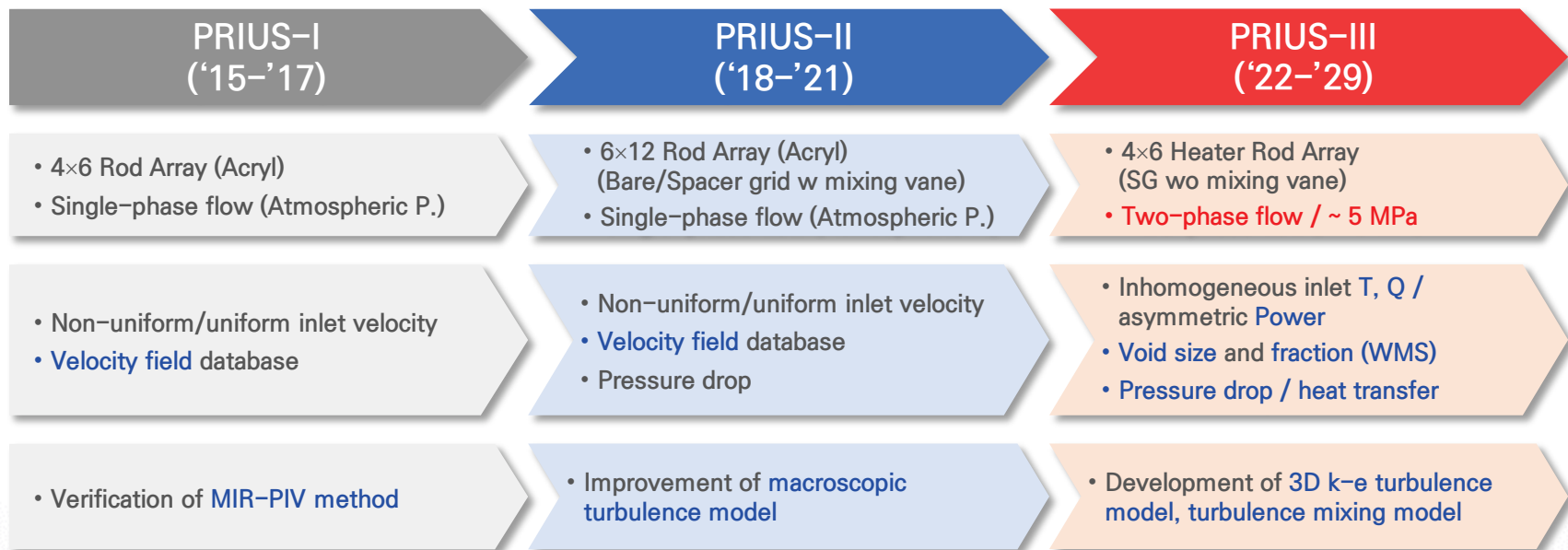
No measurements available of radial transfers!



❖ PRIUS Test Program

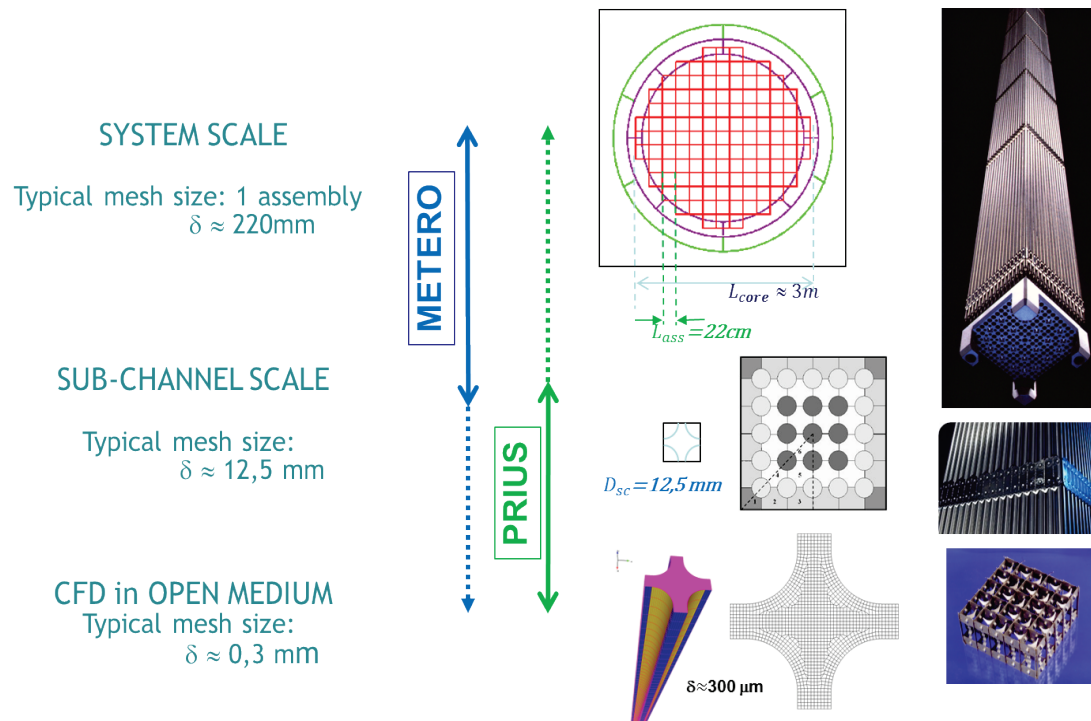
in-PWR Rod-bundle, Investigation of Undeveloped mixing flow between Sub-channels.

- PRIUS experimental campaign has launched to construct a database and improve the turbulence model for crossflow between subchannels.
- Int'l cooperative research work with CEA (METERO)



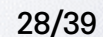
❖ PRIUS Test Program

- To construct high-resolution experimental database to verify the multi-scale safety analysis code on various analysis platforms.
- To validate and improve the turbulence model using the CFD and TH analysis codes.





❖ PRIUS-II Test Section Geometry

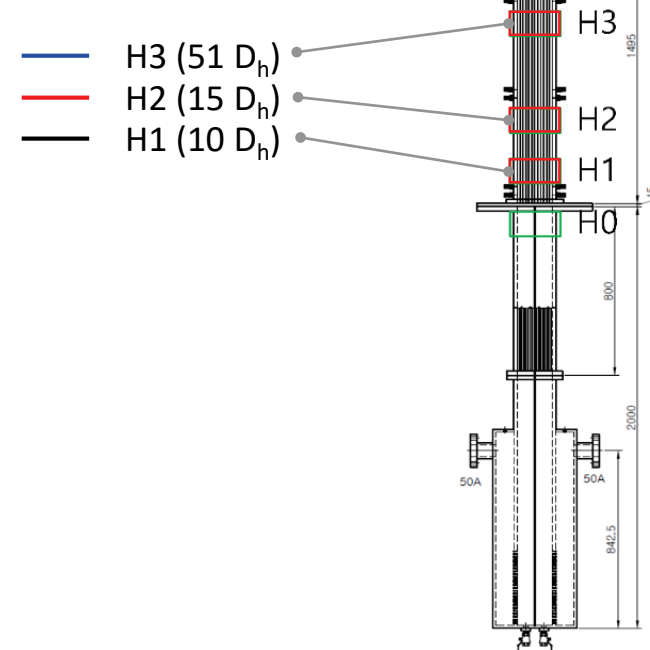
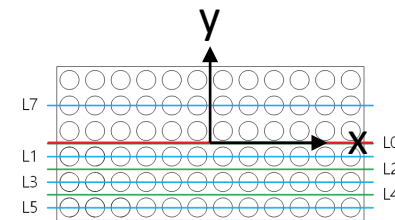
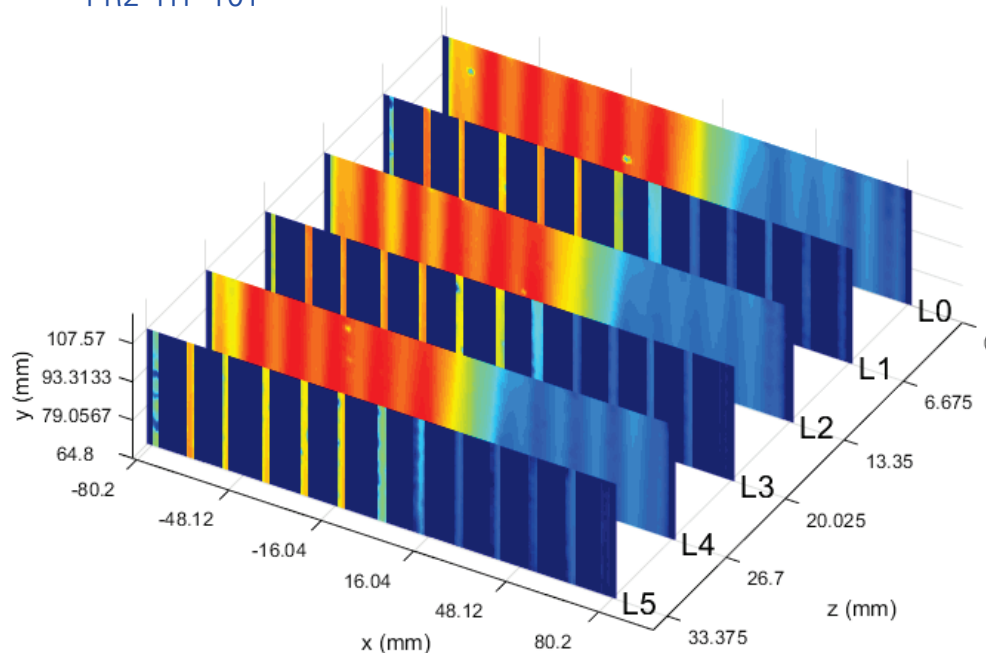


03 Rod Bundle Flow Behavior (4)

❖ Featured streamwise flow behavior

- $Re_{D_h} = 9,000$, 8:2 / 6.5:3.5

PR2-H1-T01



⟨Mean streamwise velocity⟩

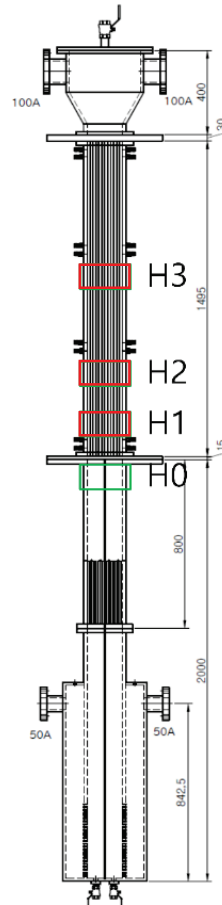
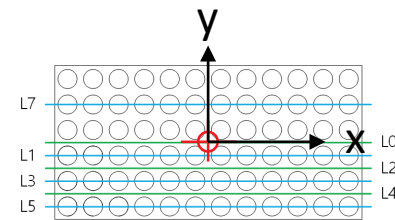
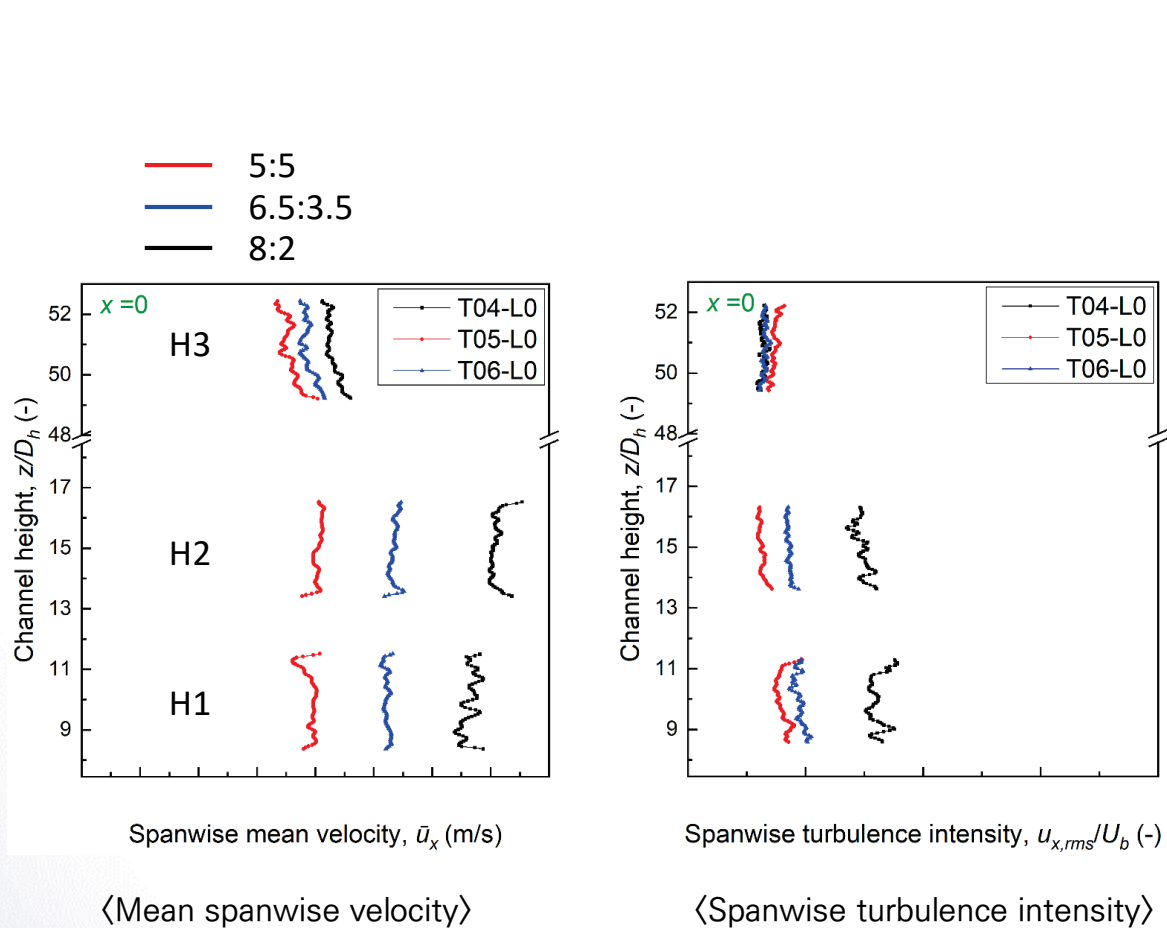
⟨Streamwise turbulence intensity⟩

⟨Measurement plane⟩

03 Rod Bundle Flow Behavior (4)

❖ Featured spanwise flow behavior

- $Re_{D_h} = 9,000$, 8:2 / 6.5:3.5 / 5:5



$\langle \text{Measurement plane} \rangle$

❖ Macroscopic Two-equation Turbulence Model

- Several source term models have been developed for various geometry conditions.
- Chandesris et al. (2001) and Nakayama and Kuwahara (2008) developed source term models for rod-bundle geometry condition.

$$\phi \frac{\partial \langle k \rangle_f}{\partial t} + \frac{\partial}{\partial x_j} \left(\phi \langle \bar{u}_j \rangle_f \langle k \rangle_f \right) = 2\phi \nu_t \langle s_{ij} \rangle_f \langle s_{ij} \rangle_f + \frac{\partial}{\partial x_j} \left(\left(\nu + \frac{\nu_t}{\sigma_k} \right) \frac{\partial \phi \langle k \rangle_f}{\partial x_j} \right) - \phi \langle \varepsilon \rangle_f + \boxed{\phi S_k}$$

$$\phi \frac{\partial \langle \varepsilon \rangle_f}{\partial t} + \frac{\partial}{\partial x_j} \left(\phi \langle \bar{u}_j \rangle_f \langle \varepsilon \rangle_f \right) = \frac{\partial}{\partial x_j} \left(\left(\nu + \frac{\nu_t}{\sigma_\varepsilon} \right) \frac{\partial \phi \langle \varepsilon \rangle_f}{\partial x_j} \right) + \phi \left(2c_1 \nu_t \langle s_{ij} \rangle_f \langle s_{ij} \rangle_f - c_2 \langle \varepsilon \rangle_f \right) \frac{\langle \varepsilon \rangle_f}{\langle k \rangle_f} + \boxed{\phi S_\varepsilon}$$

	S_k	S_ε
Nakayama and Kuwahara (2008)	$S_k = \phi^2 b \left \langle \bar{u} \rangle_f \right ^3,$ $b = \frac{0.3164}{2D_h \text{Re}_{D_h}^{0.25} \phi^2}$	$S_\varepsilon = c_{2\varepsilon} \phi^2 b \sqrt{\frac{c_D \phi}{2K}} \left \langle \bar{u} \rangle_f \right ^4,$ $K = \frac{\phi}{32} D_h^2$
Chandesris (2006)	$S_k = \varepsilon_\infty,$ $\varepsilon_\infty = 2C_f \frac{\langle \bar{u} \rangle_f^3}{D_h} \left(1 - y_{\text{lim}}^+ \sqrt{\frac{C_f}{2}} \right)$	$S_\varepsilon = c_2 \frac{\varepsilon_\infty^2}{k_\infty},$ $k_\infty = c_p \langle \bar{u} \rangle_f^2 \text{Re}_{D_h}^{-1/6}$

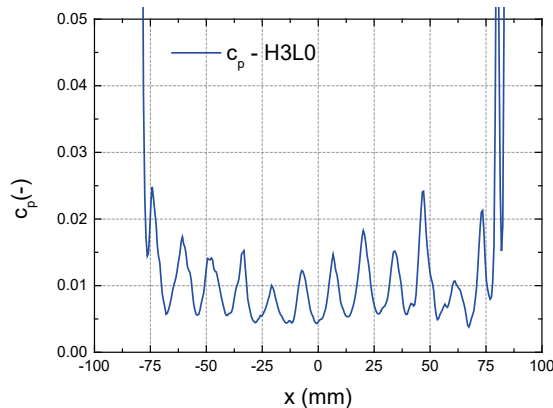
⟨Source term models for the longitudinal flow condition⟩



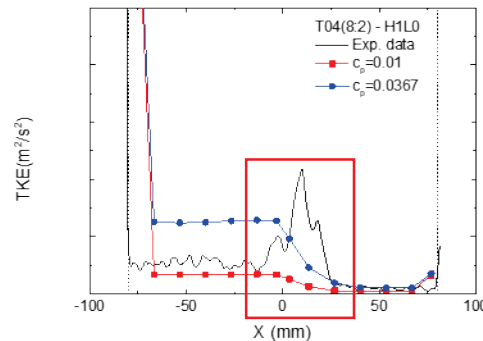
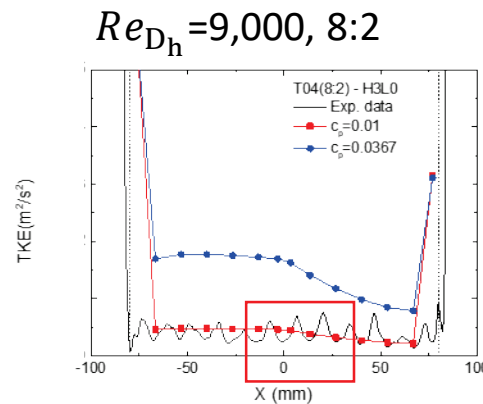
❖ Modification of the Experimental Constant c_p

- The experimental constant of Chandesris (2006) model was obtained using the data measured in the fully developed region.

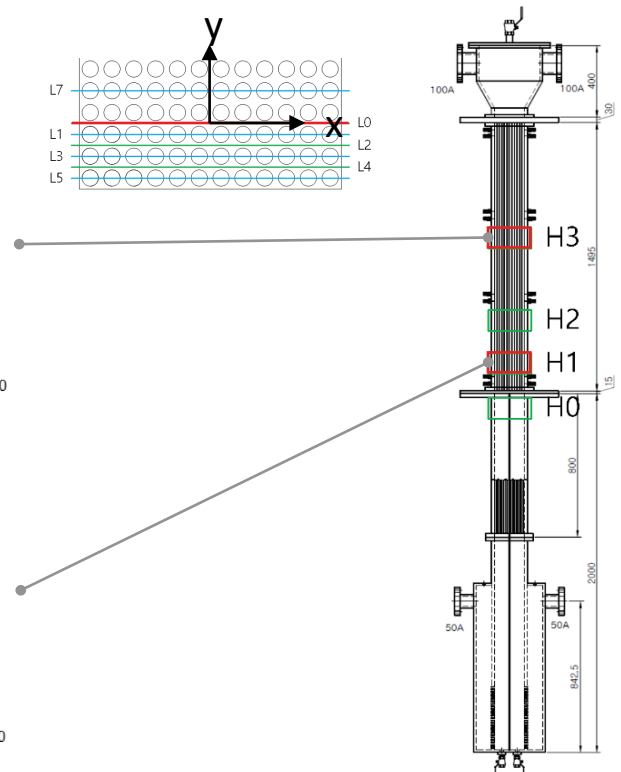
$$c_p = \frac{k_{\infty}}{\langle \bar{u} \rangle_f^2 \text{Re}_{D_h}^{-1/6}}$$



Chandesris (2006): 0.0367 for the pipe
PRIUS-II (2021): 0.01



⟨TKE distribution⟩



⟨Measurement plane⟩

❖ Experimental constant c_p modeling

- Based on the assumption that the velocity gradient affects the turbulence dissipation, a new type of c_p was proposed.

$$c_p = 0.01 + c_1 \text{Re}_l^{c_2} \left(\frac{\partial u_z}{\partial x} \right)^2$$

❖ S_k modeling

- Term including the velocity gradient was added to the source term of the TKE transport equation.

$$S_k = \varepsilon_\infty + S_a \quad S_a = c_k \frac{\mu}{\rho} \left(\frac{\partial u_z}{\partial x} \right)^2 \quad c_k = 0.225 \text{Re}_l$$

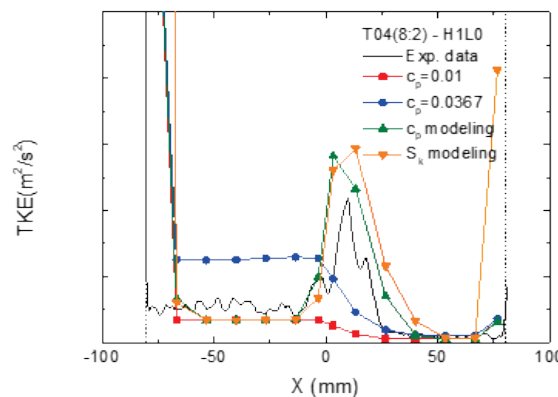
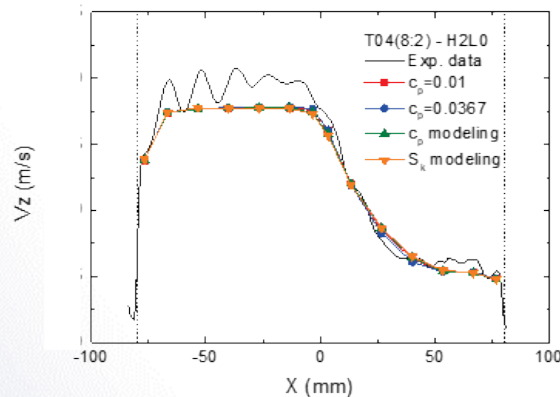
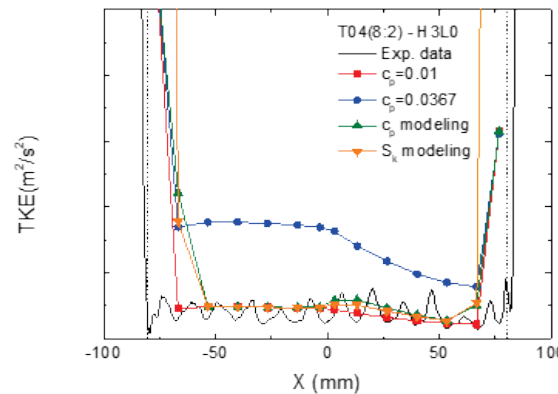
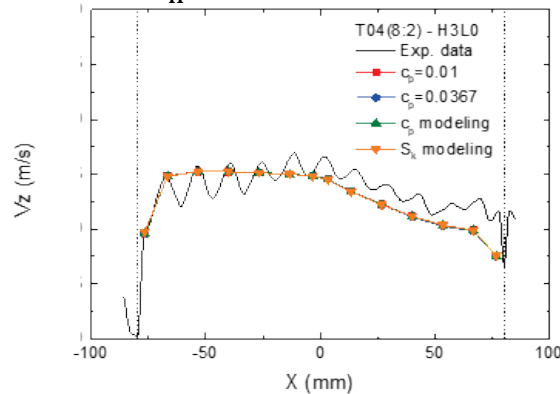
	S_k	S_ε
Chandesris (2006)	$S_k = \varepsilon_\infty,$ $\varepsilon_\infty = 2C_f \frac{\langle \bar{u} \rangle_f^3}{D_h} \left(1 - y_{\text{lim}}^+ \sqrt{\frac{C_f}{2}} \right)$	$S_\varepsilon = c_2 \frac{\varepsilon_\infty^2}{k_\infty},$ $k_\infty = c_p \langle \bar{u} \rangle_f^2 \text{Re}_{D_h}^{-1/6}$

03 Rod Bundle Flow Behavior (6)

❖ Prediction Performance of the Improved Models

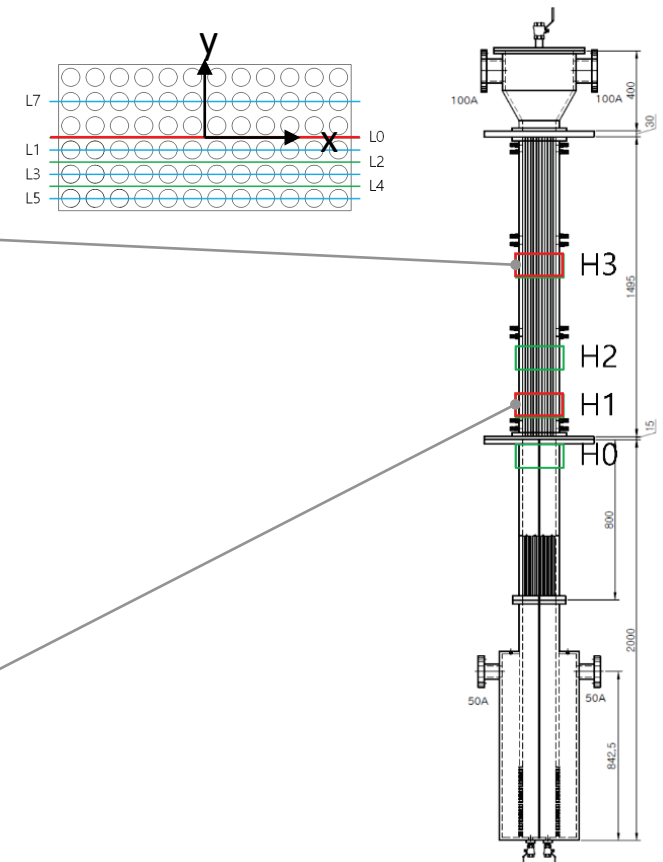
- Improved source term model predicted the TKE under asymmetric flow conditions better than the previous model.

$Re_{D_h} = 9,000, 8:2$



⟨Mean streamwise velocity⟩

⟨TKE distribution⟩



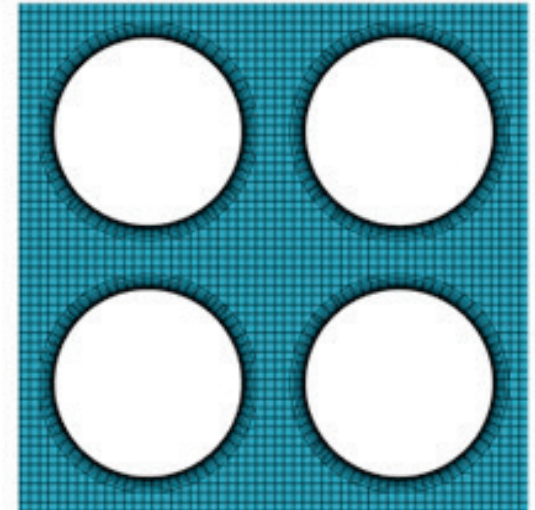
⟨Measurement plane⟩

❖ CFD Code Analysis

- STAR-CCM+ 15.06.008
- Models
 - Steady
 - Turbulence Model ($k-\varepsilon$, $k-\omega$, RST)
 - Constant Density

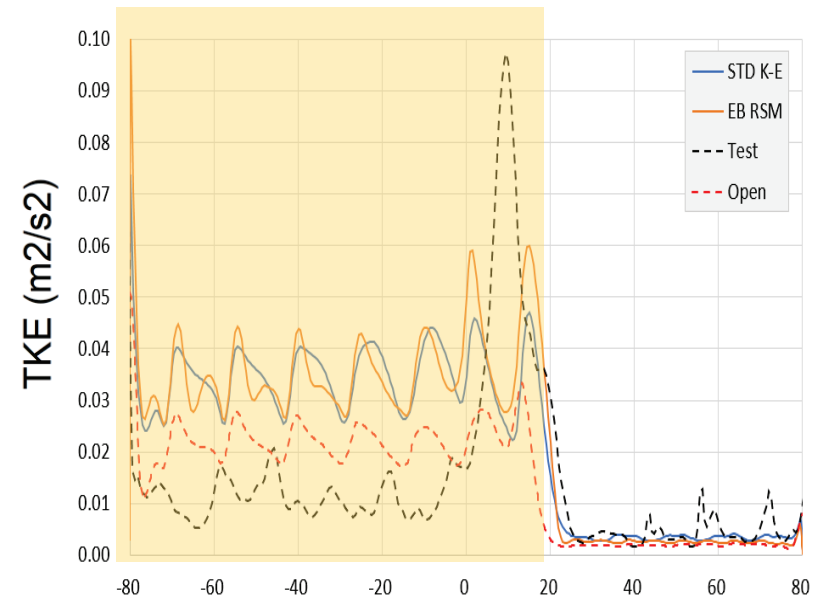
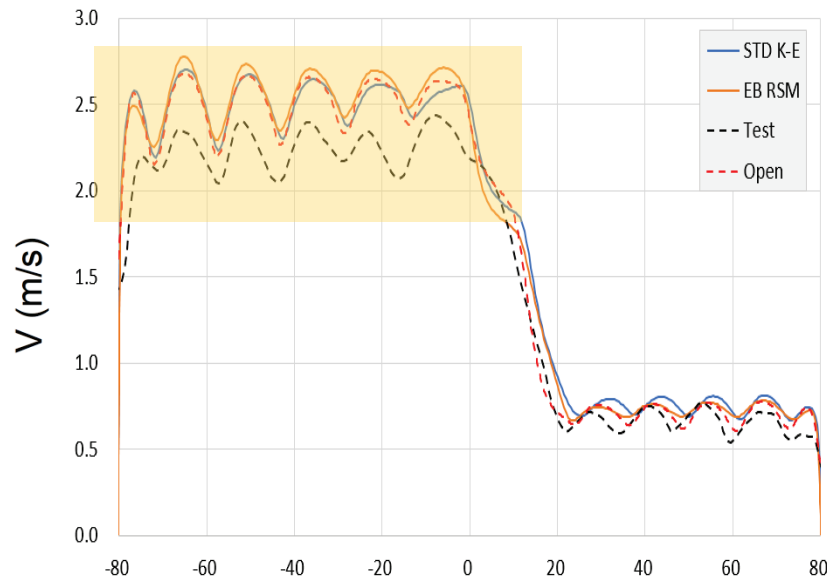


- Trimmed Mesh
 - Base Size: 0.5mm
 - Number of Layer: 12개
 - Layer Thickness: 2mm
 - Total Volume Mesh: 39,460,415



❖ CFD Code Analysis

- $k-\varepsilon$ / EB(Elliptic Blending) RSM models showed similar velocity profiles.
- TKE was over-predicted.



Summary |

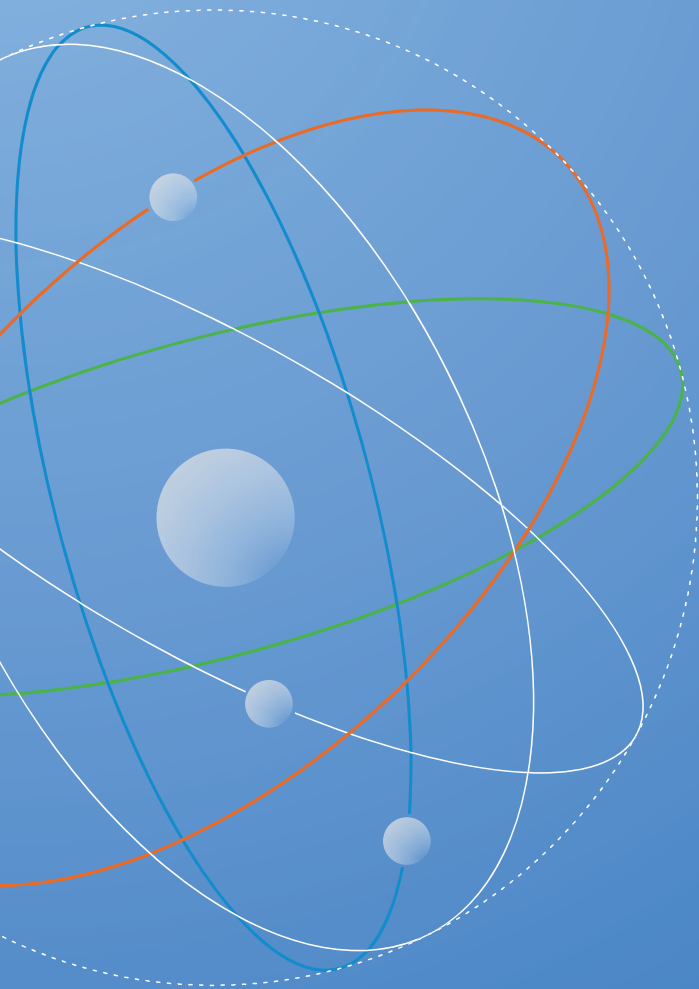


❖ CFD-grade Experiment

- To validate the physical model used in CFD simulations.
 - Experiment provides a relatively low uncertainty of validation and allows a good determination of the model uncertainty.

❖ Application of passive system and core mixing problems

- Identification of lacking data for code validation of some passive systems and core multi-dimensional flow phenomena
 - Collect experimental data with mixing in presence of buoyancy effects
 - Core TH
 - Upscaling of models from CFD to sub-channel and to porous 3D
 - CUPID code for validation of sub-channel model + validation of CFD



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